Friction factor for turbulent flow in rough pipes from Heisenberg's closure hypothesis

Esteban Calzetta

Departamento de Fisica and CONICET, FCEN Universidad de Buenos Aires, Ciudad Universitaria, 1428 Buenos Aires, Argentina (Received 9 January 2009; revised manuscript received 11 March 2009; published 22 May 2009)

We show that the main results of the analysis of the friction factor for turbulent pipe flow reported by Gioia and Chakraborty [Phys. Rev. Lett. **96**, 044502 (2006)] can be recovered by assuming the Heisenberg closure hypothesis for the turbulent spectrum. This highlights the structural features of the turbulent spectrum underlying the analysis of Gioia and Chakraborty.

DOI: 10.1103/PhysRevE.79.056311 PACS number(s): 47.27.em, 47.27.nf

I. INTRODUCTION

The accurate prediction of the friction factor for the turbulent flow of an incompressible fluid through a straight pipe of constant circular section is a matter of huge importance, both practical and fundamental [1–3]. Not surprisingly, it has been the subject of careful measurement [1,4]. There is also an array of empirical formulas to predict the friction factor in concrete situations [5,6], culminating with the sheer rendition of Nikuradse's experimental results in analytical form provided by Yang and Joseph [7]. However, the theoretical link between the phenomenological formulas and the experimental results is weak. In particular, some of the most used empirical formulas, such as Colebrook's, erase most of the structure seen in experiment.

In these circumstances, the derivation of several of the key features of the dependence of the friction factor with respect to Reynolds number for a given pipe roughness from a concrete theoretical model in [8] [henceforth called Gioia-Chakraborty (GC)] is undoubtedly an important step forward. For some background and further developments on the GC model [8] see [9–13]. The analysis by Gioia and Chakraborty [8] departs in important aspects from the view of the problem laid down by pioneers such as Prandtl and von Karman [1] and the classic textbook formulation by Landau and Lifshitz [14]. Therefore it is important to understand what are the fundamental elements underlying the success of the GC model.

Several key features of the Reynolds number dependence of the friction factor, namely, the bellies and the Strickler's regime (see Ref. [8]), can be regained if the GC analysis is combined with Heisenberg's closure hypothesis [15–17] for the turbulent spectrum. The Heisenberg theory is not generally regarded as a realistic depiction of fully developed turbulence [18,19]. Therefore, the fact that the GC analysis works even if the, at best, qualitatively correct Heisenberg theory is used instead of an (not yet known) exact turbulent spectrum gives us a new perspective on the inner working of the GC model.

This paper is organized as follows. Section II is of a review nature and presents the basic facts and definitions concerning the friction factor and the GC treatment thereof. Section III presents the Heisenberg closure hypothesis and derives the GC friction factor for this form of the spectrum. We conclude with a final appraisal of the GC friction factor formula.

II. PRELIMINARIES

A. Definitions

The goal of this section is just to put together a basic theoretical description of the Reynolds number dependence of the friction factor. Therefore we shall consider only the simplest case of a single phase incompressible fluid moving within a horizontal pipe. The section of the pipe is circular and the radius is R. We assume the flow is well developed, meaning that there is a well-defined macroscopic velocity V at every point (we shall use boldface for vector quantities). V depends only on the radial coordinate r, points in the axial direction x, and vanishes at the boundary: $V = v(r)\hat{x}$ and v(R) = 0. V is automatically divergenceless and obeys the momentum balance equations, which, written in cylindrical coordinates, are

$$\frac{\partial p}{\partial x} = \frac{1}{r} \frac{\partial}{\partial r} r \tau^{rx},\tag{1}$$

$$\frac{\partial p}{\partial r} = \frac{1}{r} \frac{\partial}{\partial r} r \tau^{rr},\tag{2}$$

where p is the pressure and τ is the stress tensor. Since the right-hand side (RHS) of Eq. (2) depends only on r, we assume that the pressure drop $\partial p/\partial x$ must be r independent. Equation (1) can be integrated (with a boundary condition imposed by regularity),

$$\tau \equiv \tau^{rx} = \frac{r}{2} \frac{\partial p}{\partial x} \equiv -\tau_0 \left(\frac{r}{R}\right),\tag{3}$$

where τ_0 is the stress at the wall. This means that to know the stress on the wall it is enough to find the stress anywhere since it obeys a simple scaling law.

Another important quantity is the average flow Q. Together with the mass density ρ and the cross surface $A = \pi R^2$ it defines the mean velocity V according to $Q = \rho AV$. The fluid is characterized by a molecular (dynamic) shear viscosity μ , (kinematic) $\nu = \mu/\rho$. With these quantities we may construct the most important dimensionless number, namely, Reynolds',

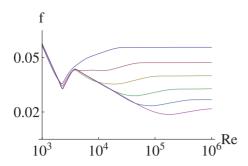


FIG. 1. (Color online) Analytic reconstruction of Nikuradse's data, as given in [7], extrapolated to the range up to Re=10⁶, actually covered in the Princeton superpipe experiment. The six lines correspond, from the bottom up, to ϵ^{-1} =507, 252, 126, 60, 30.6, and 15. Both scales are logarithmic.

$$Re = \frac{2RV}{\nu}.$$
 (4)

These scales allow us to construct an energy density scale $\epsilon = \rho V^2$. The Darcy-Weisbach formula introduces the friction factor f from the ratio of τ_0 to ϵ ,

$$\tau_0 \equiv \frac{f}{8}\rho V^2. \tag{5}$$

Our main goal is to find a relationship between f and Re.

B. Main flow regimes

In this section we shall describe the main flow regimes and the corresponding empirical formulas. We shall use as reference Nikuradse's experimental results. For practical reasons, we do not mean the actual results but rather analytical rendering of Yang and Joseph [7] thereof.

For a rough pipe the friction factor does not decrease indefinitely with increasing Reynolds number but rather converges to a finite value f_{∞} . This allows us to define a parameter $\delta_{\infty} \equiv \epsilon R$ from the condition that

$$\frac{1}{\sqrt{f_{\infty}}} = -0.868 \ln \left[\frac{\epsilon}{7.48} \right]. \tag{6}$$

We shall use this parameter to identify the several series of data from the Nikuradse experiment.

Figure 1 gives an overall impression of the data. Each curve shows a rich structure. For example, let us consider the curve corresponding to ϵ^{-1} =126 (Fig. 2). The log-log plot is essentially linear to the left of A. This corresponds to the laminar flow; at A, we have Re \sim 2000. Then there is a maximum (the so-called hump) at B, corresponding to Re \sim 4000. The log-log plot is again essentially linear up to the belly at C (Re \sim 40 000). To the right of C, the curve approaches its asymptotic value from below. The approach is very fast; beyond the point D (Re \sim 200 000) the friction factor is constant for all practical purposes [7]

We shall now review two basic regimes in this complex behavior, namely, the laminar regime, to the left of A, and the Blasius regime, from the hump B to the belly C.

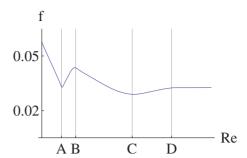


FIG. 2. (Color online) A close up of the curve corresponding to ϵ^{-1} =126. Observe the sharp minimum at A, the hump at B, and the belly at C. To the right of D the friction factor is constant.

1. Laminar regime

If the flow is laminar, the bulk velocity profile can be solved exactly and the friction factor results,

$$f_{\text{laminar}} = \frac{64}{\text{Re}}. (7)$$

In Fig. 3 we superimpose the plot of the friction factor for laminar flow [Eq. (7)] to Nikuradse's data as given in Fig. 1. We can see that the agreement is outstanding up to Reynolds numbers of a few thousands.

2. Blasius regime

One of the oldest and most accurate empirical formulas for the friction factor is Blasius',

$$f_{\text{Blasius}} = \frac{0.3164}{\text{Re}^{1/4}}.$$
 (8)

We plot this expression superimposed to Nikuradse's data in Fig. 4.

C. GC model

In this section we shall analyze the proposal by Gioia and Chakraborty [8]. Our aim is to contrast it with the experimental situation as described above.

The basic framework of the GC model is that for high enough Reynolds number the pipe is filled with a well developed turbulent flow which can be accurately described by Kolmogorov's K41 theory. It is therefore characterized by

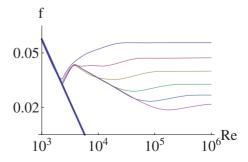


FIG. 3. (Color online) A comparison of the friction factor for laminar flow [Eq. (7)] (thick line) against Nikuradse's data as given in Fig. 1.

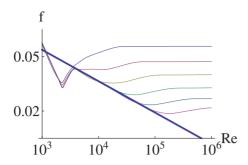


FIG. 4. (Color online) A comparison of Blasius' friction factor Eq. (8) (thick line) against Nikuradse's data as given in Fig. 1.

large velocity and length scales U_{GC} and L_{GC} . On scales l smaller than L_{GC} , the turbulent speed follows Kolmogorov scaling $u_{GC}(l) = U_{GC}(l/L_{GC})^{1/3}$ (except for small corrections to be discussed below). GC identify $L_{GC} = R$ as the pipe radius. Concerning the macroscopic flow velocity, GC assume $U_{GC} = \kappa_u V$, where V is the mean flow velocity and κ_u is a Re-independent constant (eventually Gioia and Chakraborty [8] choose $\kappa_u = 0.036$).

The detailed mechanisms of momentum transfer between the flow and the wall are rather complex [20]. Gioia and Chakraborty [8] assumed that the transfer is mainly effected by eddies of size δ_{GC} . These eddies carry a momentum ρU_{GC} along the wall. The transverse velocity u_{GC}^0 is the turbulent speed associated with the scale δ_{GC} .

$$u_{GC}^{0}(\delta_{GC}) = U_{GC}(\delta_{GC}/L_{GC})^{1/3}.$$
 (9)

The stress at the wall is $\tau_0 = \kappa_{\pi} \rho U_{GC} u_{GC}^0$ with some universal constant κ_T . Since τ_0 is linear on u_{GC}^0 , in the Blasius regime $\delta_{GC} \propto \mathrm{Re}^{-3/4}$. This is the same scaling as Kolmogorov's viscous length scale η . $\eta = R/\mathrm{Re}^{-3/4}$ is the scale at which viscous dissipation matches turbulent energy transport (Gioia and Chakraborty [8] actually interposed another dimensionless constant b=11.4 in the definition of η , and we prefer to absorb it into the many more constants to come). Therefore it becomes natural to assume $\delta_{GC} = a \eta$, where a is yet another universal dimensionless constant. The friction factor reads

$$f = \frac{8\kappa_{\tau}\kappa_{u}^{2}a^{1/3}}{\text{Re}^{1/4}}F[\text{Re}],$$
 (10)

where

$$F[\text{Re}] = \frac{\text{Re}^{1/4}}{\kappa_{c} a^{1/3} V} u_{GC}^{0}.$$
 (11)

At the level of approximation we have stayed so far, F = 1. If we choose $8\kappa_\tau \kappa_u^2 a^{1/3} = 0.3164$, then the model is built to reproduce Blasius' law for smooth pipes. This can be criticized on the grounds that it does not account for the deviations from the Blasius' law at very high Reynolds number predicted by the Colebrook equation and apparently verified by the Princeton superpipe [4]. However, these criticisms can be swept away by noting that no physical pipe can be absolutely smooth. So the real issue is how to introduce roughness into the model.

The way to modify the asymptotic behavior of the friction factor to account for pipe roughness is that the scale δ_{GC} does not decrease indefinitely with growing Reynolds number but rather stabilizes at a value $\epsilon_{GC}R$. We therefore find $f_{\infty} \propto \epsilon_{GC}^{1/3}$.

If we identify ϵ_{GC} with the parameter ϵ in Eq. (6), then this result is the so-called Strickler law. This approximate scaling was known long before the GC work, and the fact that it is so effortlessly obtained is quite remarkable.

1. Belly and Blasius regime

For finite Reynolds number, we may imagine that $\delta_{GC} = \epsilon_{GC}R + a \eta$. That is, the width of the dominant eddies at finite Reynolds number is just the sum of the widths defined by the pipe roughness and by the viscous scale. However, if the stress at the wall is defined by the turbulent velocity at δ_{GC} , and this in turn decays to $\epsilon_{GC}R$ with increasing Reynolds number, then Kolmogorov scaling implies that the friction factor reaches its asymptotic value *from above*, as in the Colebrook equation [5]. To recover the belly in Nikuradse's data (cf. Figs. 1 and 2) we need that the velocity at an essentially fixed scale $\epsilon_{GC}R$ be an *increasing* function of Re at least for large enough Reynolds number.

The basic idea is that the mean square velocity at some scale δ is the sum of contributions from eddies at all scales $k^{-1} < \delta$.

$$u^{2}[\delta] = \int_{\delta^{-1}}^{\infty} dk \mathcal{E}[k]$$
 (12)

and f is proportional to $(u^2[\delta])^{1/2}$. If the only dependence on Reynolds number was through δ , then we would obtain

$$\frac{df}{d\text{Re}} = \frac{f}{2u^2 [\delta]} \frac{\mathcal{E}[\delta^{-1}]}{\delta^2} \frac{d\delta}{d\text{Re}} < 0.$$
 (13)

Therefore the friction factor would be a monotonic function of Reynolds number. To get the feature of the belly in the friction factor we have to allow for a direct dependence of the spectrum on Reynolds number, leading to the proper result

$$\frac{df}{d\text{Re}} = \frac{f}{2u^2[\delta]} \left\{ \int_{\delta^{-1}}^{\infty} dk \frac{\partial \mathcal{E}[k]}{\partial \text{Re}} + \frac{\mathcal{E}[\delta^{-1}]}{\delta^2} \frac{d\delta}{d\text{Re}} \right\}$$
(14)

The derivative does not have a definite sign.

As a matter of fact, this sort of behavior is a prediction of K41 theory for finite Reynolds number. For large but finite Reynolds number, we have

$$\mathcal{E}[k] = \frac{3U_{GC}^2}{2R^{2/3}} \frac{1}{k^{5/3}} E[\beta k \eta], \tag{15}$$

where E is a nonincreasing function such that E[0]=1 and $E[\infty]=0$. Thus in the limit of infinite Reynolds number $\eta\mapsto 0$ we recover the one-third scaling law [Eq. (9)]. We have added the (yet another) dimensionless constant β for latter convenience. Neither β nor the form of E more generally is prescribed by K41 theory[21]. This is precisely the point where adoption of the Heisenberg closure hypothesis (or any other, see [22]) makes a difference.

We observe that inclusion of the $E[\beta k \eta]$ factor enforces a decay faster than -5/3 in the dissipative range. In any case, we now have

$$\frac{\partial \mathcal{E}[k]}{\partial \text{Re}} = \frac{3}{4} \frac{3U_{GC}^2}{2R^{2/3}} \frac{1}{k^{2/3}} \frac{\beta \eta}{\text{Re}} (-E'[\beta k \eta]) > 0.$$
 (16)

So the derivative in Eq. (14) may be positive in the appropriate range.

We can derive a more explicit result. Using Eq. (15) into Eq. (12) and calling $x = \beta k \eta$ we get, after an integration by parts,

$$u^{2}[\delta] = U_{GC}^{2} \left\{ \left(\frac{\delta}{R} \right)^{2/3} E \left[\frac{\beta \eta}{\delta} \right] - \left(\frac{\beta \eta}{R} \right)^{2/3} \int_{\beta \eta/\delta}^{\infty} \frac{dx}{x^{2/3}} (-E'[x]) \right\}. \tag{17}$$

If we use Eq. (17) to evaluate u at the scale $\delta_{GC} = \epsilon_{GC}R + a \eta$, we clearly see the two asymptotic regimes. For large Reynolds number, $\eta \mapsto 0$, $\delta_{GC} \mapsto \epsilon_{GC}R$, and $u = U_{GC}\epsilon_{GC}^{1/3}$ or, retaining first-order corrections,

$$u = U_{GC} \epsilon_{GC}^{1/3} \left\{ 1 - \frac{B}{\sqrt{\text{Re}}} \right\}$$
 (18)

provided $E[\beta \eta/\delta] = 1 + o(\eta^{2/3})$, where the constant B depends on the shape of the function E as well as on a, ϵ_{GC} , and β ,

$$B = \frac{1}{2} \left(\frac{\beta}{\epsilon_{GC}} \right)^{2/3} \int_{0}^{\infty} \frac{dx}{x^{2/3}} (-E'[x]). \tag{19}$$

In the limit where $a \eta \gg \epsilon_{GC} R$ we get instead

$$u^{2}[a\eta] = U_{GC}^{2} \left(\frac{a\eta}{R}\right)^{2/3} \left\{ E\left[\frac{\beta}{a}\right] - \left(\frac{\beta}{a}\right)^{2/3} \int_{\beta/a}^{\infty} \frac{dx}{x^{2/3}} (-E'[x]) \right\}$$
(20)

and so we recover Blasius' law with a new constant (unless $\beta/a \le 1$). Of course this new factor can be easily absorbed in any of the several dimensionless constants at our disposal.

This qualitative success is not easily transformed into a quantitative fit, however. Generally speaking, to get the fast approach to the asymptotic value characteristic of Ni-kuradse's data, very small values of β are preferred. But then the Blasius regime appears in a range of Reynolds numbers much below the experimentally observed. In any case, we have not yet accounted for the hump. We shall defer further quantitative analysis until we incorporate the hump into the GC model.

2. Hump

As we have seen, the behavior of the friction factor for Reynolds numbers over a few thousands, according to Gioia and Chakraborty [8], is the result of the competition of two opposite processes. On one hand, higher Reynolds numbers mean higher lower limits in integral [Eq. (12)], thus bringing the friction factor down. On the other, the integrand in Eq.

(12), as defined in Eq. (15), increases pointwise with Reynolds number, thus bringing the friction factor up. The first process dominates in the Blasius regime and the second dominates in the climb up to the asymptotic value.

To set a lower limit to the Blasius region, therefore, the simplest is to cut off the integral in 12, so that it becomes insensitive to the lower limit if this is low enough. The first process then becomes moot, while the second is still operative, and we get a friction factor which grows with Reynolds number.

We may mention that this second modification of the spectrum is totally outside K41 theory. Also that in a certain way it works too well since the laminar regime is obliterated.

In summary, Gioia and Chakraborty [8] proposed the form of the spectrum [cf. Eq. (15)],

$$\mathcal{E}[k] = \frac{3U_{GC}^2}{2R^{2/3}} \frac{1}{k^{5/3}} E[\beta k \, \eta] D[kR], \tag{21}$$

where

$$E[x] = e^{-x}, (22)$$

$$D[x] = \frac{x^{17/3}}{[x^2 + \gamma]^{17/6}},$$
(23)

and γ is a dimensionless constant. Introducing a dimensionless integration variable $x = \beta k \eta$ the friction factor may be reduced to the form

$$f = \frac{C}{\text{Re}^{1/4}} \left\{ \int_{h[\text{Re}]}^{\infty} dx \frac{x^4 e^{-x}}{[x^2 + g[\text{Re}]]^{17/6}} \right\}^{1/2}, \tag{24}$$

where

$$h[\text{Re}] = \frac{\beta}{a + \epsilon_{GC} \text{Re}^{3/4}},$$
 (25)

$$g[Re] = \frac{\gamma \beta^2}{Re^{3/2}}.$$
 (26)

In Fig. 5 we show a typical plot of Eq. (24), corresponding to the data for ϵ =1/126. We have extrapolated the experimental data up to Re=10¹⁰ to better appreciate the convergence to the asymptotic value. For this plot, we have chosen β/a =0.5 and $\gamma\beta^2$ =10⁴. The values of the constant C and of ϵ_{GC} were chosen to enforce the Blasius law at the value of Re=4000 and the proper asymptotic limit.

This plot represents a near optimal situation; for example, higher values of γ erase the features of the curve, while for lower values the hump disappears. Although there is a resemblance to the experimental data, it is not truly quantitatively accurate; in particular, the theoretical prediction is much smoother than the experimental plot.

III. GC MODEL BASED ON HEISENBERG CLOSURE

In this section we shall use the Heisenberg closure to derive the form of the spectrum in Eq. (12), thereby obtaining an expression for the friction factor with higher predic-

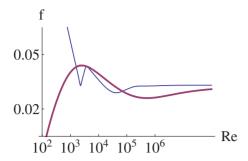


FIG. 5. (Color online) Log-Log plot of the friction factor from Eq. (24), compared to the data for ϵ =1/126. The thick line corresponds to the GC model; the thin line corresponds to the data. We have extrapolated the experimental data down to Re=10² and up to Re=10¹⁰ to better appreciate the convergence to the asymptotic values. For this plot, we have chosen β/a =0.5 and $\gamma\beta^2$ =10⁴. The values of the constant C and of ϵ_{GC} were chosen to enforce the Blasius law at the value of Re=4000 and the proper asymptotic limit.

tive power than the original GC proposal. We consider this as a toy model to test whether a turbulent spectrum based on a definite hypothesis regarding the underlying dynamics can make a difference in the accuracy of a model built along the general lines of the GC approach [23].

Heisenberg closure in the presence of boundaries

The basic idea of Heisenberg closure is that in fully developed turbulent flow the sum of the energy dissipated by viscosity and the energy transported to smaller eddies remains the same in all scales. At a given scale k_0 , the energy dissipated through viscosity is

$$Q_{\nu}[k_0] = 2\nu \langle \nabla u^2 \rangle [k_0], \qquad (27)$$

where

$$\langle \nabla u^2 \rangle [k_0] = \int^{k_0} dk k^2 \mathcal{E}[k]. \tag{28}$$

Heisenberg assumed that the energy transported by turbulence may be written as

$$Q_{turb}[k_0] = 2\nu_{turb}[k_0]\langle \nabla u^2 \rangle [k_0], \qquad (29)$$

where on dimensional grounds

$$\nu_{turb}[k_0] = A \int_{k_0}^{\infty} dk \sqrt{\frac{\mathcal{E}[k]}{k^3}}, \qquad (30)$$

where A is a dimensionless constant. The basic assumption is thus

$$Q_{\nu}[k_0] + Q_{turb}[k_0] = Q_{tot}, \tag{31}$$

independent of k_0 . If $\mathcal{E}[k] \propto k^{\alpha}$ when $k \mapsto 0$, then $\langle \nabla u^2 \rangle [k_0]$ scales as $k_0^{\alpha+3}$ while ν_{turb} scales as $k_0^{\alpha/2-1/2}$, so we must have $\alpha=-5/3$. This means that the kinetic energy increases indefinitely with eddy size, which is incompatible with the presence of the pipe. We therefore adopt the modification suggested by Parker [24], namely, we replace $\langle \nabla u^2 \rangle [k_0]$ in Eqs. (27) and (29) by

$$\langle \nabla u^2 \rangle_R[k_0] = \int^{k_0} dk (k^2 + K^2) \mathcal{E}[k], \tag{32}$$

where $K \approx R^{-1}$. The new term accounts for the increase in dissipation due to eddy deformation. Our power counting argument now gives $\alpha = -1/3$, so that the total kinetic energy in the flow is finite.

The starting point is then the balance equation

$$\{\nu + \nu_{turb}[k]\} 2\langle \nabla u^2 \rangle_R[k] = Q_{tot}. \tag{33}$$

A derivative of Eq. (33) gives

$$\frac{Q_{tot}}{\langle \nabla u^2 \rangle_R} \frac{d}{dk} \langle \nabla u^2 \rangle_R - \langle \nabla u^2 \rangle_R \frac{2A}{k^{3/2}} \sqrt{\mathcal{E}} = 0$$
 (34)

and also

$$\mathcal{E} = \frac{1}{k^2 + K^2} \frac{d}{dk} \langle \nabla u^2 \rangle_R, \tag{35}$$

so if $\xi = k^2$,

$$\frac{d}{d\xi} \langle \nabla u^2 \rangle_R^{-3} = \frac{-6A}{Q_{tot}^2} \frac{1}{\xi^2} \frac{1}{\xi + K^2},\tag{36}$$

we read the boundary condition off [Eq. (31)],

$$\langle \nabla u^2 \rangle_R^{-3} = \frac{8 \, \nu^3}{Q_{tot}^3} + \frac{6A}{K^2 Q_{tot}^2} \left\{ \frac{1}{k^2} - \frac{1}{K^2} \ln \left[1 + \frac{K^2}{k^2} \right] \right\} \tag{37}$$

and then, from Eq. (35), we get the spectrum from a simple derivative,

$$\mathcal{E} = \frac{1}{k^3 (k^2 + K^2)^2} \frac{4A}{Q_{tot}^2} \times \left\{ \frac{8 \nu^3}{Q_{tot}^3} + \frac{6A}{K^2 Q_{tot}^2} \left[\frac{1}{k^2} - \frac{1}{K^2} \ln \left(1 + \frac{K^2}{k^2} \right) \right] \right\}^{-4/3}.$$
(38)

We adopt units where $K=R^{-1}=1$. In these units, $Q_{tot}=V^3$ and $\nu=2V/\text{Re}$. Introducing

$$K_s \approx \left(\frac{3A}{4}\right)^{1/4} \frac{\text{Re}^{3/4}}{2} \equiv \left(\frac{\text{Re}}{\text{Re}_c}\right)^{3/4},$$
 (39)

then the spectrum can be rewritten as

$$\mathcal{E} = \text{constant } \frac{2}{3} \frac{1}{k^3 (k^2 + 1)^2} \left\{ \frac{1}{K_s^4} + 2 \left[\frac{1}{k^2} - \ln \left(1 + \frac{1}{k^2} \right) \right] \right\}^{-4/3}.$$
(40)

To obtain the friction factor, we need to integrate the spectrum from a lower scale K_0 up to infinity, where

$$K_0 = \frac{K_s}{(\epsilon_{Hei}K_s + a_{Hei})}. (41)$$

After identifying $K_s = 1/\eta$, this lower limit is the same as in the GC approach.

Observe that the spectrum 40 behaves as $k^{-5/3}$ in the inertial range. It displays a faster decay Re^4k^{-7} in the dissipative range. It therefore satisfies the criteria discussed in Ref. [8] and in Sec. III for reproducing the Blasius and Strickler

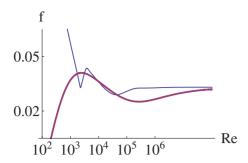


FIG. 6. (Color online) Log-Log plot of the friction factor as computed from the form 40 of the spectrum, compared to the data for ϵ =1/126. The Heisenberg model prediction is the thick line; the experimental values are the thin line. We have extrapolated the experimental data down to Re=10² and up to Re=10¹⁰ to better appreciate the convergence to the asymptotic value. For this plot, we have chosen a=1.25, ϵ_{Hei} =1/126, and Re $_c$ =1000. The overall constant is determined by fitting the theoretical value for f at infinitely large Reynolds number to the experimental asymptotic value.

scaling, as well as the belly feature in the friction factor plot.

To compare the performance of the model based on Heisenberg closure with the results from the original GC proposal, we shall seek an optimal fit to the Nikuradse data for ϵ =1/126. In all, we have four parameters Re_c, a_{Hei} , ϵ_{Hei} and an overall normalization at our disposal. To reduce parameter space, we shall assume ϵ_{Hei} =1/126 as well. The overall constant is determined by asking for a good fit for very large Reynolds number. Changes in Re_c induce rigid horizontal shifts in the plot, so a is the parameter which controls the shape of the curve. The best fit is obtained for a=1.25, which is physically acceptable. We show the result in Fig. 6

We see that the Heisenberg closure leads to an expression which is as successful as the GC model in describing the Blasius regime and the approach to the asymptotic limit. This is clearly displayed in Fig. 7, which is simply the superposition of Figs. 5 and 6.

IV. FINAL REMARKS

The GC proposal is striking in that it offers a simple explanation for the ups and downs of the plot of the friction factor against Reynolds number.

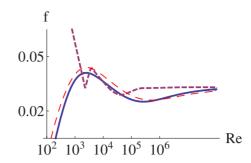


FIG. 7. (Color online) The plots of Figs. 5 and 6 combined. The experimental data correspond to the short dashes, the GC model is the long dashes, and the Heisenberg closure is the full line. There is essentially no difference between both theoretical models up to the highest Reynolds numbers.

In this note we have combined the main GC postulates with a spectrum derived from Heisenberg closure. The result fits the Nikuradse data as well as the original GC analysis. This is good news for the GC model in that it underlines the fact that the model is built on generic features rather than detailed dynamical characteristics of the flow. However, it is also problematic because Heisenberg closure is not generally regarded as realistic, especially in the dissipative range.

Both in the original and the Heisenberg closure model, moreover, it is clear that the quality of the final fit depends on the careful tuning of the many available parameters.

Our conclusion is that to make progress in understanding the friction factor of turbulent pipe flow along the direction pioneered by Gioia and Chakraborty [8] we do not need to worry about a more accurate spectrum shape but rather to provide a solid foundation for the basic assumptions of the GC analysis.

ACKNOWLEDGMENTS

We wish to thank Jose Lanziani, Salvador Gil, and Pablo Mininni for discussions and pointing Ref. [5] to us. This work was supported by University of Buenos Aires, CONICET, and ANPCyT.

^[1] H. Schlichting, *Boundary Layer Theory* (McGraw-Hill, New York, 1950).

^[2] A. S. Monin and A. M. Yaglom, Statistical Fluid Mechanics (MIT, Boston, 1971).

^[3] S. B. Pope, *Turbulent Flows* (Cambridge University Press, London, 2000).

^[4] B. J. McKeon, M. V. Zagarola, and A. J. Smits, J. Fluid Mech. 538, 429 (2005).

^[5] G. O. Cordero, Seventh Annual Meeting of the SPE International Argentine Petroleum Section Grupo de Interes en Modelado y Operacion de Redes y Ductos (unpublished).

^[6] N. Afzal and A. Seena, J. Fluids Eng. 129, 80 (2007).

^[7] B. H. Yang and D. Joseph, J. Turbul. 10, N11 (2009).

^[8] G. Gioia and P. Chakraborty, Phys. Rev. Lett. **96**, 044502 (2006).

^[9] G. Gioia and F. A. Bombardelli, Phys. Rev. Lett. 88, 014501 (2001).

^[10] G. Gioia, P. Chakraborty, and F. A. Bombardelli, Phys. Fluids 18, 038107 (2006).

^[11] N. Goldenfeld, Phys. Rev. Lett. 96, 044503 (2006).

^[12] M. Mehrafarin and N. Pourtolami, Phys. Rev. E 77, 055304(R) (2008).

^[13] N. Guttenberg and N. Goldenfeld, e-print arXiv:0808.1451.

^[14] L. D. Landau and E. M. Lifshitz, Fluid Mechanics (Pergamon,

- Oxford, 1987).
- [15] W. Heisenberg, Proc. R. Soc. London, Ser. A 195, 402 (1948).
- [16] S. Chandrasekhar, Proc. R. Soc. London, Ser. A **200**, 20 (1949)
- [17] M. Grana and E. Calzetta, Phys. Rev. D 65, 063522 (2002).
- [18] G. K. Batchelor, *The Theory of Homogeneous Turbulence* (Cambridge University Press, Cambridge, 1953).
- [19] J. O. Hinze, *Turbulence* (McGraw-Hill, New York, 1975).
- [20] A. A. Townsend, The Structure of Turbulent Shear Flow (Cam-

- bridge University Press, London, 1976).
- [21] A. Yaglom, in *New Trends in Turbulence Theory, Les Houches Course LXXIV*, edited by M. Lesieur, A. Yaglom, and F. David (Springer, Berlin, 2001).
- [22] V. S. L'vov, I. Procaccia, and O. Rudenko, Phys. Rev. Lett. 100, 054504 (2008).
- [23] C.-M. Tchen, Phys. Rev. 93, 4 (1954).
- [24] E. Parker, Phys. Rev. 90, 221 (1953).