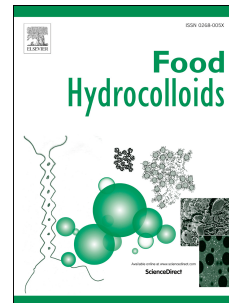


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Production of soy protein concentrate with the recovery of bioactive compounds:
From destruction to valorization

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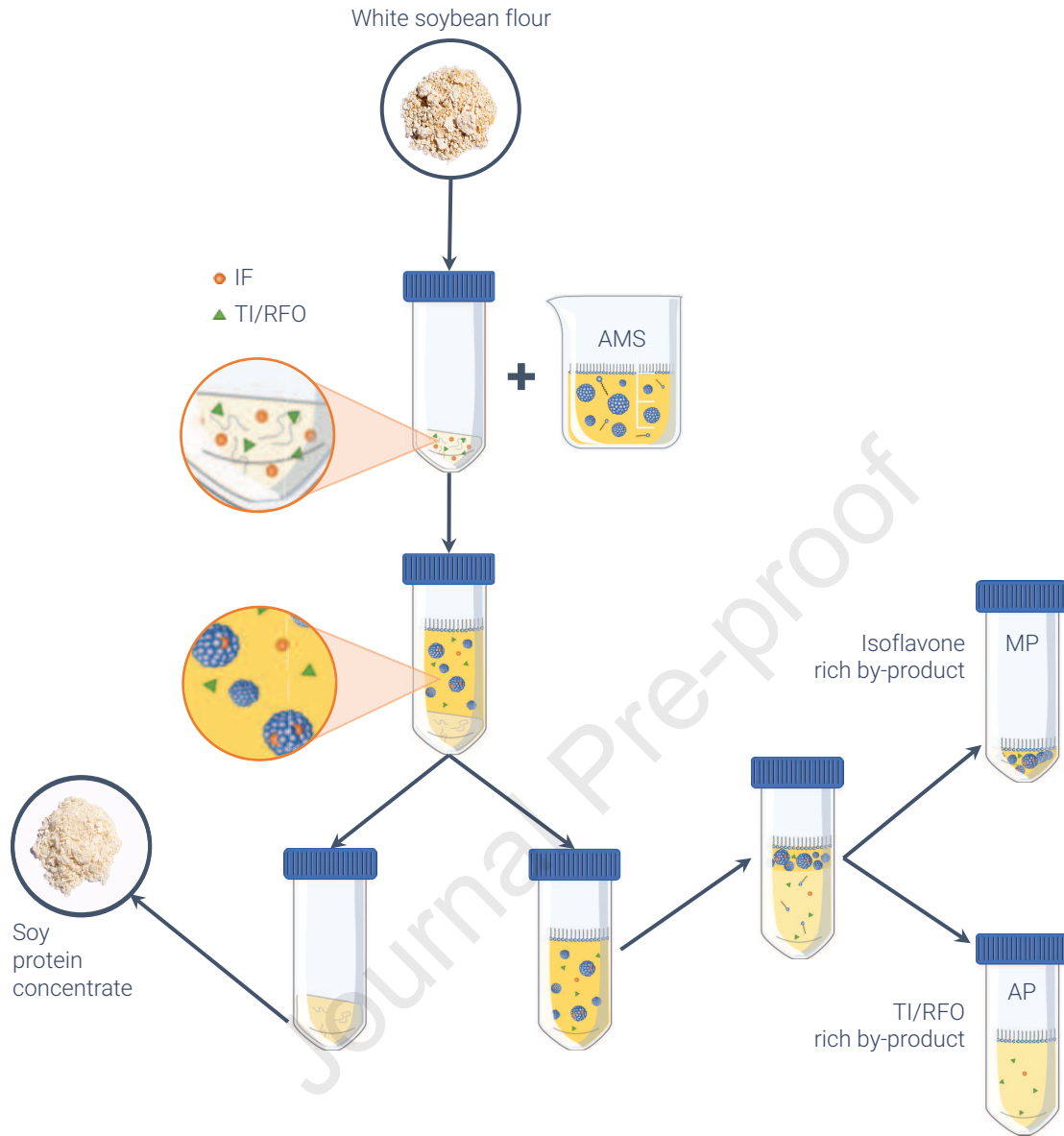
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1

2 Research paper

3 **Production of soy protein concentrate with the recovery of**
4 **bioactive compounds: from destruction to valorization**

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22

23 **Abstract**

24 This work aimed to develop a novel methodology based on aqueous
25 micellar systems (AMS), for producing soy protein concentrates (SPC) from
26 soybean flour and recovering high-valuable bioactive compounds as by-products.
27 Ethoxylated aliphatic alcohols Tergitol 15-S-7 and Tergitol 15-S-9, non-toxic and
28 biodegradable surfactants, were selected to form the AMS. The methodology
29 consisted of an extractive stage of soybean flour with AMS, which rendered both
30 a pellet, i.e., the SPC, and a supernatant containing the extracted bioactive
31 compounds. The latter was further heated above the cloud point temperature, thus
32 resulting in a biphasic system formed by a micelle-rich phase (MP) and an
33 aqueous phase (AP). Obtained SPC showed a noticeable loss (~90%) of trypsin
34 inhibitor activity, a total protein content close to 60%, soluble protein amounts
35 varying from 19% to 34%, and remarkable released (by simulated digestion)
36 antioxidant and antihypertensive activities. Those indicators are similar to or even
37 better than those corresponding to SPC from the classical acid-extraction method.
38 The AMS also exhibited an enhanced efficiency for extracting antinutrients such
39 as non-digestible oligosaccharides, trypsin inhibitors, and lectins mostly
40 recovered at the AP and separated from isoflavones, which were concentrated and
41 isolated at the MP. The recovery of all the mentioned bioactive compounds,
42 whether beneficial or undesirable, broadens their uses in research, food, and
43 pharmacological fields.

44 This successful performance, simplicity, scalability, and sustainability
45 make the proposed AMS-based extraction a powerful tool for processing plant
46 derivatives and valorizing their by-products.

47

48 **Keywords:** aqueous micellar two-phase system; isoflavones; trypsin inhibitors;
49 galactooligosaccharides; antioxidant activity; antihypertensive activity

50

51 **1. Introduction**

52 Soybean [*Glycine max* (L.) Merr.] is the most important legume crop
53 produced and consumed globally (Day, 2013; Jia et al., 2020). This legume and
54 its by-products are considered one of the primary alternative protein sources for
55 animal and human consumption (35-40%). Soybean has not only become an
56 increasingly popular food. However, it has also attracted much interest because of
57 the positive effect that its high intake produces on health, in particular in Asian
58 populations (Kulling et al., 2001). Soy-based foods also contain a wide range of
59 biologically active secondary metabolites, i.e., bioactive compounds, which can
60 confer either beneficial or undesirable effects. Among the former, antioxidant and
61 antihypertensive bioactivities have been widely reported (Balisteiro et al., 2013;
62 Coscueta et al., 2016; González-Montoya et al., 2016). Consumption of this
63 legume may reduce the risk of chronic diseases, such as cardiovascular diseases
64 and cancer, as well as reduce the risk of osteoporosis and relieve the symptoms of
65 menopause (Messina, 2014; Xiao et al., 2012). Phytochemicals responsible for
66 such protective activities include saponins, phytates, protease inhibitors, phenolic
67 acids, isoflavones, lecithin, lectin, and bioactive peptides (de Mejia et al., 2003;
68 C. C. Lee et al., 2017; Lule et al., 2015; Xu et al., 2015). However, some declared
69 beneficial activities, at specific doses and conditions, also have their dark side.
70 Soybean contains various antinutritional bioactive compounds that exhibit
71 undesirable physiological effects, such as preventing the absorption of nutrients.
72 The main antinutritional compounds comprise lipoxygenase, trypsin inhibitors,

73 lectin, and others in minor quantities, such as tannins, non-digestible
74 oligosaccharides, saponins, alkaloids, phenolic compounds, and phytates. Trypsin
75 inhibitors are the most critical components of antinutritional factors responsible
76 for growth retardation and digestive and metabolic diseases (Boisen & Eggum,
77 1991; Gatel, 1994). Therefore, the inactivation of trypsin inhibitors becomes a
78 requirement to improve the absorption of soy proteins in the digestive tract, thus
79 representing a challenge for the food industry and research development (Liu,
80 1997). At present, "detoxification," i.e., the inactivation of soybean antinutrients,
81 is carried out through various processes (Akande & Fabiyi, 2010; Newkirk,
82 2010). Denaturing the thermolabile antinutrients (trypsin inhibitors and lectins)
83 by heat is the most widespread classical inactivation process. It causes the loss of
84 their activity and results in improving protein digestibility. However, this process
85 also leads to the indiscriminate destruction of other essential nutrients and
86 bioactive molecules in the legume (Agrahar-Murugkar & Jha, 2010; Y. Chen,
87 2015; Jasti et al., 2015; Murugkar, 2015). Roasting in a rotary drum dryer or
88 conventional grain dryer (temperatures vary between 110-170 °C) can reduce
89 trypsin inhibitors up to 85%, while conventional drying with hot air at 100 °C for
90 two hours reduces trypsin inhibitors activity by 80% (Agrahar-Murugkar & Jha,
91 2010; Carvalho et al., 2013; Stewart et al., 2003). Other detoxification
92 methodologies include extrusion, micronization, sterilization by autoclaving,
93 dielectric thermal treatment technology, infrared, and enzymatic chemical
94 treatment. However, they are not applicable on a macro scale due to their high
95 cost (Vagadia et al., 2017). Besides, all the processes mentioned are destructive;
96 this deprives the opportunity to valorize those antinutrients that present beneficial
97 properties under certain conditions (Dang & Van Damme, 2015; Gomes et al.,

98 2011). As an initial step, extracting and isolating those compounds is necessary.
99 That would allow their toxicological and clinical evaluation application and their
100 subsequent commercialization as supplemental ingredients.

101 Soybean flour, which is obtained from grinding dehulled soybeans, is one
102 of the most widely marketed protein-rich food ingredients. Subjecting soybean
103 flour to a washing process with appropriate extractive liquids allows for obtaining
104 a soy protein concentrate (SPC). That is an ingredient with higher protein
105 content/quality and lower content of bioactive compounds, e.g., antinutrients,
106 which leach out in the washing liquids. This non-destructive detoxification
107 process allows for recovering bioactive compounds; however, it is not yet applied
108 for that purpose due to the lack of technologies capable of separating the different
109 phytochemicals remaining in the extracts in a viable and sustainable way.
110 Traditionally, SPC is obtained from defatted soybean flour by precipitating
111 proteins and discarding soluble sugar and minor constituents with an alcohol-
112 water mixture or a diluted acid solution in the pH range of 4.0-4.8 (Erickson,
113 1995). The yields of SPC for these conventional processes have been reported to
114 vary between 60-70% concerning the flour protein content (Erickson, 1995).
115 Thus, approximately two-thirds of the protein content of soy flour is recovered as
116 insoluble residues after the extraction. In contrast, the remaining one-third,
117 mainly containing protein antinutrients, is lost (Alibhai et al., 2006).

118 Recently, scientists have evaluated a wide range of new non-toxic, non-
119 flammable, and biodegradable solvents to develop sustainable and
120 environmentally friendly extraction methods (Bajkacz & Adamek, 2017). Certain
121 surfactants exhibit the mentioned properties and represent an economical
122 alternative to expensive and dangerous organic solvents. In aqueous media, they

123 form aggregates, i.e., micelles, capable of interacting with hydrophilic or
124 lipophilic molecules through hydrophobic, dipolar, and hydrogen bonding
125 interactions; thus, these AMS become useful for extractive purposes (Sharma et
126 al., 2015). Besides, they can separate into two phases, a micelle-poor one and a
127 micelle-rich one, when heated above a critical temperature (cloud point), thus
128 acquiring separating properties. AMS successfully recovered soybean
129 phytochemicals, such as isoflavones. A Genapol X-080 AMS performed
130 outstandingly in extracting daidzein from *Puerariae radix* (He et al., 2005).
131 Furthermore, previous works carried out by our team demonstrated that Triton X-
132 114, Genapol X-080, Tergitol 15-S-7 (Tg7), and Tergitol 15-S-9 (Tg9) AMS
133 were suitable for extraction of total soy isoflavones (Cordisco et al., 2016;
134 Coscueta et al., 2018). Genapol X-080 systems were suitable for extracting
135 antinutrients from soybean flour; however, a complete characterization (protein
136 content, antioxidant and antihypertensive activities) of the obtained SPC was not
137 performed (Haidar et al., 2018).

138 In this context, this work aimed to develop a soybean flour detoxifying
139 methodology, AMS-based, capable of producing protein concentrates with
140 similar or improved quality to those obtained by classical methods and recovering
141 high-valuable bioactive compounds as by-products. Thus, we proposed AMS
142 formed by the biodegradable surfactants Tg7 and Tg9 as extractive systems since
143 they represent a sustainable alternative industrially applicable. We considered
144 antioxidant and antihypertensive activities, digestibility, and trypsin inhibitory
145 activity as key parameters, other than protein content, to define the final SPC
146 quality. Regarding the leached bioactive compounds, we have considered the
147 molecular distribution pattern of the extracted proteins as one of the extraction

148 efficiency indicators, together with the recovery and distribution coefficients of
149 non-protein compounds (isoflavones and raffinose family oligosaccharides).
150 Finally, we compared the traditional methodology and the one proposed here
151 based on their advantages and disadvantages and provided future perspectives.

152

153 **2. Materials and methods**

154 **2.1. Materials**

155 The surfactants Tergitol 15-S-7 (Tg7) and Tergitol 15-S-9 (Tg9) were
156 supplied from Sigma-Aldrich (St. Louis, MO, USA). White soybean flour (i.e.,
157 non-thermal treated soybean flour) was supplied by the food processing company
158 Molinos Río de la Plata SA (San Lorenzo, Argentina). Crystallized salt-free
159 bovine trypsin, porcine pepsin (800-1000 U mg⁻¹ protein), pancreatin (4xUSP),
160 angiotensin-I converting enzyme (peptidyl-dipeptidase A, EC 3.4.15.1, 5.1 U
161 mg⁻¹), crystalline α -N-benzoyl-DL-arginine-p-nitroanilide (BAPNA), bile salts
162 and Trolox (6-hydroxy-2,5,7,8-tetramethyl-chroman-2-carboxylic acid) were
163 obtained from Sigma-Aldrich (St. Louis, MO, U.S.A.) and used without further
164 purification. Fluorescein [3',6'-dihydroxyspiro (isobenzofuran-1[3H],9'[9H]-
165 xanten)-3-one] was purchased from Fisher Scientific (Hanover Park, IL). AAPH
166 [2,2'-azobis (2-amidi-nopropane) dihydrochloride] was purchased from Aldrich
167 (Milwaukee, WI). The tripeptide Abz-Gly-Phe(NO₂)-Pro was obtained from
168 Bachem Feinchemikalien (Bubendorf, Switzerland). Tris [tris (hydroxymethyl)
169 aminomethane] was obtained from Fluka (GmbH, Germany). Isoflavone standards
170 (Sigma-Aldrich, St. Louis, MO, USA) were dissolved in pure methanol until
171 obtaining the following concentrations: daidzin 1.5-80.0 μ g mL⁻¹; daidzein 0.3-

172 17.0 $\mu\text{g mL}^{-1}$; genistin 0.7-40.0 $\mu\text{g mL}^{-1}$ and genistein 0.2-13.0 $\mu\text{g mL}^{-1}$. All the
173 other reagents were of analytical grade and used without further purification.
174 Deionized water was used to prepare all the solutions.

175 **2.2. Methods**

176 White soybean flour (henceforth called soybean flour) was treated following
177 traditional and AMS-based extraction processes. Samples from the resulting
178 supernatants, treated solids, permeates, and extracts were subjected to different
179 analytical procedures to determine performance indicators. Simultaneously, non-treated
180 soybean flour was also evaluated for comparison purposes. Figure 1, provided for a
181 more precise understanding, shows a schematic diagram of all the developed processes
182 and techniques whose descriptions are given below.

183 **2.2.1. Production of soy protein concentrates**

184 Soy protein concentrates (SPC) were prepared according to the classical
185 acid-washing method (Sair, 1959). Briefly, a suspension of 20.00% m/V soybean
186 flour and 25.00 mM citrate buffer pH 4.5 (3.00 g of flour in 60.00 mL of buffer)
187 was incubated in a bath at 40 °C and continuously stirred (150 rpm) for 45 min.
188 Then, the system was centrifuged (4000 rpm) at 15 °C for 15 min, thus obtaining
189 two fractions: a supernatant and an insoluble fraction, i.e., treated solid (SPCa).

190 SPC were also obtained by applying AMS as extractive solvents. AMS
191 formed by two non-ionic surfactants, Tg7 and Tg9, were evaluated. Appropriate
192 amounts of surfactants were dissolved in 50.00 mM sodium citrate (NaCit) at pH
193 4.5 until a final concentration of 5% m/m. This surfactant concentration was
194 selected according to previous optimization tests (Coscueta et al., 2022). Higher

195 concentrations were discarded to avoid high viscosity conditions representing a
196 technical disadvantage. Each AMS was prepared by mixing 3.00 g of a given
197 surfactant (Tg7 or Tg9) with 50.00 mM NaCit buffer pH 4.5 until a final system
198 volume of e 60.00 mL. This mixture and a sample of soybean flour (3.00 g) were
199 incubated separately in a thermostatic bath for 20 min to reach the extraction
200 temperature (45 °C). After the incubation, both components (flour and surfactant
201 solution) were placed into an Erlenmeyer, mixed, and stirred for 45 min inside
202 the thermostatic bath, maintaining the temperature at 45 °C. Then, the system was
203 centrifuged (4000 rpm) at room temperature for 10 min, thus obtaining a pellet
204 (SPC) and a supernatant, separated by decantation. The supernatant was
205 incubated again in a thermostatic bath and allowed to stand until total phase
206 separation (approximately 15 min). A phase of low micelle concentration, i.e.,
207 aqueous phase (AP) and a phase rich in micelles (MP), were obtained by
208 decanting. The phase separation temperatures, 45 °C for Tg7 and 60 °C for Tg9,
209 were selected for each surfactant according to the phase diagram previously
210 determined. These temperatures were a few degrees above the respective cloud
211 point to obtain similar volumes of MP. Experiments were performed in triplicate
212 for each surfactant.

213 All the resulting SPC (from traditional and AMS-based extractions) were
214 neutralized (final pH 6.5) by adding 20.00 mL of 25.00 mM phosphate buffer
215 solution at pH 7.0 and 0.50 mL of 1.00 M NaOH solution and then lyophilized.
216 Finally, the Kjeldahl reference method analyzed the total protein content of each
217 lyophilized SPC (SPCa, SPC Tg7, SPC Tg9).

218 **2.2.2. FTIR spectrometry**

219 Fourier transform infrared (FTIR) spectrometry characterized the soybean
220 flour and the SPC. The spectra were acquired by averaging 30 measurements at
221 wavenumbers from 500 to 4000 cm^{-1} with a resolution of 4 cm^{-1} . The spectra
222 were normalized for the maximum absorbance. The amide-I band's second
223 derivative was used to identify the different spectral components of soybean flour
224 and SPC. The subsequent spectral deconvolution was performed by applying a
225 Gaussian fitting (Arrondo et al., 1993; Zana et al., 1998). Measurements were
226 carried out in an infrared spectrometer, model ABB MB3000 (ABB,
227 Switzerland), equipped with a deuterated triglycine sulfate detector and provided
228 with a horizontal reflection accessory MIRacle™ (PIKE Technologies, USA), for
229 attenuated total reflectance, with a diamond crystal plate/Se.

230 ***2.2.3. Extraction of trypsin inhibitors and soluble protein***

231 Reference methods globally accepted for estimating trypsin inhibitory
232 activity in soybean-derived products share the same principle: trypsin inhibitors
233 are extracted from a weighed sample under the alkaline condition at which soy
234 protein solubility is enhanced (Liu, 2021). In this work, the extraction/lixiviation
235 was carried out by mixing 1.00 g of soybean flour/SPC with 50.00 mL (V_E) of
236 10.00 mM NaOH and stirring at room temperature for three hours, according to
237 the standard method proposed by Kakade et al. (1974) and later improved
238 (AOCS, 2009; Kakade, 1974). A final centrifugation step (3500 rpm) for 10 min
239 was carried out to recover the supernatant, which was conveniently diluted (with
240 a dilution factor F_D) to determine the trypsin inhibitory activity (TIA) and soluble
241 protein content.

242 ***2.2.4. Trypsin inhibitory activity (TIA)***

243 TIA was measured according to the modified methodology proposed by
 244 Coscueta et al. (2017). The procedure was adapted to reduce the working
 245 volumes and develop the assay in a 96-well microplate, as shown in Table 1. The
 246 enzymatic reaction progress was monitored by absorbance measurements (400
 247 nm) for 2 min. All the determinations were performed on the Multiskan GO
 248 (Thermo Fisher Scientific Corporation) spectrophotometer operated by the SkanIt
 249 3.2 software (Thermo Fisher Scientific Corporation). The TIA was calculated as
 250 follows:

$$\text{TIA}' = 100 \frac{0.350 (m_{\text{control}} - m_{\text{sample}})}{0.040} F_D V_E \quad (1)$$

251 where 100 is a conversion factor (to convert 0.01 u. Abs in trypsin inhibition
 252 units); $m_{\text{control}} - m_{\text{sample}}$, the difference between the slopes corresponding to the
 253 absorbance vs. time curves, in the absence (control) and presence of trypsin
 254 inhibitors (sample); F_D , the dilution factor of supernatant from extraction; V_E is
 255 the extraction volume of 0.01 M NaOH solution (50 mL, see section 2.2.3), used
 256 for 1 g of soybean flour; 0.040, the aliquot (mL) of supernatant dilution used in
 257 the continuous assay; and 0.350, the final reaction volume (mL) in the microplate
 258 well. Finally, the TIA of a given sample was expressed as a percentage of the
 259 total TIA present in soybean flour ($\text{TIA} = \text{TIA}'_{\text{sample}} / \text{TIA}'_{\text{soybean flour}} \times 100$) to
 260 facilitate the comparison of extractive efficiencies exhibited in the different
 261 treatments.

262 **Table 1.** Continuous method to determine trypsin inhibitory activity adapted for use in a
 263 microplate reader.

Reagents	Control [†]	Sample [†]
Tris buffer 0.050 M, pH 8.20	140	100
Trypsin working solution	70	70
Diluted supernatant	---	40
Incubate at 37 °C inside the microplate reader for 2 min, then add		
BAPNA working solution (pre-heated at 37 °C)	140	140

†Volumes expressed in μL .

264

265 **2.2.5. Determination of soluble protein content**

266 We determined the soluble protein content by the bicinchoninic acid
 267 method (Smith et al., 1985), adapted for use in a 96-well microplate. This method
 268 measured the protein content in extracts from alkaline lixiviation of SPC and
 269 permeates from *in vitro* gastrointestinal simulation (see section 2.2.6). A stock
 270 bicinchoninic acid (BCA) solution was prepared with this composition: BCA
 271 1.00% (m/V), sodium tartrate 0.16% (m/V), Na_2CO_3 2.00% (m/V), NaOH 0.40%
 272 (m/V), and NaHCO_3 0.95% (m/V), the final pH being 11.2. A stock CuSO_4
 273 solution of 4.00% (m/V) was also prepared. The working BCA reagent was
 274 prepared by mixing the BCA stock solution (diluted 1:10) with the stock CuSO_4
 275 solution to a 50:1 ratio. A calibration curve made with bovine serum albumin
 276 (BSA) with concentrations of 50-1000 $\mu\text{g mL}^{-1}$ was used. The protocol was
 277 carried out by placing 25 μL of sample in each well and then adding 200 μL of
 278 working BCA reagent simultaneously in all the wells. The microplate was
 279 incubated at 37 °C for 30 min before obtaining the absorbance values at 562 nm.
 280 Incubation and readings were performed on the Multiskan GO (Thermo Fisher

281 Scientific Corporation) spectrophotometer operated by the SkanIt 3.2 software
282 (Thermo Fisher Scientific Corporation).

283 **2.2.6. *In vitro simulated gastrointestinal digestion***

284 The *in vitro* simulated gastrointestinal digestion (SGI) was carried out for
285 all SPC and soybean flour. The digestive process in the mouth and esophagus,
286 where carbohydrates are mainly affected, was not simulated since this work
287 focused on the digestion of proteins and phenolic compounds. Replicates (300
288 mg) from each applied methodology were adequately pooled and homogenized
289 into one sample. A given amount of the pooled sample (280 mg) was mixed with
290 6.00 mL of acidified water (pH 2.0). The pH was adjusted to 2.0 with 1.00 N
291 HCl, and the final volume was completed to 7.00 mL with the same acidified
292 water. The mixture was incubated at 37 °C and shaken at 130 rpm for 20 minutes
293 to temper the digestive process. Before starting the SGI, 1.00 mL of supernatant,
294 representing the sample at the initial time (T1), was removed from each
295 experiment. The initial stage of the SGI began with the stomach digestion step,
296 the gastric juice being simulated with pepsin 25 mg mL⁻¹, prepared in 0.10 N HCl
297 (Aura, 2005). 0.3 mL of this "gastric juice" was added, left at 37 °C, and shaken
298 at 130 rpm for 60 min. Then, the gastric stage was terminated by increasing the
299 pH to 6.5 with 100.00 mM NaHCO₃ solution. An aliquot of 1.00 mL was then
300 withdrawn, thus representing the sample corresponding to the end of the
301 mentioned stage (T2). For the intestinal step, pancreatic juices were simulated
302 with a solution of pancreatin 2 mg mL⁻¹ and bile salts 12 mg mL⁻¹ diluted in a
303 solution of 100.00 mM NaHCO₃ (Laurent et al., 2007). 1.50 mL of pancreatic
304 solution was added to the system. The temperature was returned to 37 °C and
305 stirring decreased to 45 rpm. This stage was extended for 90 min (T3) and then

306 stopped by freezing at $-30\text{ }^{\circ}\text{C}$. Three independent SGI experiments were
307 performed for each pool. Finally, all the samples from the SGI process were
308 nano-filtered in 3 kDa pore membranes (Amicon® Ultra-4, Millipore), the
309 resulting permeates (T1, T2, and T3) being subsequently analyzed (bioactive
310 peptides and phenolic compounds). Enzymatic solutions were freshly prepared
311 and sterilized by filtration with $0.22\text{ }\mu\text{m}$ membrane filters (Millipore, Billerica,
312 MA, USA). After being sterilized, the solutions were kept in an ice bath to avoid
313 enzymatic self-degradation. A thermostatic water bath at $37\text{ }^{\circ}\text{C}$ was used to
314 simulate the physiological temperature of the human body. Mechanical agitation
315 (parallel peristaltic movements) was implemented, with intensities emulating
316 those reached in each digestive compartment.

317 **2.2.7. Antioxidant activity**

318 The oxygen radical scavenging capacity (ORAC) was determined by the
319 method proposed by Coscueta, Brassesco, & Pintado (2021). The antioxidant activity of
320 each sample (permeates T1, T2, and T3) was evaluated in triplicate and expressed
321 as $\mu\text{mol Trolox Equivalent per gram of initial digested sample (SPC or soybean}$
322 flour) on a dry basis.

323 **2.2.8. ACE inhibitory activity**

324 The ACE inhibitory activity was carried out using the fluorometric assay
325 described by Coscueta et al. (2021). The inhibitory activity on ACE (iACE) of
326 each sample (permeates T1, T2, and T3) was evaluated in triplicate and expressed
327 as the concentration capable of inhibiting 50% of the enzymatic activity (IC_{50}). A
328 non-linear model calculated the IC_{50} values. The results were expressed as μL
329 mL^{-1} to inhibit 50% of the enzymatic activity.

330 **2.2.9. Size exclusion chromatography**

331 The molecular mass distribution of the protein components in the
332 supernatant from traditional extraction and the aqueous phase (AP) from AMS-
333 based extraction was analyzed by size exclusion chromatography. The
334 chromatographic runs were performed at a flow of 0.5 mL min⁻¹ with 25 mM
335 phosphate buffer (pH 7) containing 150 mM NaCl and 0.2 g L⁻¹ NaN₃. Standard
336 proteins with known molecular masses (Thyroglobulin, 669 kDa; Ferritin, 440
337 kDa; Aldolase, 158 kDa; Conalbumin, 75 kDa; Ovalbumin, 43 kDa; Carbonic
338 anhydrase, 29 kDa; Ribonuclease A, 13.7 kDa; Aprotin, 6, 5 kDa) were used to
339 calibrate the system. The AKTA pure 25 L system (GE Healthcare Life Sciences,
340 Freiburg, Germany) was used in a configuration consisting of two high-
341 performance piston pump systems, a pressure monitoring system for column
342 protection, a mixing chamber, a V9-IA injection valve, a Superdex® 200 10/300
343 GL column connected in series to a Superdex Peptide 10/300 GL column (GE
344 Healthcare Life Sciences, Freiburg, Germany), and a length U9-L UV detector
345 fixed wave at 280 nm. The system was controlled by UNICORN software.

346 **2.2.10. Determination of isoflavones by HPLC**

347 The identification and quantification of extracted isoflavones on
348 supernatant from traditional extraction and both phases (AP and MP) of micellar
349 systems were carried out using high-performance liquid chromatography
350 (HPLC). Initially, each analyzed sample was conveniently diluted (1:3 with pure
351 MetOH) and filtered on a 0.45 µm filter. Chromatography was carried out on a
352 reversed-phase column (COSMOSIL 5C18-AR-II Packed Column - 4.6 mm D.I.
353 x 250 mm) with two mobile phases. Mobile phase A consisted of ultra-pure water

354 acidified with glacial acetic acid (0.1% V/V), while phase B was constituted by
355 acetonitrile acidified with glacial acetic acid (0.1 % V/V). The operation involved
356 injecting 20 μL of sample and eluting it with a linear gradient from 80 to 0% of
357 phase A over 25 min, at a constant flow of 0.8 mL min^{-1} and a column
358 temperature of 25 $^{\circ}\text{C}$. Each isoflavone was identified by considering the
359 absorbance spectrum and the retention time of standards. The concentration of
360 each isoflavone was determined by measuring the area under the peak and
361 interpolating it on the corresponding calibration curve. The results were
362 expressed in μg of isoflavone per gram of soybean flour on a dry basis. The
363 Waters e2695 modular separation system was used, with a UV/Vis photodiode
364 array detector (PDA 190-600 nm). The acquisition of the data and the analysis
365 were carried out using the Empower 3 software.

366 ***2.2.11. Determination of non-digestible oligosaccharides by HPLC***

367 The content of raffinose family oligosaccharides in the supernatant from
368 traditional extraction and both phases (AP and MP) of micellar systems was
369 determined by HPLC. Aliquots (30 μL) of the undiluted liquid samples were
370 analyzed by chromatography. The mobile phase was a 13.00 mM H_2SO_4 solution,
371 with a flow of 0.8 mL min^{-1} , at isocratic elution. HPLC quality standards of
372 raffinose, stachyose, glucose, and sucrose were used to identify the mentioned
373 compounds in the samples by considering their retention time. The peaks for
374 raffinose and stachyose were so close together that we had to measure them as
375 one, which we called raffinose family oligosaccharides. The values were
376 expressed in relative units (RU), given by the product between the integrated area
377 and the mass of liquid obtained for each fraction, referred to as 1 gram of soybean
378 flour (RU g^{-1}). An HPLC system prepared for the identification and quantification

379 of sugars was used, consisting of a Knauer WellChrom Pump K-1001 module
 380 (Knauer GmbH, Germany) and a differential refractive index (RI) detector K-
 381 2301 (Knauer GmbH, Germany). The separation was carried out on an Aminex
 382 HPX-87H 300 x 7.8 mm column (Bio-Rad, Hercules, USA) coupled to a Micro-
 383 Guard Cation H⁺ precolumn (Bio-Rad, Hercules, USA), maintained at a
 384 temperature of 42 °C by an Eldex CH-150 column oven (Eldex Laboratories,
 385 Napa, CA). The data were acquired and analyzed using Clarity v.5.0.5.98
 386 software (DataApex Ltd, Prague, Czech Republic).

387 *2.2.12. Extraction efficiency parameters*

388 The distribution coefficients (K_d) and phase recovery performance (Pr) in
 389 the different AMS were determined for both isoflavones and raffinose family
 390 oligosaccharides. The K_d was estimated as:

$$K_d = \frac{C_{MP}}{C_{AP}} \quad (2)$$

391 where C_{MP} and C_{AP} are the concentrations of the analyte (isoflavones or raffinose
 392 family oligosaccharides) in the MP (micellar phase) and AP (aqueous phase),
 393 respectively. On the other hand, the Pr was determined:

$$Pr(\%) = \frac{C_{MP/AP} V_{MP/AP}}{(C_{MP} V_{MP} + C_{AP} V_{AP})} 100 \quad (3)$$

394 where C_{MP/AP} is the concentration of the analyte in either the MP or AP, selected
 395 according to the phase of the highest recovery, these V_{MP/AP} is the volume of the
 396 corresponding phase. Equation (3) is only valid when analytes distribute entirely
 397 between the two phases without precipitating at the interphase.

398 **2.2.13. Statistical analysis**

399 All the experiments were carried out in triplicate, except for specific cases
400 where something different was indicated, and the results were expressed as the
401 mean value with their standard deviation (SD). Before any comparative statistical
402 analysis, an exploratory study was carried out for all the data sets to determine
403 the compliance of normality and homoscedasticity. Then the means were
404 analyzed statistically by analysis of variance (ANOVA) followed by a posthoc
405 test using Tukey (Tukey, 1949). A significance level of 5% was considered. All
406 statistical analysis was carried out with the aid of RStudio V 1.0.143.

407 **3. Results and discussion**

408 According to previous results (Coscueta et al., 2022), we designed a new AMS-
409 based process applied to soybean flour for producing SPC and recovering valuable
410 bioactive compounds as by-products. A graphical scheme and technical details of the
411 proposed methodology are presented in Figure 2 to facilitate reading this article and
412 interpreting the results.

413 Figure 2 shows an initial micellar extraction performed by applying AMS on
414 soybean flour. Then, a phase separation produced a MP and an AP by heating the
415 extract (supernatant of the first extraction) to a temperature higher than the cloud point.
416 It is important to note that the micellar extraction for Tg7 is considered a "cloud point"
417 extraction since the extraction temperature (45 °C) is above the Tg7 CP (39 °C). This is
418 not so for Tg9 since its cloud point (61 °C) is higher than the working temperature.

419 **3.1. Producing soy protein concentrates: characterization of the product**

420 **3.1.1. FTIR spectroscopy**

421 Although the literature has reported the non-ionic Tg7 and Tg9 as mild
422 surfactants, it was necessary to evaluate their effect on soy protein structure since
423 it might affect its functional properties (Nadar et al., 2017; Vicente et al., 2017).
424 The spectroscopic analysis of polymeric molecules is complex due to the
425 molecular vibrations that arise from numerous atoms. FTIR is an advantageous
426 technique for the study of protein systems. There are several easily identifiable
427 regions in the middle infrared spectrum, having nine characteristic bands called
428 amide-A, B, I, II ... VII; the amide-I, amide-II, and amide-III being the most
429 widespread ones used in structural studies of protein

430 Figure 3A shows the FTIR spectra for flour (starting material) and SPC
431 (products). The amide-A ($3500\text{-}3200\text{ cm}^{-1}$) and amide-B ($3100\text{-}2500\text{ cm}^{-1}$) bands come
432 from a Fermi resonance between the first harmonic of amide-II and the vibration of the
433 N-H stretch. Notably, the spectral band of amide-B showed an intense alteration after
434 the process, which indicates a conformational change in the secondary structure of the
435 matrix of the SPC (Chang & Tanaka, 2002). This band's intensity increased drastically for
436 the SPCa and the SPC Tg9 compared to the soybean flour. However, only slight
437 changes were noticeable for the SPC corresponding to Tg7. The amide-I and II bands
438 are the two central regions of the infrared spectrum for protein. The amide-I (between
439 1700 and 1600 cm^{-1}) is mainly associated with the stretching vibration C=O (70-85%)
440 and is directly related to the conformation of the main peptide chain (Chang & Tanaka,
441 2002). Amide-II ($1600\text{-}1500\text{ cm}^{-1}$) results from the N-H bending vibration (40-60%) and
442 the C-N stretch vibration (18-40%). When structural alterations such as denaturation or
443 aggregation occur, these two bands significantly decrease in intensity (Nishinari et al.,
444 2014). Figure 3B shows the highest and lowest amide-I and II signals for the flour and
445 SPCa, respectively. In contrast, it shows intermediate intensities for the SPCs obtained

446 by the micellar systems. The SPC Tg7 spectrum was like the flour, while the SPC Tg9
 447 spectrum was higher than the SPCa. Amide-III (between 1300 and 1200 cm^{-1}) is a very
 448 complex band that results from a mixture of several coordinate shifts; it does not exhibit
 449 noticeable differences between SPCs and flour (Figure 3B).

450 Even if the primary protein structures were the same, the secondary and the
 451 tertiary structures sometimes are not. The amide-B allowed us to analyze what
 452 happened to the secondary structures of the proteins. The most interesting regions in the
 453 FTIR spectra are the amide-I and II regions since changes in these regions were
 454 observed for other proteins (Arrondo et al., 1993; Susi & Byler, 1986). To analyze the
 455 secondary structures, we applied a deconvolution procedure of the amide-I band (Figure
 456 3C-F) (Fabian et al., 1993). The second derivative curve allowed the identification of
 457 the different spectral components used in a deconvolution procedure with Gaussian
 458 curve fitting. Table 2 presents the contribution percentages of the various secondary
 459 structure types, calculated as the ratios between the areas of the curves corresponding to
 460 the different component bands and the total area below the spectral curve.

461 **Table 2.** Protein secondary structure in soybean flour and SPC by FTIR analysis.

Product	Secondary structure (%) [†]			
	α -helix	β -sheet	Random coil	β -turns
Soybean flour	62	38	0	0
SPCa	42	44	0	14
SPC Tg7	12	24	43	20
SPC Tg9	67	28	0	4

[†] Structural composition of the amide-I, obtained from the area under each deconvoluted band and expressed as a percentage of the total area.

462

463 The data revealed that amide-I for all SPCs consists of nine or ten main
 464 components, unlike flour, which exhibits only two. We found the main band of the
 465 soybean flour and SPCa FTIR spectra in the amide-I region between 1660-1650 cm^{-1}

466 (62% and 42% of the total area, respectively, Table 2). This corresponds to the
467 vibrational movements of the amide residues of the main chain in a helical
468 conformation. The soybean flour also presented another large band between 1650 and
469 1600 cm^{-1} corresponding to the β -sheet structure, which is in the minority (38%).
470 Meanwhile, the SPCa also had smaller bands at 1637-1600 cm^{-1} and 1700-1682 cm^{-1} ,
471 related to β -sheet structures (44%), which slightly exceeded the content of α -helix
472 (42%). Besides, it presented two bands corresponding to β -turn structures (1674 cm^{-1}
473 and 1666 cm^{-1}). Both β -sheet and β -turn structures indicate a greater union of the amide
474 protons by forming hydrogen bonds (FAO & Berk, 1992). We did not observe a common
475 pattern in the FTIR spectra of the Tg7 and Tg9 SPCs (Table 2). The SPC Tg7 showed
476 the principal peak in the region corresponding to the unordered structure (1639-1638
477 cm^{-1}), thus representing the highest structural percentage (43%). The second main
478 structure was the β -sheet type, contributing about 24%. Finally, the SPC Tg9 had a
479 structural distribution like the flour, with 67% of α -helix and 28% of β -sheet.

480 The structural alterations suffered by the SPC protein are related to the process
481 conditions, such as temperature, surfactant concentration, and the medium's pH. It
482 should be noticed that those conditions may affect inter/intramolecular interactions
483 (formation/rupture of hydrogen bonds, hydrophobic effects) of protein molecules, thus
484 resulting in conformational changes. Notably, the applied pH (pH 4.5) corresponds to
485 the isoelectric point of most of the matrix proteins. This pH facilitates aggregation by
486 non-electrostatic forces, thus decreasing protein solubility in the final concentrate
487 (Derringer & Suich, 1980). We must not ignore that although the applied methodologies
488 allow concentrate proteins, they cause the loss of soluble carbohydrates and a
489 considerable amount of soluble protein. That enriches the final product in proteins
490 already insoluble in the starting soybean flour, either by extracting the oil with hexane

491 or the solvent removal step in the previous soybean processing. It should be noticed that
 492 changes in the secondary structure of soy proteins caused by a given treatment might
 493 affect not only their conformation but also functional properties such as gel
 494 transparency, solubility, surface hydrophobicity, and emulsifying capacity (X. Chen et
 495 al., 2013; Zhao, Chen, Chen, et al., 2008). Therefore, the information introduced here
 496 could be critical for further understanding and correlating the SPC applications.

497 **3.1.2. Protein content and trypsin inhibitory activity**

498 The SPC produced by the different methodologies were analyzed and compared
 499 with each other and the starting soybean flour. Initially, we analyzed the total protein
 500 content by the Kjeldahl reference method (section 2.2.1). Then, we performed aqueous
 501 extractions to evaluate the trypsin inhibitory activity (TIA) and the amount of soluble
 502 protein by the bicinchoninic acid method (section 2.2.5). The results reported in Table 3
 503 indicated that the total protein varied according to the type of surfactant used in the
 504 proposed technique. SPC Tg9 presented a total protein value comparable to SPCa, while
 505 SPC Tg7 showed a total protein like the starting soybean flour. When comparing the
 506 surfactants, Tg7 was demonstrated to be less efficient in concentrating proteins than
 507 Tg9, thus evidencing a higher protein extractive power.

508 **Table 3.** Total protein content, soluble protein, and trypsin inhibitory activity analysis for SPC
 509 and soybean flour.

Product	Pt ^{†,1}	TIA ^{†,2}	Ps ^{†,3}
Soybean flour	54.6 ± 2.1 ^a	100 ± 7	84 ± 4
SPCa	64.0 ± 1.5 ^b	11 ± 1 ^a	29 ± 4 ^{a,b}
SPC Tg7	57.4 ± 0.7 ^{a,c}	10 ± 2 ^a	34 ± 7 ^b
SPC Tg9	60.7 ± 2.1 ^{b,c}	12 ± 3 ^a	19 ± 4 ^a

† Values are expressed as mean \pm SD on a dry basis. ¹ Total protein content (Pt) expressed as g proteins (100 g product)⁻¹. ² Trypsin inhibitory activity (TIA) expressed as a percentage from the starting soybean flour. ³ Soluble protein content (Ps) expressed as g BSA (100 g total proteins)⁻¹. ^{a-d} Values from the same column that share a superscript do not present statistical differences, given the analysis of their variances (ANOVA) with Tukey's posthoc test for a significance level of 0.05.

510

511 As shown in Table 3, the inhibitory activity of trypsin was considerably reduced,
512 around 90%, in all the SPC, thus reaching satisfactory levels that agreed with those
513 predicted in a previous optimization work (Coscueta et al., 2022). In this regard, none of
514 the methodologies differed significantly. However, this drastic reduction in the TIA
515 resulted in a significant decrease in the protein solubility in 10 mM NaOH. That is a
516 well-known disadvantage of protein concentration methods, i.e., the resulting SPC
517 present low protein solubility after rehydration and poor functional properties. Protein
518 exposure to extreme conditions may cause this low solubility (Alibhai et al., 2006;
519 Fisher et al., 1986). We mean alcohol or acid extraction, heat treatment, precipitation, or
520 centrifugation by extreme conditions. Besides, the reduction of protein solubility could
521 also be the result of the enrichment of the final product is already insoluble proteins
522 before the concentrating process, as we mentioned previously. Different treatments that
523 allow for significant solubility recovery can mitigate this disadvantage's impact
524 (Johnson, 1999). Also, particularly for the AMS-based extractions, the Tg9 led to the
525 most significant protein solubility loss.

526 **3.1.3. Digestibility and bioactivity**

527 To analyze the performance of different SPC at *in vitro* simulated
528 gastrointestinal digestion (SGI), we measured soluble protein, antioxidant activity, and
529 antihypertensive activity at each stage (T1, T2, and T3). We measured soluble protein
530 considering protein compounds with MW less than 3 kDa (enriched peptide fraction),

531 the antioxidant activity by ORAC, and the antihypertensive activity from the inhibitory
532 capacity on ACE (iACE). The response variable was recorded three times on the same
533 experimental unit (pooled sample); therefore, we considered the collected data "repeated
534 measures." So, we analyzed through the "Generalized Linear Models" procedure. Table
535 A1 (see Annex) reports the results of fitting the general linear statistical models. These
536 models relate the response variables soluble protein, antioxidant activity, and
537 antihypertensive activity with three categorical predictive factors: experimental units (I),
538 substrate (M: starting soybean flour or SPC from a given extractive methodology), and
539 SGI's stage (T). Relationships between the observed responses and the predictor
540 variables were statistically significant since, for each model, the P-value was less than
541 0.05. Besides, the determination coefficients (R^2) indicated that the adjusted models
542 explained between 99.6% and 99.7% of the respective variability.

543 For the general digestion process (Table A2 in Annex), irrespective of the
544 sample considered, the three responses adopted significantly different values according
545 to the stage of the SGI. Interestingly, T2 showed higher soluble protein than T3. This
546 finding is attributable to the analytical technique used for protein quantification, the
547 bicinchoninic acid method. That assay depends on the ability of proteins to reduce Cu^{+2}
548 to Cu^{+1} in an alkaline solution (biuret reaction), thus resulting in a purple product.
549 Cysteine, tyrosine, and tryptophan residues are mainly responsible for reducing copper.
550 However, unlike Coomassie dye-binding methods, the peptide skeletons also contribute
551 to color formation, helping to minimize the variability derived from differences in
552 protein composition. The peptide skeleton loss resulting from the release of peptides
553 during stomach digestion (T2) may cause the decreasing signal. These peptides can be
554 further degraded to tripeptides, dipeptides, and free amino acids in the intestinal stage
555 (T3). On the other hand, the ORAC values increased during the gastric phase and

556 practically kept constant in the intestinal phase. About iACE, the IC_{50} decreased
557 significantly at each stage of the process, thus indicating a sustained increase in the
558 inhibitory activity.

559 When considering the samples separately (Table A3 in Annex), we identified
560 three homogeneous groups concerning ORAC and two for soluble protein and iACE.
561 The mean soluble protein released during the digestion of the SPC Tg7 was the lowest
562 one, while the remaining samples did not show differences. Concerning ORAC, the
563 SPC Tg9 and the soybean flour did not differ significantly and surpassed the other
564 samples, the SPC Tg7 showing the lowest level of this bioactivity. On the other hand,
565 the maximum iACE was for the SPC Tg7 and the minimum for SPCa and SPC Tg9,
566 while the soybean flour did not differ from the mentioned groups.

567 Figure 4 shows the soluble protein content, ORAC, and iACE profiles as a
568 function of each digestive stage. The lines represent each I and the color, each level of
569 M. For soluble protein (Figure 4A), the SPCa presented a different behavior than the
570 others. As explained above, it showed a marked peptide release during the gastric phase
571 and a later decrease in the signal during the intestinal phase. That could be indicative of
572 more significant peptide degradation. The SPC Tg9 exhibited an increase in the peptide
573 content during the first stage, keeping it constant until the end of digestion. About the
574 soybean flour and SPC Tg7, the peptide release was almost continuous throughout the
575 digestive process. The results for ORAC (Figure 4B) differed, with SPC Tg7 and SPC
576 Tg9 being markedly different from the other samples. SPC Tg7 showed constant
577 antioxidant activity during the gastric phase, which increased during intestinal
578 digestion. At the same time, SPC Tg9 evidenced a drastic increase and a later reduction
579 in the gastric and intestinal stages, respectively. Unlike the other two responses, the

580 iACE pattern (Figure 4C) was similar for all samples throughout the SGI, with a greater
 581 increase in inhibitory activity during the gastric phase.

582 At the end of the digestion, the soluble protein was similar (Table 4) for all the
 583 products. At the same time, the antioxidant activity of both SPCa and SPC Tg7 was
 584 practically 30% lower than that corresponding to the soybean flour and SPC Tg9.
 585 Concerning iACE, all the products achieved high bioactivities.

586 **Table 4.** Multiple comparisons for each response by product.

Substrate	Means observed at the end of the SGI [†]		
	Ps ¹	ORAC ²	iACE ³
Soybean flour	8.5 ± 0.8 ^a	737 ± 51 ^a	47 ± 6 ^a
SPCa	7.2 ± 0.2 ^a	518 ± 20 ^b	53 ± 6 ^a
SPC Tg7	7.4 ± 0.8 ^a	437 ± 34 ^b	58 ± 4 ^a
SPC Tg9	8.8 ± 0.6 ^a	672 ± 65 ^a	49 ± 6 ^a

[†] Values expressed mean ± SD on a dry basis. ¹ Soluble protein content (Ps) in mg BSA (g of substrate)⁻¹,
² ORAC in μmol TE (g of substrate)⁻¹, ³ iACE as IC₅₀, μg mL⁻¹. ^{a, b} Values from the same column that
 share a superscript do not present statistical differences, given the analysis of their variances (ANOVA)
 with Tukey's posthoc test for a significance level of 0.05.

587 It is expectable that soybean flour with higher protein solubility will release a
 588 greater number of peptides from its digestion and even higher antioxidant and
 589 antihypertensive activities. However, we did not observe this behavior in this work,
 590 probably due to its content of protease inhibitors. Protease inhibitors reduce proteolysis,
 591 releasing a larger proportion of peptides with more than 20 amino acids during flour
 592 digestion (Capriotti et al., 2015). These peptides probably play a nutritional role since
 593 their size belongs to the range (3-51 amino acids) compatible with the absorption
 594 through the intestinal epithelium. However, it should be noted that peptides that exceed
 595 20 amino acids are known to exhibit minimal bioactivity properties (Roberts et al.,
 596 1999). For this reason, we previously filtrated with 3 kDa pore membranes samples
 597 used to determine ORAC and iACE bioactivities. Consequently, the retention of most

598 peptides released during the filtration step could cause the reduced bioactivity values
599 found for samples from soybean flour digestion.

600 **3.2. Recovering bioactive compounds: characterization of by-products**

601 **3.2.1. Protein characterization by size**

602 After applying both methodologies to prepare protein concentrates, we
603 characterized the protein size profile of the supernatant from the classical
604 extraction (acid extraction) and the AP from AMS-based extraction, presumably
605 rich in antinutritional factors. For that, we used size exclusion chromatography
606 (SEC).

607 We identified three main regions when analyzing the chromatograms
608 (Figure 5). The first region (I) corresponds to large proteins and polypeptides, the
609 second one (II) to medium/small peptides, while the third (III) contains free
610 amino acids and small molecules capable of absorbing at 280 nm. We focused
611 our principal interest on the region I since it corresponds to the protein
612 antinutritional factors in soybean flour. Even though they are unwanted
613 compounds for nutritional purposes, they have biological capacities in the health
614 area, making it interesting to recover them intact.

615 Within region I, peaks 1 and 2, with approximate average MW of ~690
616 kDa and ~296 kDa, respectively, may include protein aggregates and the native
617 quaternary structure of glycinin. Peak 3 (~120 kDa MW) may correspond to β -
618 conglycinin (native and denatured) and denatured glycinin. Peak 4 (~72 kDa
619 MW) may include subunits of β -conglycinin (α , α' , and β) and acid subunits of
620 glycinin. On the other hand, peak 5 (~30 kDa MW) may comprise the basic

621 subunits of glycinin, lectin, and the Kunitz-type trypsin inhibitor. The Bowman-
622 Birk type trypsin inhibitor was in peak 6 (~13 kDa MW). The soybean's principal
623 antinutrients are lectin, the Kunitz, and Bowman-Birk trypsin inhibitors, all being
624 the extraction's target molecules. Finally, the peak 7 (~4 kDa MW) may contain a
625 peptide of high commercial value and currently growing interest, lunasin (Seber
626 et al., 2012; Serra et al., 2016; Singh et al., 2017). We fractionated both peaks 5
627 and 6 prior to analysis by mass spectrometry (MALDI-TOF/TOF), thus
628 confirming the presence of the lectin and the trypsin inhibitors.

629 Table A4 (see Annex) shows the areas calculated for each peak in region I
630 and the total area for regions II and III. Neither the micellar extraction with Tg9
631 nor the classical method extracted protein aggregates or glycinin, while the Tg7
632 extracted them. For peak 3, the AP Tg9 differed from the others showing the
633 lowest value, while for peak 4, it only differed from the AP Tg7. Notably, the
634 Tg7 system exhibited the highest leaching ability when the first four peaks were
635 analyzed globally. Concerning antinutritional factors, both the classic method and
636 the AP Tg7 showed to be the best ones to extract Kunitz trypsin inhibitors and
637 lectins. At the same time, the AP Tg9 exhibited the best performance in removing
638 the Bowman-Birk trypsin inhibitor.

639 Additionally, it is worth mentioning that Tg9 evidenced a marked
640 extractive capability for peak 7, which could contain the lunasin. This is a
641 remarkable feature given the high value that this peptide has acquired for its
642 proven beneficial properties for health, namely antioxidant, anti-inflammatory,
643 and chemopreventive (de Mejia et al., 2021; Dong et al., 1995; French et al.,
644 2004; Hao et al., 2020; Pivato et al., 2012; Zhao, Chen, Xue, et al., 2008).
645 Finally, from inspection of regions II and III, the AP Tg9 presented the highest

646 content of small peptides, free amino acids, and small molecules that absorb at
647 280 nm relative to the classic and Tg7 AP.

648 **3.2.2. Extraction and purification of isoflavones**

649 The potential ability to extract and isolate isoflavones of high commercial
650 value is one of the proposed methodology's attractive properties. Table 5 reports
651 isoflavone amounts leached by each system, determined by HPLC. The AMS
652 differed markedly from the control (classical process), exhibiting a higher
653 extractive ability of total isoflavone content. A more detailed analysis showed
654 that the AMS Tg7 stood out from the classical method when extracting the
655 glycosylated forms (daidzin and genistin). However, for the aglycones, those two
656 systems were not different. On the other hand, Tg9 highly exceeded the control at
657 extracting daidzin. However, it led to achieving similar or even lower genistein
658 and daidzein extraction, respectively, probably due to its more hydrophilic nature.
659 Table 5 also reveals that all the extracts have different compositions of
660 isoflavones, with the glycosylated forms being the predominant ones in all cases.
661 These results agree with the higher content of β -glycosides concerning the
662 aglycones in soybean and derivatives. For example, it is well known that the
663 aglycones of soybean flour are approximately 2-3% of the total isoflavone
664 content, while the unconjugated β -glycosides represent 34% of the total
665 isoflavone (Andrade et al., 2016). Table 5 also includes the distribution
666 coefficients (K_d) of isoflavones between the micelle-rich/-poor phases (MP and
667 AP). All the K_d measured were $\gg 1$, thus confirming a marked isoflavones
668 preference for the MP. Table 5 also shows the phase recovery performance at the
669 micellar phase (Pr). The calculation of this efficiency parameter needed the phase
670 volumes in each AMS. The mean MP volumes of the Tg7 and Tg9 systems were

671 10.3 and 9.1 mL, respectively, while their corresponding mean AP volumes were
 672 44.7 and 40.9 mL. The differences in the total volumes recovered were due to the
 673 liquid retained by the solid in each case. Note that the reduced volume of MP
 674 regarding that of AP (four times lower) and Kd values higher than 1 results in
 675 increased isoflavone concentration in the MP. On the other hand, the high found
 676 Pr values demonstrate the remarkable effectiveness of AMS at recovering the
 677 isoflavones in the MP. Considering the extractive and concentrating properties,
 678 the AMS Tg7 was the best system to recover all the isoflavones. It allowed not
 679 only to extract more isoflavones than the traditional method but also to achieve
 680 four to five times higher concentrations. This finding is technologically
 681 promising since it involves a considerable reduction of volumes to be handled,
 682 thus leading to industrially advantageous processes.

683 **Table 5.** Comparison of the amount of isoflavones extracted by the different methodologies.

Isoflavone		Methodology			
		Micellar extraction		Classic extraction	
		Tg7	Tg9		
Aglycones †	Daidzein	Amount ¹	62.0 ± 3.6 ^{a, b}	61.1 ± 1.4 ^a	70.0 ± 3.1 ^b
		Kd ²	23.8 ± 2.5	6.1 ± 0.6 ^a	NA
		Pr ³	85.8 ± 3.1	57.6 ± 2.4	NA
	Genistein	Amount ¹	40.2 ± 2.0 ^a	30.3 ± 1.8 ^a	35.0 ± 2.4 ^a
		Kd ²	14.3 ± 2.7 ^a	14.2 ± 2.8 ^a	NA
		Pr ³	78.7 ± 6.5 ^a	78.2 ± 7.0 ^a	NA
	Daidzin	Amount ¹	490.1 ± 20.3 ^a	513.9 ± 22.6 ^a	183.0 ± 15.8
		Kd ²	4.2 ± 0.2	6.0 ± 0.3	NA
		Pr ³	49.3 ± 1.1	57.2 ± 1.3	NA
Genistin	Amount ¹	770.4 ± 21.4	461.2 ± 4.3 ^a	418.7 ± 15.3 ^a	
	Kd ²	7.4 ± 0.4	11.2 ± 1.1	NA	
	Pr ³	63.0 ± 1.3	71.4 ± 2.0	NA	
Total †	Amount ¹	1362.8 ± 47.2	1066.5 ± 30.1	706.7 ± 36.7	
	Kd ²	6.4 ± 0.4	8.0 ± 0.7	NA	

	Pr ³	59.5 ± 1.5 ^a	64.0 ± 1.9 ^a	NA
--	-----------------	-------------------------	-------------------------	----

† Values are expressed as mean ± SD. ¹ Amount in µg (g of soybean flour)⁻¹. ² Distribution coefficient (Kd). ³ Phase rich in micelles recovery performance (Pr) expressed in %. ^{a, b} Values from the same row that share a superscript do not present statistical differences, given the analysis of their variances (ANOVA) with Tukey's posthoc test for a significance level of 0.05.

684

685 When analyzing our results and those corresponding to other
686 methodologies (Table 6), we found that the amounts of aglycones recovered with
687 the proposed processes are similar or superior to most of them. The extraction
688 with 70% ethanol achieved the highest amount of genistein and daidzein, but the
689 extracted matrix was another soy derivative, such as okara (Jankowiak et al.,
690 2014). When comparing the yields from ethanol and pure water extractions, water
691 alone cannot extract the less hydrophilic isoflavones. However, adding
692 surfactants can revert that (Cao et al., 2012). It is also important to note that direct
693 micelles improve extractive performance. AMS here proposed (Tg7/Tg9) and
694 Triton X-114 AMS (Cordisco et al., 2016) extracted more isoflavones (aglycones
695 and β-glycosides) than those obtained by reverse micelles (Zhao et al., 2010).
696 That suggests that the use of direct micelles improves extractive performance.
697 When MP concentrates the target compounds, the surfactant presence may
698 compromise the applicability of the final product. To solve this problem, in
699 previous work, our research group applied a second extractive step, i.e., a back
700 extraction, to make isoflavones displace from the AM to the AP (Cordisco et al.,
701 2016). It is worth mentioning that the decision to include this step in the process
702 will depend on the final use of isoflavones, i.e., as cosmetics or food ingredients.

703

704 **Table 6.** Soy isoflavones extracted with different methodologies.

Methodology	Source	Amount [†]				Reference
		Daidzein	Genistein	Daidzin	Genistin	
AMS Tg7	Flour	62.00 ± 3.60 ^a	40.20 ± 2.00 ^a	490 ± 20 ^a	770.40 ± 21.40 ^a	**
AMS Tg9	Flour	61.10 ± 1.40 ^a	30.30 ± 1.80 ^{b,c}	514 ± 23 ^a	461.20 ± 4.30 ^b	**
AMS Triton X-114	Flour	142.60 ± 2.60	69.60 ± 0.20	350 ± 8 ^b	736.50 ± 3.30 ^a	(Cordisco et al., 2016)
Water/acetone/ethanol	Flour	NA	38.00 ± 0.01 ^a	382 ± 12 ^b	467.00 ± 8.00 ^b	(Andrade et al., 2016)
Acetonitrile 80%	Bean	36.60 ± 2.00 ^b	36.30 ± 0.40 ^{a,b}	670 ± 18 ^c	644.70 ± 22.40	(M. J. Lee et al., 2015)
Methanol 80%	Bean	22.10 ± 2.50 ^c	26.40 ± 1.30 ^c	631 ± 15 ^c	587.60 ± 2.20	(M. J. Lee et al., 2015)
Water	Okara	22.00 ± 10.00 ^c	3.00 ± 4.00 ^d	108 ± 22	71.00 ± 16.00 ^c	(Jankowiak et al., 2014)
Ethanol 70%	Okara	173.00 ± 8.00	194.00 ± 14.00 [*]	160 ± 7 ^d	171.00 ± 7.00	(Jankowiak et al., 2014)
Reverse AMS Triton X-100	Flour	NA	79.03 ± 4.31	168 ± 5 ^d	118.24 ± 4.98	(Zhao et al., 2010)
Supercritical CO ₂	Flour	30.93 ± 0.04 ^{b,c}	1.71 ± 0.01 ^d	–	53.64 ± 0.06 ^c	(Rostagno et al., 2002)

[†] Amount of isoflavones expressed as mean ± SD, in µg (g of soybean flour)⁻¹. ^{a-d} Values from the same column that share a superscript do not present statistical differences, given the analysis of their variances (ANOVA) with Tukey's posthoc test for a significance level of 0.05. ^{*} Values not included in the analysis due to being out of homoscedasticity (Bartlett's test). ^{**} Values corresponding to the present work.

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706

707 **3.2.3. Extraction of raffinose family oligosaccharides**

708 Soy carbohydrates are largely undesirable due to their low digestibility. In
 709 this regard, the process evaluated here could extract oligosaccharides belonging
 710 to the raffinose family. Table 7 shows that the amount of leached oligosaccharide
 711 by the AMS was 48-53% higher than that of the traditional methodology. So,
 712 both AMS Tg7 and AMS Tg9 had a better extracting performance, i.e., higher
 713 detoxifying capacity. According to the Kd values lower than 1, those
 714 oligosaccharides slightly prefer the AP, probably due to their hydrophilic nature.
 715 This finding, together with the larger volumes of the AP (3.3-4.5 times the MP
 716 volume), are responsible for the high obtained Pr, close to 85% for both
 717 surfactants.

718 **Table 7.** Comparison of the amount of raffinose family oligosaccharides extracted by the
 719 different methodologies.

Methodology		Raffinose family oligosaccharides [†]		
		Amount ¹	Kd ²	Pr ³
Micellar extraction	Tg7	17.9 ± 1.0 ^a	0.76 ± 0.05 ^a	85.1 ± 1.3 ^a
	Tg9	18.5 ± 1.3 ^a	0.75 ± 0.02 ^a	85.7 ± 0.9 ^a
Classic extraction		12.1 ± 0.8	NA	NA

[†] Values are expressed as mean ± SD. ¹ Amount in RU (g of soybean flour)⁻¹. ² Distribution coefficient (Kd). ³ Aqueous phase recovery performance (Pr) expressed in %. ^a Values from the same column that share a superscript do not present statistical differences among themselves, given the analysis of their variances (ANOVA) with Tukey's posthoc test for a significance level of 0.05.

720

721 Considering that it is also possible to separate most of the raffinose family
 722 oligosaccharides from the isoflavones by simply decanting the phases, the
 723 proposed methodology constitutes a better alternative than those currently used.
 724 Besides, soy galactooligosaccharides represent an alternative and economical
 725 carbon source for microbial conversion to value-added products such as succinic

726 acid and ethanol (Thakker et al., 2014). Consequently, the applied AMS-based
727 extraction allows obtaining a by-product for further uses in bio-conversion
728 processes.

729 **4. Conclusions**

730 This study, aimed to perform a novel AMS-based extracting methodology,
731 was driven by the following research questions: -Are SPC from the traditional
732 and proposed methodology of comparable quality? -What about their nutritional
733 and bioactive properties? -Compared to the classical methodology, how is the
734 AMS performing in extracting soluble proteins, antinutrients, and isoflavones? -Is
735 it possible to recover these components separately from the extracts to valorize
736 them? In light of all presented results, it is possible to answer all the questions
737 and conclude:

738 -The AMS-based extractive methodology produced SPC noticeably
739 depleted in trypsin inhibitor content (TIA loss of 90%) with total protein close to
740 60% and variable protein soluble amounts ranging from 19% to 34%, these
741 parameters being similar to those corresponding to SPC from classical methods.
742 The secondary structure content, determined as a fingerprint of the obtained
743 product, showed either alpha helix (SPC Tg7) or random coils (SPC Tg9)
744 increases concerning SPC control (SPCa). This finding might affect their
745 functional properties (emulsifying, solubility, etc.) and open potential new
746 applications. Additionally, remarkable antioxidant and antihypertensive activities,
747 other than high soluble protein content, were detected in peptides released during
748 *in vitro* digestibility assays, thus confirming the high quality of the obtained
749 product.

750 -The AMS-based methodology also exhibited a markedly enhanced extractive
751 performance of raffinose family oligosaccharides (~50% higher than the
752 traditional one), thus resulting in a successful soybean flour detoxifying strategy.
753 Due to its non-destructive character, it allowed recovering raffinose family
754 oligosaccharides and other valuable by-products, such as Kunitz and Bowman-
755 Birk trypsin inhibitors, lectins, and lunasin, potentially applicable in research and
756 fermentation fields. Additionally, these compounds, primarily recovered in the
757 aqueous phase of AMS, were separated from isoflavones (isolated and
758 concentrated in the micelle phase). Regarding this issue, AMS demonstrated
759 improved efficiency in extracting isoflavones, thus exhibiting both selectivity for
760 aglycone/glycone isoflavone forms and high yields, e.g., almost twice as large as
761 that of the traditional method and even higher than those obtained with organic
762 solvents such as methanol. These advantages make AMS a powerful tool for the
763 food and cosmetic industries.

764 Finally, it is possible to affirm that the proposed AMS-based extraction
765 constitutes a sustainable, simple, and scalable alternative that deserves
766 consideration among the new technologies for processing plant derivatives and
767 obtaining more valuable products and by-products.

768

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778

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1022

1023 **Figure Captions**

1024 **Figure 1. Methodology outline.** Flow diagram of the complete methodology, including
1025 the raw material (white soybean flour), the processes applied, the products and by-
1026 products obtained, and the analyses performed. For the processes and analyses, the
1027 subsection number corresponding to their description in the Materials and Methods
1028 section was also indicated.

1029 **Figure 2. Process outline.** Scheme of the proposed methodology to produce SPC with
1030 SMA. ME: micellar extraction; MP: micellar phase; AP: aqueous phase.

1031 **Figure 3. FTIR.** Standardized ATR-FTIR absorbance spectra of soybean flour and
1032 protein concentrates (SPCs). **A)** Full spectrum from 4000 to 800 cm^{-1} . **B)** Most
1033 important characteristic amide regions (I, II and III). Comparison of the amide-I region
1034 of the deconvoluted ATR-FTIR absorbance spectra for: **C)** soybean flour; **D)** SPCa; **E)**
1035 SPC Tg7; **F)** SPC Tg9. The curve fit was performed with Gaussian lines. The peak
1036 position of each component corresponding to the amide band was deduced from the
1037 second derivative spectra. The sum of the fitted curves is shown as a solid line, closely
1038 overlaid the original spectrum, shown as a dashed line (C) or colored line (D, E, and F).

1039 **Figure 4. SGI.** Levels of each response depending on the stage of the SGI. The lines
1040 display the observations for each experimental unit for: **A)** soluble protein (Ps); **B)**

1041 ORAC; C) iACE. Stages of the process: T1, beginning of the gastric stage; T2, end of
1042 gastric stage; T3, end of the intestinal stage.

1043 **Figure 5. Size exclusion chromatography.** Chromatograms (solid lines) of molecular
1044 size distribution of the APs obtained by the classical method and the AMSs of Tg7 and
1045 Tg9. The horizontal dotted lines represent the baseline of each chromatogram, and the
1046 vertical dashed ones divide regions: I, II and III. The numbers represent the peaks
1047 corresponding to region I.

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Annex

Production of soy protein concentrate with the recovery of bioactive compounds: from destruction to valorization

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Nerli

Table A1. Analysis of variance for fitted general linear models.

Response	Source	SS*	DF**	MS***	F	P	R ²
Ps	Model	687	24	28.604	228	0.000	0.996
	Residue	2,510	20	0.126			
	Total	689	44				
ORAC	Model	3557270	24	148219	276	0.000	0.997
	Residue	10759	20	538			
	Total	3568030	44				
iACE	Model	7580240	24	315843	251	0.000	0.997
	Residue	25209	20	1260			
	Total	7605440	44				

*SS, sum of squares; **DF, degrees of freedom; ***MS, mean square.
 P < 0,05 is considered significant.

Table A2. Multiple comparisons for each response by T.

T	Least squares mean †		
	Ps ¹	ORAC ²	iACE ³
T1	2.59 ± 0.09	51 ± 6	1015 ± 9
T2	9.63 ± 0.09	460 ± 6	283 ± 9
T3	8.37 ± 0.09	577 ± 6	57 ± 9

† Values are expressed on dry basis, as mean ± SEM calculated by least squares. ¹ Ps in mg (g of product)⁻¹, ² ORAC in μmol TE (g of product)⁻¹, ³ iACE as IC₅₀, μg mL⁻¹. All the values in the same column present statistical differences among themselves, given the analysis of their variances (ANOVA) with Tukey's posthoc test for a significance level of 0.05.

Table A3. Multiple comparisons for each response by product.

Product	Least squares mean †
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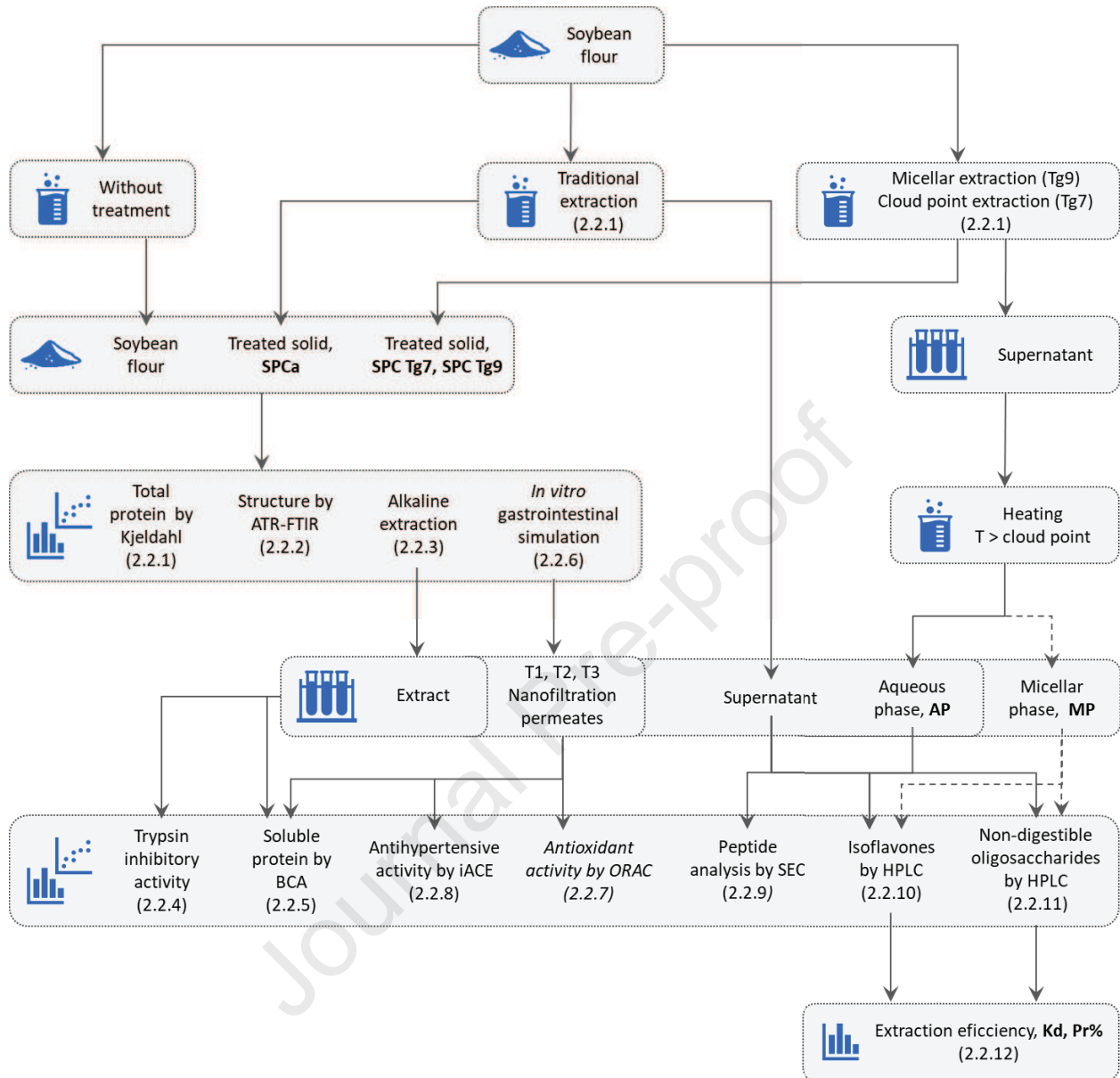
	Ps ¹	ORAC ²	iACE ³
Flour	6.3 ± 0.3 ^a	473 ± 13 ^a	452 ± 12 ^{a, b}
SPCa	7.5 ± 0.3 ^a	326 ± 13	428 ± 12 ^a
SPC Tg7	4.8 ± 0.3	178 ± 13	489 ± 12 ^b
SPC Tg9	6.9 ± 0.3 ^a	534 ± 13 ^a	431 ± 12 ^a

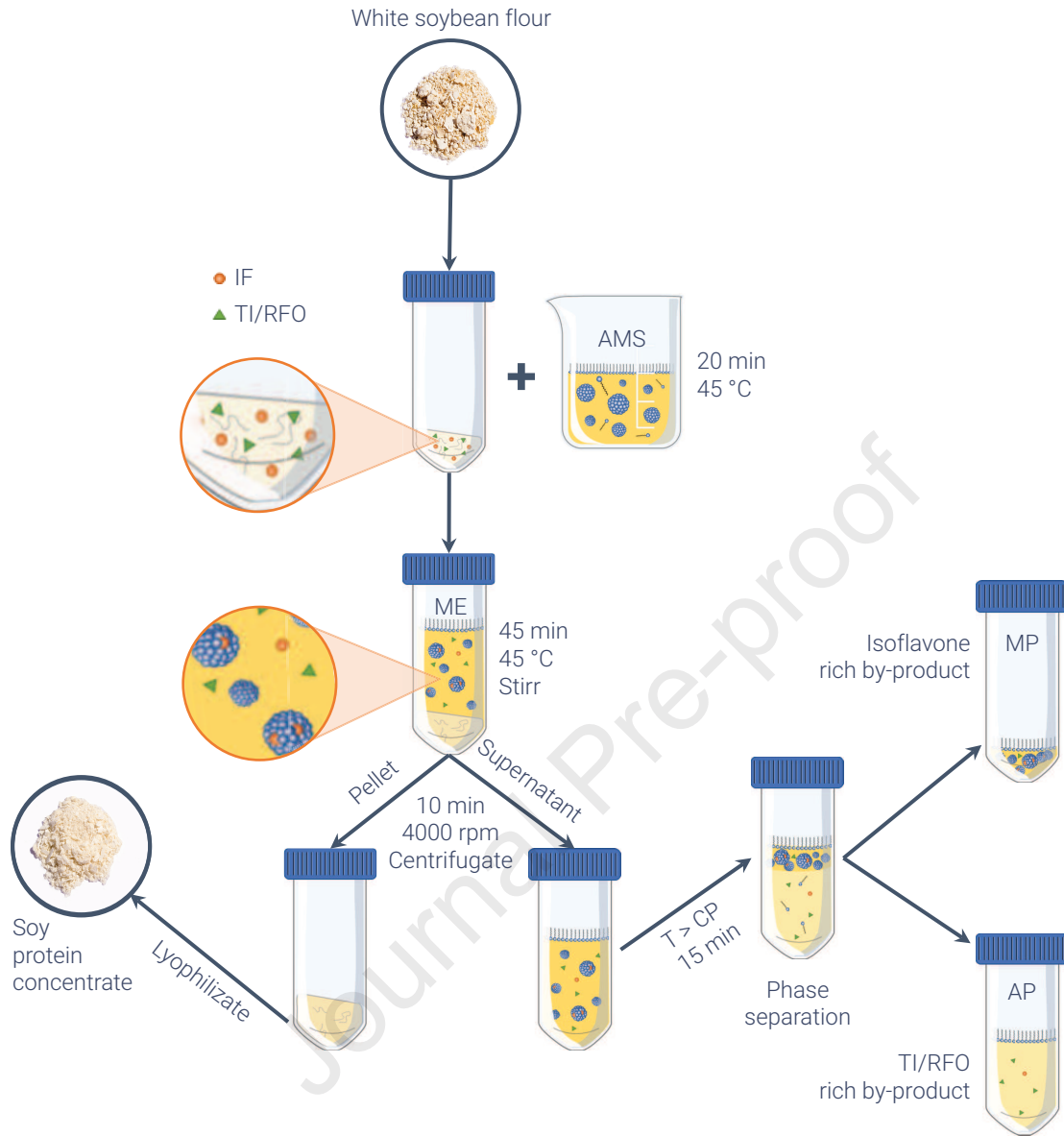
† Values are expressed on a dry basis, as mean ± SEM calculated by least squares. ¹ Ps in mg (g of product) ⁻¹, ² ORAC in μmol TE (g of product) ⁻¹, ³ iACE as IC₅₀, μg mL⁻¹. ^{a, b} Values from the same column that share a superscript do not present statistical differences among themselves, given the analysis of their variances (ANOVA) with Tukey's posthoc test for a significance level of 0.05.

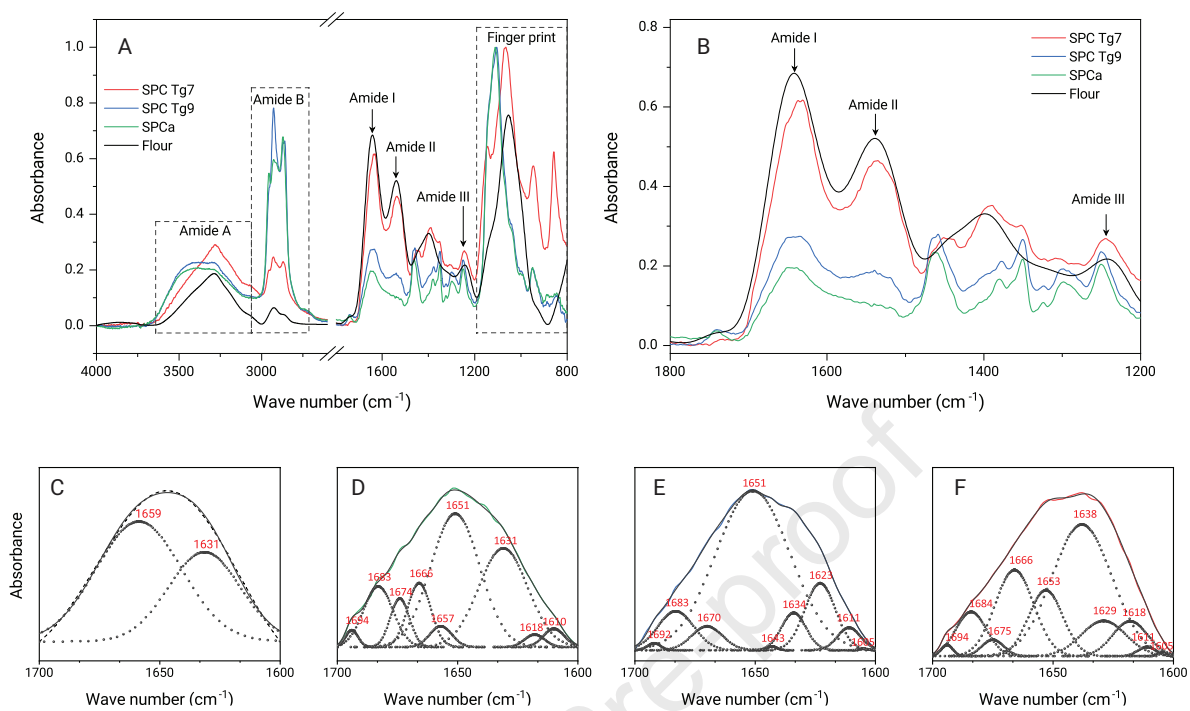
Table A4. Peak areas belonging to the region I and total areas of regions II and III.

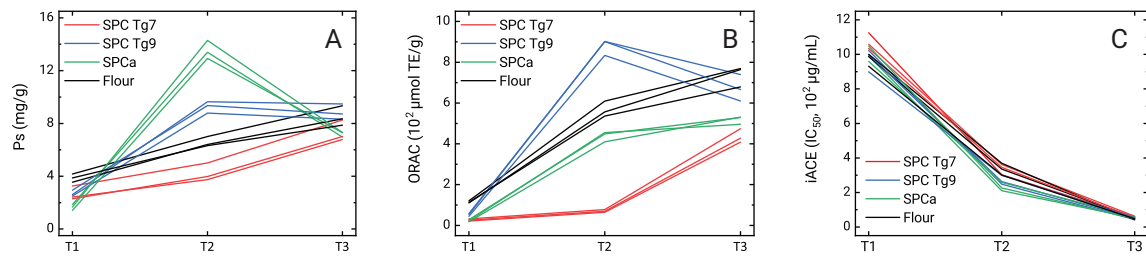
Region	Peak	Area (mL*mAU) †		
		Tg7 AP	Tg9 AP	Classic AP
I	1	1.6 ± 0.1	NA	NA
	2	2.5 ± 0.2	NA	NA
	3	7.3 ± 0.5 ^a	5.4 ± 0.5	7.3 ± 0.6 ^a
	4	4.7 ± 0.3 ^a	4.5 ± 0.3 ^a	4.8 ± 0.4 ^a
	5	11.2 ± 0.8 ^a	7.3 ± 0.5	14.4 ± 1.0 ^a
	6	4.0 ± 0.2	5.8 ± 0.5	3.1 ± 0.2
	7	2.4 ± 0.1	5.1 ± 0.3	1.1 ± 0.1
II		49.6 ± 4.2 ^a	77.1 ± 3.9	49.2 ± 3.2 ^a
III		66.3 ± 4.0	94.3 ± 7.1	51.3 ± 2.3

† Values are expressed as mean ± SD. ^{a, b} Values from the same row that share a superscript do not present statistical differences among themselves, given the analysis of their variances (ANOVA) with Tukey's posthoc test for a significance level of 0.05.

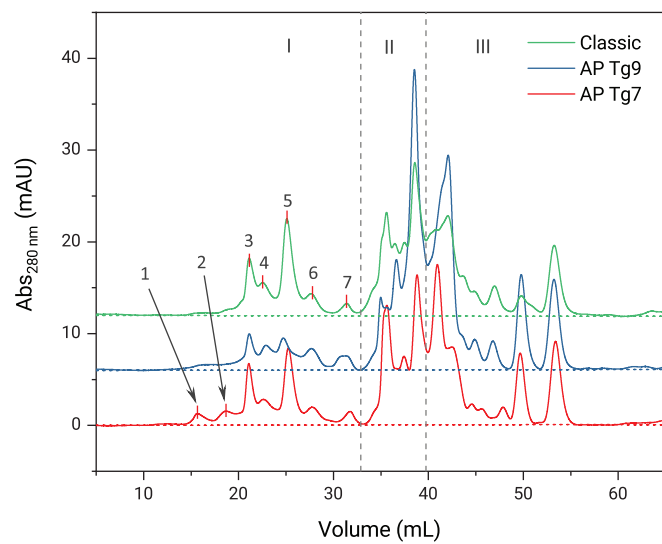








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Highlights

Aqueous micellar systems (AMS) allowed producing soy protein concentrates (SPC)

Quality of SPC from AMS was similar to that of SPC from classical acid washing method

SPC from AMS showed remarkable antioxidant and antihypertensive activities

Trypsin inhibitors and non-digestible oligosaccharides were recovered as by-products

Isoflavones were concentrated and separated from antinutrients

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CRedit author statement

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Manuela Pintado: Writing - Review & Editing, Supervision, Project administration, Funding acquisition. **Bibiana B. Nerli:** Conceptualization, Resources, Writing - Review & Editing,

Supervision, Project administration.

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Declaration of interests

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

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