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Arsenic Entrapment in Reactive Columns of Residual Soils

Magalí E. Carro Perez¹ and Franco M. Francisca²

Abstract: The purpose of this research is to evaluate the aptitude of two residual soils for the remediation of arsenic (As) contaminated 3 groundwater. Batch and soil column tests were performed to evaluate removal of As from water. Permeable soil columns were prepared with 4 5 mixtures of sand (90%) and two lateritic soils (10%). Results showed that removal of As in batch tests ranged from 95–99% when using a solid-liquid ratio equal to 1:10. Experimental results obtained in the soil column tests and calibrated simulation models showed that the 6 amount of water that can be decontaminated depends on the initial As concentration and the flow rate. Maximum adsorption capacities 7 in bath test and removal efficiency in soil columns tests clearly relates with the amount of iron compounds in the solid phase. The quality 8 9 of residual soil samples are related to a high iron content to favor As removal and low clay-size particle content to achieve acceptable flow rates for water purification in low-cost permeable filters and permeable reactive barriers. DOI: 10.1061/(ASCE)EE.1943-7870.0000697. 10 11 © 2013 American Society of Civil Engineers.

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13 Author keywords: Adsorption; Flow; Arsenic; Remediation.

14 Introduction

15 Aquifers containing arsenic (As) concentrations higher than that recommended for drinking water were identified in many places 16 around the world. In general, the presence of arsenic was associated 17 18 with either natural or anthropogenic sources. In any case, this situation was responsible for limitations in possible uses of ground-19 20 water as a source of drinking water or for agriculture purposes. The pH and redox potential affect the speciation of arsenic. In general, 21 22 inorganic arsenic was found in surface water and groundwater 23 either as arsenite (As III) under reducing conditions or arsenate (As V) under oxidizing conditions (Masscheleyn et al. 1991; 24 25 Smedley et al. 2002).

The ingestion of water containing As has been related to serious 26 27 health problems including cancer, skin problems, vascular disease, and neuropathy (Smith et al. 2002; Aballay et al. 2012). This sit-28 29 uation has become of fundamental importance in many places around the world where groundwater is the main source of drinking 30 31 water, such as in Bangladesh and India, and when groundwater 32 is the only source of water for dispersed and rural population in 33 Latin America (Francisca and Carro Perez 2009; Bundschuh et al. 34 2010). The maximum As concentration suggested by the World 35 Health Organization (WHO) for drinking water is 0.01 mg/L 36 (WHO 2006).

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Removal of As is a challenging problem in many places around the world where aquifers contain concentrations of this substance that exceed drinking water standards. Different remediation techniques were developed in the past decades for the removal of arsenic from water. Alternatives available for arsenic removal include chemical oxidation, precipitation, coagulation, inverse osmosis, adsorption, biological degradation, enhanced bioremediation, electrokinetic, phytoremediation, biosorption, and photochemical oxidative technologies (Litter et al. 2010). Among them, adsorption is frequently preferred because of its low cost and abundance of reactive materials that can be used for the sequestration of arsenic.

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The adsorption in a waste by-product, in zero valent iron, iron nanoparticles, and natural products attracted the attention of several researchers (Daus et al. 2004; Kanel et al. 2005; Chen et al. 2007; Jovanovĭcand Rajakovĭc2010; Mlilo 2010; Tuutijärvi et al. 2010). Indeed, previous research with activated carbon, bauxite, hematite, goethite, gibbsite, zeolites, and clay minerals showed that arsenic was successfully removed from water (Litter et al. 2010). Among the existing sorbent materials, residual soils present the advantage of their abundance and low cost, which is fundamental to find economical arsenic remediation techniques. Both As(III) and As(V) were successfully removed from water in batch tests with lateritic soils (Maiti et al. 2007).

Weathering of rocks generates different horizons within a soil profile. Residual and lateritic soils form in a wet and tropical climate and are rich in iron oxides and aluminum hydroxides. The accumulation of iron compounds in these soils gives the possibility of using these materials for the removal of As. Micro-scale particle-fluid interaction mechanisms are responsible for the attraction between the As and iron compounds, leading to the adsorption of dissolved As ions. Therefore, the As concentration in water reduces. This behavior was successfully confirmed by means of batch tests (Maji et al. 2008; Gibbons and Gagnon 2010). However, in the case of permeable reactive filters, the influence of flow conditions and initial As concentration on the sequestration of As in the residual soil still needs to be determined.

The purpose of this study was to evaluate the potential of two samples from the B-horizon within a soil profile for the decontamination of As contaminated water. The main interest was to 76 determine the effect of adsorption mechanisms and flow rate con-

77 ditions on the sequestration of arsenic ions dissolved in the liquid

vsed as permeating fluid in reactive soil columns.

79 Underlying Physical Concepts

A brief review of the fundamental mass transport phenomenon is presented in this section, giving that advection and diffusion mechanisms are used to explain the displacement of As within the pores of a reactive soil column or permeable barrier.

84 Mass Transport in Granular Filters

85 Displacement of dissolved ions inside porous media is controlled 86 by chemical diffusion, advection, and mechanical dispersion. The 87 relationship between these phenomena mainly depends on soil 88 properties and is frequently evaluated by analyzing the Peclet's 89 number (Fetter 1993). Assuming homogeneous and isotropic 90 media, saturated with a fluid that follows Darcy's law, and consid-91 ering one-directional flow, the total mass transport per unit area and 92 time F [kg/(m² · s)] is

$$F = n_e v_e C - n_e D_L^* \frac{\partial C}{\partial x} \tag{1}$$

$$\frac{\partial F}{\partial x} = -n_e \frac{\partial C}{\partial t} \tag{2}$$

93 where t (s) = time; n_e = effective porosity; v_e (m/s) = seepage 94 velocity; C (kg/m³) = contaminant concentration; and D_L^* 95 (m²/s) = longitudinal hydrodynamic dispersion coefficient. The 96 presence of high ionic strength solutions or extreme pH conditions 97 affects the particle surface charge and modifies the hydraulic con-98 ductivity and seepage velocity (Jo et al. 2001).

99 The partial differential equation that describes the solute trans-100 port in reactive porous media is obtained by incorporating diffu-101 sion and advection as mass transport mechanisms and the effect of 102 source/sink for the chemical substance under consideration (Sharma 103 and Reddy 2004)

$$D_L^* \frac{\partial^2 C}{\partial x^2} - v_e \frac{\partial C}{\partial x} \pm \frac{r}{n_e} = \frac{\partial C}{\partial t}$$
(3)

104 where $r = -(B_d/\theta).(\partial C^*/\partial t)$ (kg/m³/s) = rate of mass production/ 105 consumption given by the kinetic model of reaction; B_d (kg/m³) = 106 porous media bulk density; θ = volumetric water content (or 107 porosity for saturated media); and C^* = adsorbed mass on soil 108 particles per unit weight of solids. The amount of As adsorbed 109 on soil particles can be further related to the initial contaminant 110 concentration (C_0) through any adsorption isotherm.

111 Adsorption delays contaminant percolation and transport. The 112 time, or pore volume of flow, needed by the center of mass of a 113 contaminant plume to pass through a soil column, with respect 114 to the expected time or volume for nonreactive transport (diffusion + advection only) defines a retardation factor (R). The solution 115 116 of Eq. (3) depends on the boundary and flow conditions. However, 117 for advection-dominated systems and all possible boundary condi-118 tions, the solution to Eq. (3) becomes (Ogata and Banks 1961)

$$C_{(x,t)} = \frac{C_0}{2} \operatorname{erfc}\left(\frac{R.x - v.t}{2\sqrt{D_L^*.t.R}}\right) \tag{4}$$

120The retardation factor R can be either computed from calibrated121isotherms or directly measured in soil column tests.

Materials and Methods

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Soils

The tested materials included sand and two different residual soils that were identified as lateritic soils.

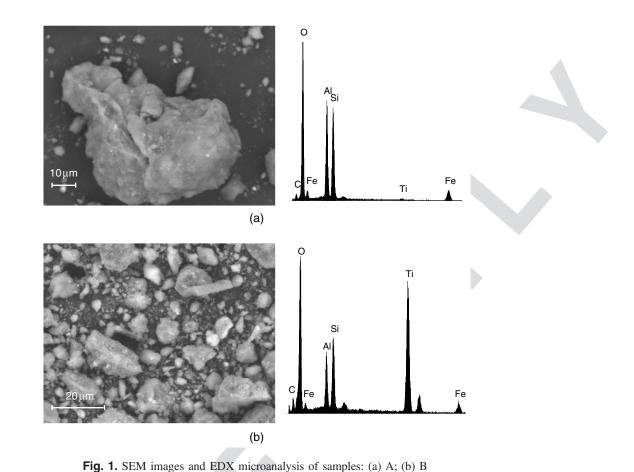
The sand was taken from the Anisacate River in Córdoba, Argentina. An optic diffraction test reveals that this coarse grain soil is mainly composed by pure minerals, including quartz (43%), feldspars (12%) and muscovite (1%), and rock fractions composed by granite (38%) and other clasts in a less percentage. The sand was classified as poorly graded sand according to the Unified Soil Classification System (ASTM 2007). The mean particle diameter determined from sieve analysis was 1 mm, and only 10% of grains (by weight) have a particle diameter lower than 0.41 mm. Montoro and Francisca (2010) determined that this sand was nonreactive and highly permeable and that it showed no significant physicochemical interactions with high ionic strength solutions.

The two residual samples were obtained from a B-horizon in a 138 weathering profile from 1 m below the surface at two sampling 139 points 10 m apart from each other, in Oberá, Misiones, Argentina 140 (Table 1). The two samples had high content of particles smaller 141 than 2 μ m (ASTM 2007). The liquid limit, plastic index (ASTM 142 2007), and amount of particles smaller than 74 μ m (ASTM 2007) 143 showed that specimens A and B classified as CL and CH according 144 to the Unified Soil Classification System, which corresponded to 145 inorganic clays of medium and high plasticity, respectively (ASTM 146 2007). High amounts of aluminum and iron oxides were identified 147 in the semiquantitative chemical composition determined from 148 scanning electron microscopy (SEM) images and energy dispersive 149 X-ray (EDX) analyses (Fig. 1). The EDX-spectra were obtained 150 from a visual field of 5 μ m × 5 μ m. X-ray diffraction tests revealed 151 that sample A was mainly composed of quartz, hematite, and 152 kaolinite and in less proportion of plagioclase and lithiophorite. 153 In sample B, the most abundant minerals were quartz, goethite, 154 kaolinite, anatase, plagioclase, and titanite (Fig. 2). The minerals 155 identified in the X-ray diffraction tests are in good agreement with 156 the chemical composition determined from the EDX spectra. 157

The sand was mixed with either sample A or sample B to pre-158 pare permeable soil columns. Different mixtures were prepared to 159 evaluate the behavior of the soil columns. Very low hydraulic con-160 ductivity was observed when the amount of residual soil was higher 161 than 20%, and fine particle migration was observed when the 162 residual soil content was lower than 2.5%. Then, soil mixtures were 163 prepared with 90% of sand and 10% of either sample A or sample B 164 (by weight). The amount of residual sample from the B-horizon in 165 the mixture was selected to obtain hydraulic conductivities higher 166 than 5×10^{-8} m/s to facilitate liquid displacement inside the pores 167 and to avoid the effect of fine particle migration. The sand formed a 168 rigid skeleton containing the silt and clay size particles of the 169 residual soil which created a reactive matrix. 170

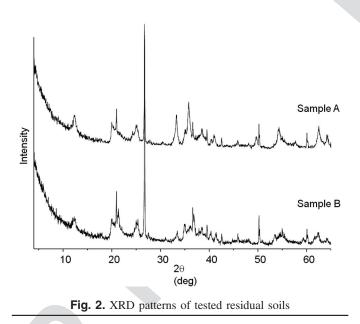
Table 1. Relevant Properties of the Soils

	Sample		
Property	А	В	
Liquid limit (%)	45.3	65.0	
Plastic index (%)	18.6	39.7	
Fine particles <74 μ m (%)	100	100	
Clay size particles <2 μ m (%)	75	66	
Specific gravity	2.79	2.80	
Specific surface (m^2/g)	3.7	3.7	
Fe content (% in w/w)	5.47	2.98	



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F2:1



171 Arsenic Solutions

172 Solutions containing different As concentrations were prepared 173 from the dissolution of arsenic trioxide (As₂O₃) in an alkaline 174 medium obtained with sodium hydroxide (NaOH) and distilled 175 water. Arsenic concentrations were 0.1; 0.5; 1; 5; 10; 15; 20; 176 and 25 mg/L, which includes the registered concentration in 177 most aquifers in the center of Argentina. The pH and Eh of the 178 obtained solutions were pH = 7.3-7.9 and Eh = 175-230. Thus, 179 the main expected arsenic speciation was $HAsO_4^{2-}$ according to 180 Masscheleyn et al. (1991).

Arsenic Measurements

The arsenic concentrations were determined by means of arsenic 182 test strips (Arsen 10 and Arsen 50 from Quantofix). The color 183 of a paper strip after reacting with arsine gas was compared with 184 color charts to obtain the arsenic concentration. This colorimetric 185 method was improved to enhance the accuracy of the measure-186 ments. An improved analysis of reactions was implemented with 187 the purpose of eliminating the operator influence on results. The 188 implemented method consisted of taking 10 high resolution pic-189 tures of the paper strip from a specific distance, camera setting, 190 and illumination conditions in the first minute after the reaction. 191 These color RGB pictures were converted to 8-bit gray scale im-192 ages and then analyzed to obtain histograms of digital levels. 193

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Two calibration curves were obtained by measuring solutions with known arsenic concentrations. Then, As concentrations of samples under test conditions were obtained from the digital level of the arsenic strips and the calibration curves developed in this work. Limit of detection (LOD) using this technique was $6.5 \ \mu g/L$. A complete description of this method can be found in Carro Perez and Francisca (2013).

Selected samples were also tested by using gaseous hydride/ atomic absorption spectrometry (GHAA), following the procedure suggested by the USEPA (1999). Obtained results correlate with each other with a coefficient of determination $R^2 = 0.99$ (Carro Perez and Francisca 2013).

Experimental Tests

Batch and soil column tests were performed to evaluate arsenic 207 adsorption in samples A and B. In both cases, tests were carried 208 out at room temperature (20°C). 209 Batch tests were performed by following the ASTM D4646
Standard (ASTM 2007) using a 250-mL flask, 200 mL of arsenic
solutions with concentrations from 0.1–25 mg/L, 20 g of dry soil
particles, and stirring times between 2 and 24 h. After that, the mixture was centrifuged at 4000 rpm for 60 minutes, and the recovered
liquid was analyzed to determine the arsenic concentration.

The soil column tests were performed in transparent cells having 216 217 5 cm in diameter and 5 cm in length (Fig. 3). Laterite-sand mixtures 218 were moistened with distilled water and placed in the cell in three layers of equal height by giving 25 blows per layer with a 219 10.95-mm diameter blunt tip bar. All columns were prepared with 220 221 porosity and dry unit weight equals to 0.3 and 19 kN/m³, respec-222 tively. Two porous stones and Fisherbrand qualitative grade P5 filter papers were placed at the top and bottom of the specimens. 223 224 The sand forms a rigid skeleton containing the finer particles of 225 samples A and B, which create a reactive matrix. These samples 226 were permeated with distilled water by following the constant head 227 technique (ASTM 2007) until obtaining constant hydraulic conduc-228 tivity. Then, the specimens were permeated with a solution of 229 1 mg/L of As without modifying the hydraulic gradient (Fig. 3). 230 The liquid permeated through the samples was collected in the 231 outlet port and the presence of arsenic was determined at different 232 times (or pore volumes of flow) during 150 days. The pore volume 233 of flow (U) is a dimensionless ratio and is computed as the total volume of liquid permeated through the specimen divided by the 234 235 volume of voids. The monitoring of the relationship between the 236 effluent's concentrations measured at different pore volume of flow 237 allowed computing the retardation factor as previously indicated.

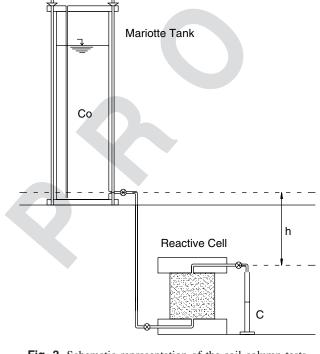
238 Adsorption of As on lateritic soil particles was verified by meas-239 uring the zeta potential of soil particles at different pH conditions. 240 The arsenic concentrations ranged from 1-20 mg/L. The zeta po-241 tential measurements were performed after the sorption/reaction of 242 particles with the arsenic solutions in the batch tests. These measurements were performed by using the Zeta-Meter 3.0+ equip-243 244 ment, which includes a microscope, a voltage generator, a zeta 245 potential meter, and an electrophoretic cell with platinum electro-246 des. The number of particles, zeta potential, standard deviation of the measurements, voltage change, and velocity factor were recorded during the tests.

Results and Analysis

Batch Tests

Removal of arsenic in batch tests was from 95–99% for sample A and 92-99% for sample B. The amount of As adsorbed on soil particles (C^*) showed a nonlinear behavior with the equilibrium concentration (C) for all tested initial As concentrations. Theoretically, the nonlinear Freundlich and Langmuir isotherms models were fitted to the experimental data by using a least square fitting technique (Fig. 4). Table 2 shows the obtained equations. The higher coefficient of determinations were $R^2 = 0.985$ and $R^2 =$ 0.922 for the Freundlich and Langmuir isotherm when fitting experimental results of sample A and B, respectively (Table 2). However, the Langmuir isotherm fitted the experimental results of sample A almost with the same coefficient of determination as the Freundlich model. Then, the use of the Langmuir model is preferred for the two tested residual soils, and therefore, estimated maximum adsorption capacities were 0.295 and 0.262 mg/g for the samples A and B, respectively. These values resulted slightly higher than that determined by Maji et al. (2008) for laterite soil and suggested that tested residual soils can be used for the remediation of As contaminated water. Even tested soils have a low efficiency in removing As in comparison with synthetic materials (Table 3); however, residuals soils have the advantage that they are natural, abundant, and low-cost materials.

The zeta potential at pH higher than the point of zero charge 273 (PZC ~ 3.5) was negative. The obtained values were attributed to the simultaneous contribution of the negative electrical charges of clay particles and the positive electrical charges of the iron oxides in the tested samples. The effect of adsorption on the surface charge was obtained by testing solutions with different initial 278





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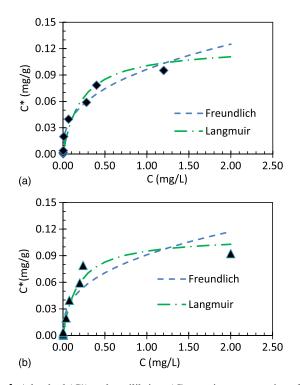


Fig. 4. Adsorbed (C^*) and equilibrium (C) arsenic concentrations fromF4:1batch sorption tests performed with: (a) sample A; (b) sample BF4:2

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Table 2. Modeling Equations for the Fitted Isotherms	Table 2.	Modeling	Equations	for the	Fitted	Isotherms
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		Sample A		Sample B	
T2:2	Model	Equation	R^2	Equation	R^2
T2:3 T2:4	Freundlich Langmuir	$C^* = 0.225C^{0.215}$ $C/C^* = (1/0.887) + (C/0.295)$	0.985 0.962	$C^* = 0.22C^{0.2}$ $C/C^* = (1/0.987) + (C/0.262)$	0.913 0.922

Table 3. Comparison of Maximum Sorption Capacities (C^*_{max}) of Natural
and Synthetic Adsorbents used for the Removal of As from Water

		C^*_{\max}	Arsenic	
8:1	Adsorbent	(mg/g)	type	Reference
3:2	Naturals			
3:3	Sample A	0.295	As(V)	This study
3:4	Sample B	0.262		
3:5	Siderite	0.516	As(V)	Guo et al. (2007)
8:6		1.040	As(III)	
3:7	Algae Lessonia nigrescens	28.2–45.2	As(III)	Hansen et al. (2006)
8:8	Oxisol			
3:9	Goethite	12.4	As(V)	Ladeira et al.
10		7.5	As(III)	(2004)
11	Gibbsite	4.6	As(V)	
12		3.3	As(III)	
13	Kaolinite	0.23	Total	
14	Laterite soil	0.18	Total	Maji et al. (2008)
15	Natural iron ores	0.4	As(V)	Zhang et al. (2004
16	Kaolinite	0.86	As(V)	Mohapatra et al.
17	Montmorillonite	0.64		(2007)
18	Illite	0.52		
19	Zeolite (clinoptilolite)	0.0015	As(V)	Bilici Baskan and Pala (2011)
20	Synthetics			1 414 (2011)
21	Fe ₃ O ₄ nanoparticle-coated	0.96	As(V)	Chen et al. (2011)
	boron nitride nanotubes			
22	Synthetic zeolites	34.8-35.8	As(V)	Chutia et al. (2009
23	Chitosan zero valent iron	94 ± 1.5	As(III)	Gupta et al. (2012
24	Nanoparticles	119 ± 2.6	As(V)	1
25	Bone char	4.00	As(III)	Mlilo et al. (2010
26		4.58	As(V)	
27	Iron oxide-coated sand	0.02857	As(III)	Gupta et al. (2005
28	Iron oxide Fe_2O_3	0.66	As(V)	Jeong et al. (2007
29	Aluminum oxide Al_2O_3	0.17		e 、
30	Nanoscale	1.8	As(III)	Kanel et al. (2005
31	Zero-valent iron			,
32	Granular activated carbon	2.5	As(V)	Di Natale et al. (2008)
33	Iron-treated clinoptilolite	0.008-0.009	As(V)	Bilici Baskan and Pala (2011)
34	Activated carbon oat hulls	3.09	As(V)	Chuang et al. (2005)
35	Amorphous iron(III) phosphate FePO ₄	10	As(V)	Lenoble et al. (2005)
36	Crystalline iron(III) phosphate FePO ₄	9		< /
37	Hydrolyzed acid treated	21.6	As(V)	Maiti et al. (2012)
38	laterite	9.4	As(III)	

279 concentrations of As. In all cases, the obtained z-potential became 280 more negative with the As adsorption given that positive surface 281 charges of the iron oxides were partially balanced by the negative charge of the arsenate $HAsO_4^{2-}$ (Fig. 5). Then, the higher the C^* , the 282 283 more negative the electrical surface charge.

284 The calibrated adsorption isotherms allowed computing the re-285 tardation factor theoretically (Fetter 1993), which can be used for 286 the estimation of the expected behavior of soil columns with differ-287 ent bulk densities. The direct measurement of retardation factor was

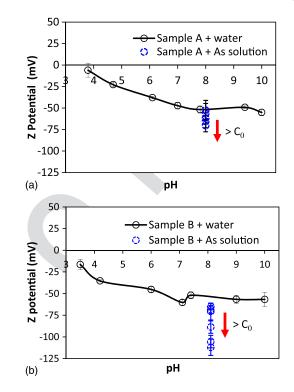


Fig. 5. Z-potential for samples: (a) A; (b) B before and after in contact F5:1 with arsenic solutions; arrows indicate increasing adsorbed arsenic (C^*) F5:2 from 0.004-0.08 mg/g, and error bars corresponds to a confidence interval of 95% F5:4

also preformed to obtain reliable values for long-term tests in permeating soil columns (Sharma and Reddy 2004).

Soil Column Tests

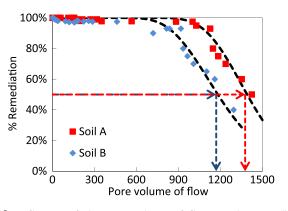
The removal of arsenic (%) was determined by measuring the 291 arsenic concentration of the liquid collected in the outlet port 292 (Fig. 6). Flow rate was equal to 6.48×10^{-6} m/s for the sample 293 A and 5.28×10^{-6} m/s for the sample B. Soil columns were very 294 effective in reducing the arsenic concentrations when the pore volume of flow was lower than 900 and 600 for sample A and B, respectively. Given that porosities were 0.3, the amount of water that can be purified was 270 and 180 times the total volume of the columns, respectively. The As concentration in the effluent showed a removal higher than 98% before the threshold pore volumes of flow; thereafter, remediation efficiency decreased dramatically.

The high remedial efficiency observed during the first days of 302 permeation was produced as a result of arsenic adsorption. Arsenic 303 was retained inside the soil column given that close-to-zero con-304 centrations were measured in the effluent even when the volume 305 of water permeated through the specimens was several times higher 306 than the pore volume. This produced a retardation effect delaying 307 the presence of arsenic in the outlet port. Thus, adsorption clearly 308 prevailed over the advection and diffusion of arsenic ions inside the 309 soil pores. 310

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F6:1 **Fig. 6.** Influence of the pore volume of flow on the remediation F6:2 efficiency

311 Discussion and Practical Application

312 Concentration of arsenic in the outlet port increased with the num-313 ber of pore volume of flow. The influence of pore volume of flow 314 (U) on the final concentration (C) experimentally measured was successfully modeled by Eq. (4) by using a least-squares fitting 315 316 technique (dashed lines in Fig. 6). The soil hydraulic conductivity, 317 porosity, and cell dimensions were included as experimentally de-318 termined in the soil column tests. The model parameters that better 319 fitted the experimental results obtained for the sample A were hydrodynamic dispersion coefficient $D_L^* = 3.7 \times 10^{-12} \text{ (m}^2/\text{s)}$ and 320 retardation coefficient R = 1,377, while for sample B they were 321 $D_L^* = 6.5 \times 10^{-12} \text{ (m}^2/\text{s)}$ and R = 1,170. 322

323 Obtained results confirms that the sample with higher iron content (sample A) identified in the EDX analysis has a higher 324 325 maximum adsorption capacity (Tables 1 and 2). This trend is in agreement with the higher retardation factor obtained for sample 326 327 A in comparison with sample B (Fig. 6). In addition, the internal 328 redistribution of As caused by spatial distribution of redox gradients may also be responsible for this observation (Masue-Slowey 329 330 et al. 2011).

The flow rate, which is controlled by the hydraulic conductivity 331 332 and gradient, and the initial arsenic concentration determined the 333 time of As percolation through soil columns or permeable reactive 334 barriers. The lifetime of the permeable reactive filters is defined as 335 time of permeation required to observe concentrations higher than 336 0.01 mg/L in the outflow, if the water is been used for drinking (WHO 2006). Lifetime can be obtained from the pore volume 337 338 of flow, hydraulic gradient, barrier thickness, and Eq. (4). Fig. 7 339 shows that the lower the initial concentration and gradient, the 340 larger the number of pore volumes of flow needed to reach arsenic 341 concentrations higher than 0.01 mg/L in the outflow when assum-342 ing null changes in porosity and hydrodynamic dispersion.

Initial concentration and hydraulic gradient were the two fun damental parameters for the design of permeable reactive filters
 given that they control the lifetime and the volumetric flow rate.

346 At high As concentration (e.g., $C_0 > 0.1 \text{ mg/L}$, one order of 347 magnitude higher than the allowed concentration for drinking 348 water), the main factor controlling the lifetime of reactive soil col-349 umns was the hydraulic gradient or seepage velocity. The modeling of soil barriers 0.1 m in length, initial concentration $C_0 = 1 \text{ mg/L}$, 350 and hydraulic gradient i = 0.01 showed that As concentrations in 351 the effluent were lower than 0.01 mg/L during more than 2,800 352 353 and 1,600 days for samples A and B, respectively. Then, these 354 materials can be used for the remediation of aquifers by means of 355 permeable reactive barriers. However, lifetime reduces significantly

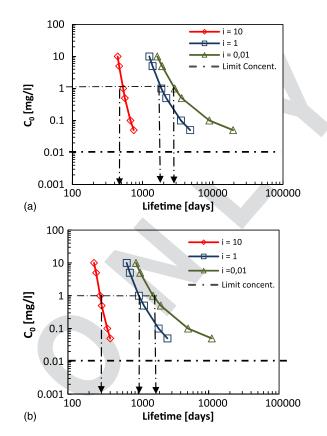


Fig. 7. Influence of the arsenic initial concentration (C_0) and hydraulicF7:1gradient (i) on the lifetime of permeable reactive soil columns:F7:2(a) sand-sample A mixture; (b) sand-sample B mixtureF7:3

when the hydraulic gradient increases, as in the case of filters in water purification systems (Fig. 7).

At very low As concentration ($C_0 < 0.1 \text{ mg/L}$), the initial concentration has higher influence on lifetime than seepage velocity. In addition, regardless the hydraulic gradient, the lower the As concentration in the permeating liquid, the higher the lifetime of the reactive columns. At the limit, when $C_0 < 0.01 \text{ mg/L}$, the expected lifetime was extremely long.

The higher maximum adsorption capacity of the lateritic sample 364 A with respect to the lateritic sample B was associated with the 365 higher amount of Fe (%) forming oxides and higher amount of 366 particles less than 2 μ m (clay size). The lateritic sample A contains 367 Fe: 5.47% (w/w) and particles < 2 μ m = 75%, while sample B 368 contains only Fe: 2.98% (w/w) and particles $<2 \mu m = 66\%$ 369 (Table 1). Considering the minerals encountered in these samples 370 of soils, the presence of hematite and goethite in samples A and B, 371 respectively, is responsible for the adsorption and removal of As 372 from the permeating liquid. Therefore, the higher the amount of 373 Fe (%), the higher the lifetime of permeable reactive filters as 374 observed from the comparison of Figs. 7(a and b). 375

Summary and Conclusions

Lateritic soils from the north of Argentina were very effective in
removing arsenic in batch and soil column tests. Obtained results377showed that this geomaterial can be used for the developing of
alternative techniques for the remediation of arsenic contaminated
groundwater.380

More than 90% of arsenic removal was obtained in all batch 382 tests. Inorganic As moved from aqueous solutions to the solid 383

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phase by means of adsorption mechanisms that were successfully
predicted by means of isotherm adsorption models. This observation was verified by measuring changes in the z-potential of the soil
particles associated to the arsenic adsorption.

The Langmuir isotherm model well represented the experimental results obtained in this research with coefficient of determinations higher than $R^2 = 0.92$. The maximum adsorption capacity according to Langmuir equation resulted in the range of 0.262-0.295 mg/g.

Removal of As in reactive soil columns of laterite-sand mixtures reached values as high as 95–98% of the initial concentration. From the calibration of the mass transport equation, the longitudinal hydrodynamic dispersion coefficient and retardation factor resulted $D_L^* = 3.7 \times 10^{-12} \text{ (m}^2/\text{s)}$ and R = 1,377 for the sample A and $D_L^* = 6.5 \times 10^{-12} \text{ (m}^2/\text{s)}$ and R = 1,170 for the sample B.

The initial concentration and hydraulic gradient had a signifi-399 400 cant effect on the lifetime of soil columns and permeable reactive 401 filters (until the As percolates). The effect of seepage velocity pre-402 vailed over the initial concentration when water contains high As levels. However, if initial concentration was lower than 0.03 mg/L, 403 404 the influence of seepage velocity became of less importance, and 405 the time required for the percolation of As became extremely long. 406 These results confirm natural residual soils from the north of Argentina can be successfully used for the removal of As from 407 408 water by means of low-cost reactive filters when the influence of 409 competing ions can be neglected.

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