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# Hydrogen sorption kinetics of magnesium hydride enhanced by the addition of $Zr_8Ni_{21}$ alloy

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#### ABSTRACT

Hydrogen absorption and desorption kinetics, and thermodynamics of MgH<sub>2</sub> ball milled with addition of the  $Zr_8Ni_{21}$  alloy have been studied. Different additive amounts were used from 3 to 12.5 wt%. The highest reversible capacity of 6.5 wt% of hydrogen was found for the samples with 3 and 5 wt% of additive. The best reaction kinetics was found with 10 wt% of additive: 5.9 wt% H<sub>2</sub> was desorbed in 4 min at 300 °C and 0.1 bar of hydrogen pressure. Regardless of the different storage capacities, all the samples were almost fully hydrided in 1 min using a hydrogen pressure of 10 bar at 250 and 300 °C. The enthalpy of formation of magnesium hydride was not affected by the presence of the additive.

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#### 1. Introduction

Magnesium hydride is one of the most studied materials for hydrogen storage in solid state. It is characterized by high gravimetric capacity and good reversibility of the hydrogen absorption/desorption (a/d) process, but has the handicap of a too high desorption temperature (around 300 °C, due to the rather high value of the formation enthalpy, 76 kJ/mol) and a sluggish hydrogen a/d kinetics. It is also abundant, cheap and environment friendly. While it is very difficult to modify the thermodynamics, it has been shown that the comminution of the hydride particles by high energy milling along with the use of additives like metal oxides [1,2] or transition metals [3–6] significantly improves the a/d kinetics.

Recently, attention has been paid to the study of catalytic properties of multicomponent alloys composed by transition metals [7–10]. Dehouche et al. observed that MgH<sub>2</sub> ball-milled with some Zr–Ni alloys exhibited an improved a/d kinetics, which also depended on the stoichiometry of the alloy [11]. More precisely, the eutectoid composition  $Zr_{36}Ni_{64}$  formed by the two crystalline phases  $Zr_7Ni_{10}$  and  $Zr_8Ni_{21}$  [12] showed a faster kinetics than  $Zr_7Ni_{10}$  and  $Zr_9Ni_{11}$ . This motivated the question about

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the influence of the  $Zr_8Ni_{21}$  phase on the a/d kinetics. In a study of hydride-forming alloys in nickel-metal batteries Ruiz et al. observed that  $Zr_8Ni_{21}$  had a better charge/discharge performance than  $Zr_7Ni_{10}$  and  $Zr_9Ni_{11}$  [13].

On the basis of the previous considerations, we have studied  $MgH_2$  powders ball milled with  $Zr_8Ni_{21}$ , analyzing the corresponding activation process and a/d hydrogen kinetic and thermodynamic properties.

#### 2. Materials and methods

The  $Zr_8Ni_{21}$  alloy was prepared by arc-melting the elements Zr and Ni under Ar atmosphere inside a water cooled copper crucible in order to avoid contamination. The purities were 99.9% for Zr and Ni, and 99.999% for Ar. A reduction of contamination from the furnace atmosphere was obtained by melting a sacrificial button before Zr and Ni melting. The arc was established by a torch with tungsten tip. The additive was remelted three times to ensure homogeneity. Then, it was wrapped in a Ta foil which is a getter of oxygen and annealed for 30 days at 1000 °C inside an evacuated quartz capsule. Thereafter, several cycles of heating and cooling from ambient temperature to 250 °C at 15 bar of hydrogen were performed on the alloy to make it brittle and so facilitate its reduction into small pieces by crushing.

MgH<sub>2</sub> powder, supplied by Goldschmidt (95% MgH<sub>2</sub> + 5% Mg), was ball milled under Ar atmosphere with the amounts indicated below the obtained  $Zr_8Ni_{21}$  grains for 20 h in a hardened steel vial using a SPEX-8000 shaker mill with a ball to powder ratio 10:1. Five different MgH<sub>2</sub>-*x* wt%  $Zr_8Ni_{21}$  compounds, with *x* = 12.5, 10, 7.5, 5, 3, labelled 12.5 cat, ..., 3 cat, respectively, were synthesized. Sample handling was carried out inside a M-Braun glove box filled with Ar (contamination levels lower than 1 ppm for oxygen and 0.1 ppm for water).

The hydrogen a/d process was studied by means of a Sievert's type apparatus supplied by Advanced Materials Co. Before each a/d measurement the samples were dehydrided for 1 h at 250 °C and  $4 \times 10^{-4}$  bar. The kinetic data were obtained by

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Fig. 1. SEM image of MgH\_2–10 wt%  $\rm Zr_8Ni_{21}$  obtained with backscattered electrons. The white spots correspond to the additive particles and the grey regions to the MgH\_2 matrix.

measuring the hydrogen pressure in calibrated reservoirs connected to the sample chamber by valves. In the absorption experiments, the pressure in a small reservoir was set at 10 bar before valve opening. In the desorption experiments, the hydrided sample was connected to an evacuated larger reservoir. Due to the gaseous hydrogen present in the sample holder, there was a rise in the reservoir pressure of approximately 0.1 bar immediately after the valve opening. We took this value as the output pressure during desorption. Powder X-ray diffraction (XRD) patterns were measured by a Philips PW 1820/00 diffractometer using the Cu-K\alpha radiation. The samples were placed into the sample holder and covered with an 8  $\mu$ m kapton foil inside the glove box in order to avoid air contamination. A blank measurement performed on only kapton foils showed two broad diffraction peaks below 20° that did not interfere with the patterns of the phases under analysis. Scanning electron microscopy (SEM) observations were performed by using a Cambridge Stereoscan 440 SEM equipped with Philips PV5800 EDS.

# 3. Results and discussion

The catalyzed hydride powders obtained after 20 h milling display a homogeneous distribution of the additive particles, which can be well distinguished from the MgH<sub>2</sub> in the SEM image of sample 10 cat reported in Fig. 1. The white spots, with size not exceeding 1  $\mu$ m, are due to the elastic collisions of backscattered electrons with the heavy nuclei of zirconium, while the grey weak region is due to the light nuclei of magnesium hydride.

#### 3.1. Activation of samples

Ten cycles of hydrogen a/d at 250 °C were performed for the activation of all samples and an extra cycle at 300 °C in the special case of sample 3 cat. The result of the activation cycles was a stabilized absorption kinetics. In Fig. 2 are shown the absorption curves for the 1st, 5th, and 10th cycles of sample 10 cat at 250 °C and 10 bar. The hydrogen absorbed within 1 min was 4.8, 5.2 and 5.7 wt%, respectively, which is an increment of 19% after 10 cycles. This can be due to the mechanical stress produced by expansion and contraction during cycling that may comminute the magnesium particles by cracking and change their surface extension and characteristics. This transformation may allow hydrogen to react with material that was previously inaccessible. Dehouche et al. suggested that in their Zr-Ni doped compounds rougher surfaces may be due to the formation of nanochannels that facilitate the hydrogen access to the particle bulk [11]. The improvement continues up to 10 cycles and then a steady state is reached, as seen with subsequent cycles from the 10th to 16th. The need of a/d cycles to reach the optimal sorption properties has been reported for other Mg-based hydrides (e.g. the  $Mg + Mg_2Ni$  composite [5]).

The milling and activation processes also introduce changes in the crystalline structure and chemical composition. In Fig. 3,



Fig. 2. Absorption curves at  $250 \degree C$  and 10 bar for the sample MgH<sub>2</sub>-10 wt% Zr<sub>8</sub>Ni<sub>21</sub>.

the XRD patterns of an as-milled (bottom) and an activated (top) hydrided sample are shown. The broad peaks of the as milled sample are due to the reduced size of the grains, the lattice strain and the structural defects produced by high energy milling. There is a major contribution of  $\beta$ -MgH<sub>2</sub> and a lower one of  $\gamma$ -MgH<sub>2</sub>: the former is the equilibrium phase of magnesium hydride, the latter is a high pressure metastable phase typically generated by milling. The pattern exhibits low intensity peaks of pure Mg, present in the commercial magnesium hydride, and also a peak of Mg<sub>2</sub>Ni. The Mg<sub>2</sub>Ni may be originated by a mechanically driven solid-state displacement reaction, where Ni moves from the Zr<sub>8</sub>Ni<sub>21</sub> additive into MgH<sub>2</sub>. The Mg<sub>2</sub>Ni formation was also found by other authors in similar experiments [5,11]. Little contributions of MgO by air contamination during material handling, milling process or X-ray measurements cannot be ruled out.

After activation with hydrogen a/d cycles, the diffraction peaks of a hydrided sample are sharper, this fact being due to the relaxation of strain and reduction of structural defects. The disappearance of  $\gamma$ -MgH<sub>2</sub> peaks testifies that magnesium hydride relaxed completely to the  $\beta$ -phase. The increment in Mg<sub>2</sub>Ni intensity and formation of Mg<sub>2</sub>NiH<sub>4</sub> indicate that Ni continues reacting with Mg during a/d cycling. The peak of ZrH<sub>2</sub>, not observed in the as-milled sample, may be produced by the remaining Zr after the mentioned Mg–Ni reaction, the possibility of which is also suggested by the experiments of Ebrahimi-Purkani and Kashani-Bozorg on ball-milled Mg and Ni [14]. Their differential scanning



Fig. 3. Diffraction patterns of  $MgH_2-10\,wt\%$   $Zr_8Ni_{21}$  as-milled (bottom) and hydrided after cycling (top).



Fig. 4. Hydrogen storage capacity of catalyzed  $MgH_2$  as a function of additive amount and temperature. The empty portion of the bars corresponds to the theoretical capacity (see text).

calorimetry measurements showed that the Mg–Ni reaction was thermally activated at 250 °C, the temperature at which we performed the a/d cycles. The Mg<sub>2</sub>Ni is possibly produced in our case at the interfaces between MgH<sub>2</sub> and Zr<sub>8</sub>Ni<sub>21</sub> particles, yielding MgH<sub>2</sub> particles superficially covered by Mg<sub>2</sub>Ni. This is a possible explanation of part of the improved sorption properties which will be reported in the following. Finally, diffraction peaks corresponding to MgO and dehydrided Mg and Mg<sub>2</sub>Ni are also observed, accounting for the hydrogen capacity reduction in comparison with the theoretical value.

In Fig. 4 is shown the weight percentage of hydrogen reversibly absorbed by the five compounds at a reservoir pressure of 10 bar for 1 h, period long enough to ensure the saturation of all samples. The dark and light grey bars correspond to the sample temperatures of 250 and 300 °C, respectively. The empty portion of the bars represents the extra capacity that would have been measured if all the magnesium of the compound had been hydrided. Taking into account that magnesium hydride theoretically stores 7.6 wt% of hydrogen, the resulting capacity is 7.6•(1 - x/100) wt%. As said, the discrepancies between the two values are due to the presence of MgO and unreacted material. The storage capacity is almost the same at both temperatures: for the sample 10 cat the values are 6.1 and 5.9 wt% for T = 250 and 300 °C, respectively, in agreement with the values reported by Dehouche et al. for magnesium hydride doped with 10 wt%  $Zr_{36}Ni_{64}$  [11]. According to Fig. 4, the highest storage capacity of 6.5 wt% is found for samples 3 cat and 5 cat.

# 3.2. Effect of the additive amount on kinetics of activated samples

The absorption kinetics of magnesium hydride with  $Zr_8Ni_{21}$  additive at 250 and 300 °C and 10 bar is shown in Fig. 5. The best rate at 250 °C is obtained with 5 wt% of  $Zr_8Ni_{21}$ :5.3 wt% of  $H_2$  in 16 s. It is observed that the absorption kinetics does not depend strongly on the additive amount and that all the samples reached 80% of the storage capacity in 30 s and 90% in 1 min at both temperatures. Since the absorption rate depends on the difference between the reservoir and equilibrium pressures, a slowing down of kinetics is expected at T = 300 °C, as seen in Fig. 5. For instance, sample 10 cat reaches 80% of the storage capacity in 25 s at T = 300 °C and in 19 s at T = 250 °C. These values are slightly better than those reported by Barkhordarian et al. for absorption measurements in similar



Fig. 5. Hydrogen absorption at 10 bar of catalyzed  $\mbox{MgH}_2$  for different additive amounts.

conditions of  $0.2 \text{ mol}\% \text{ Nb}_2\text{O}_5$  doped MgH<sub>2</sub> milled for 20 h or more [2].

The most interesting results are observed during desorption. In Fig. 6, which reports the amount of hydrogen desorbed by completely hydrided samples connected to a reservoir at 0.1 bar and T = 300 °C, is shown that all samples desorb completely in 4 min, except the sample 3 cat that took 8 min. The maximum desorption rate (calculated from the minimum of the numerical derivative of each curve) is reported in Fig. 7 as a function of the amount of additive, showing that the best value of 3.8 wt%/s is obtained for sample 10 cat. A higher additive amount may not introduce extra benefits but only reduction of storage capacity. The samples were desorbed in a finite volume reservoir, where pressure increased lightly during desorption, so the reported kinetics might be underestimated.



Fig. 6. Hydrogen desorption of catalyzed MgH<sub>2</sub> at 300 °C and 0.1 bar.



Fig. 7. Maximum desorption rate at  $T = 300 \circ C$  and 0.1 bar of catalyzed MgH<sub>2</sub>.

Similar values of desorption kinetics are reported for 0.5 mol% Nb<sub>2</sub>O<sub>5</sub> doped MgH<sub>2</sub> milled for 20 h or more [2].

# 3.3. Thermodynamic behaviour

Fig. 8 shows the absorption and desorption pressurecomposition isotherms (PCI) at 250 and 300 °C. The pressure of coexistence between the partially hydrided compound and the gaseous hydrogen is given by the plateau pressure calculated by average of all the plateau points at the given temperature. At 250 °C the absorption and desorption plateau pressure are very close, 0.44 and 0.37 bar, respectively. At 300 °C both pressures have, within the experimental error, the same value of 1.94 bar. This means that for the MgH<sub>2</sub> catalyzed by the Zr<sub>8</sub>Ni<sub>21</sub> alloy, there is a small hysteresis between absorption and desorption curves measured at the same temperature. The hysteresis is originated by strain and disorder of the MgH<sub>2</sub> lattice, due to expansion during absorption, higher if compared with relaxed strain and disorder during desorption: higher strain and disorder increase the plateau pressure, which is lowered by their relaxation [15]. The low hysteresis in the present case may be due to the presence of the additive which, being unstable, favours lattice mobility and therefore less stress during the formation of MgH<sub>2</sub>. The lattice mobility is higher at high temperature and consequently the hysteresis decreases. Hints of a second plateau is suggested by the shoulder in the absorption curve, produced by hydriding of little amounts of Mg<sub>2</sub>Ni, seen also in the corresponding XRD pattern of Fig. 3, which has a higher plateau pressure than magnesium hydride. The formation of Mg<sub>2</sub>Ni was



Fig. 8. PCI curves at 250 °C (black) and 300 °C (grey) for MgH<sub>2</sub>-10 wt% Zr<sub>8</sub>Ni<sub>21</sub>.



**Fig. 9.** van't Hoff plots of hydrogen a/d for MgH<sub>2</sub>-10 wt% Zr<sub>8</sub>Ni<sub>21</sub>.

also reported for other MgH<sub>2</sub> samples with additives containing Ni (see e.g. Refs. [3,16,17]).

The enthalpy and entropy of the reaction were obtained by the van't Hoff plots of Fig. 9, resulting to be  $\Delta H = -73.9 \pm 0.7$  and  $-77.7 \pm 0.8$  kJ/mol and  $\Delta S = 134.2 \pm 1.2$  and  $141.8 \pm 1.5$  kJ/mol for absorption and desorption, respectively, in agreement with previous data (see, e.g., Ref. [16]), proving once more that the use of an additive to MgH<sub>2</sub> does not change the thermodynamic properties of hydrogen a/d process.

## 4. Conclusions

Hydrogen absorption and desorption kinetics of MgH<sub>2</sub> could be improved by adding  $Zr_8Ni_{21}$  as reaction catalyst up to the limit of 10 wt%. For this composition the maximum desorption rate was found to be 3.8 wt%/s and complete desorption occurred in 4 min at 300 °C and 0.1 bar of hydrogen pressure. These values are similar to the best results found in literature. A hydrogen storage capacity of 5.9 wt% at 250 °C and of 6.1 wt% at 300 °C vs. the theoretical value of 6.8 wt% was found, due to the presence of Mg oxide and inactive Mg and Mg<sub>2</sub>Ni. The highest hydrogen reversible capacity of 6.5 wt% at 300 °C was obtained with the samples with less additive amount. The kinetic behaviour did not change after 10 hydrogen a/d cycles onwards. The thermodynamic properties of MgH2 are not modified by the additive within the experimental error.

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