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# Non-isothermal reaction mechanism and kinetic analysis for the synthesis of monoclinic lithium zirconate ( $m\text{-Li}_2\text{ZrO}_3$ ) during solid-state reaction

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## Abstract

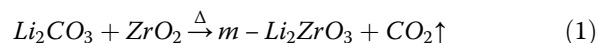
Non-isothermal reaction mechanism and kinetic analysis for the synthesis of monoclinic lithium zirconate ( $m\text{-Li}_2\text{ZrO}_3$ ) were investigated by processing of TG-DTA, along with XRD, DLS, and HRTEM. For this purpose, the solid-state reaction of  $\text{Li}_2\text{CO}_3$  with  $\text{ZrO}_2$  was carried out by TG-DTA at different heating rates (10, 20, and 30 °C/min) from room temperature to 1100 °C. The thermal data was used to calculate the kinetic parameters by two types of isoconversional methods: Flynn-Wall-Ozawa (FWO) and Kissinger-Akahira-Sunose (KAS). The reaction mechanism was determined by the model-fitting method, applying the Coats-Redfern (CR) approximation to the different solid-state reaction models. The results confirmed the formation of pure  $m\text{-Li}_2\text{ZrO}_3$ , consists of semispherical particles of about 490 nm, using a very short reaction time. The average activation energy obtained by FWO and KAS methods were 274.73 and 272.50 kJ/mol, respectively. It was found that the formation of  $m\text{-Li}_2\text{ZrO}_3$  from  $\text{Li}_2\text{CO}_3$  with  $\text{ZrO}_2$  is governed by the three-dimensional diffusion mechanism. Based on these results, a microscopic reaction model of the formation of  $m\text{-Li}_2\text{ZrO}_3$  was proposed.

**Keywords:**  $m\text{-Li}_2\text{ZrO}_3$ , Solid-state reaction kinetics, Non-isothermal, TG-DTA, XRD

## Introduction

Monoclinic lithium zirconate ( $m\text{-Li}_2\text{ZrO}_3$ ) is a ceramic material that has potential applications in different fields including solid-state lithium-ion batteries (Dong et al. 2015; Sherstobitova et al. 2016; Zhan et al. 2018), solid sorbent for  $\text{CO}_2$  capture (Ida and Lin 2003; Kordatos et al. 2017; Chattaraj 2017), and nuclear reactors (Taddia et al. 2005; Oyaidzu et al. 2006; Chitnis et al. 2018). While  $m\text{-Li}_2\text{ZrO}_3$  is conventionally prepared via solid-state reaction of  $\text{Li}_2\text{CO}_3$  with  $\text{ZrO}_2$  (see Eq.(1)) (Wyers and Cordfunke 1989; Pfeiffer and Knowles 2004; Sree Rama Murthy et al. 2017), its formation kinetics has not been reported in the scientific literature. In the

bibliographic review on reaction kinetics, a study was found on the decomposition of  $m\text{-Li}_2\text{ZrO}_3$  into  $\text{ZrO}_2$  (Pfeiffer and Knowles 2004). It is worth highlighting the fact that the knowledge of the reaction kinetics and mechanism are very important in order to optimize the solid-state process for large-scale production and advanced applications. Moreover, reasonable mechanistic conclusions can be drawn from the kinetic data (Lu and Wu 2008; Mandal 2014).



Some of the analytical methods used to study the reaction kinetics in the solid-state are thermogravimetric analysis (TGA), differential-thermal analysis (DTA), X-ray diffraction (XRD), differential-scanning calorimetry (DSC), and nuclear magnetic resonance (NMR) (Mandal 2014; Vyazovkin et al. 2011; Khawam and Flanagan

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2006; Ghuge and Mandal 2017). For any one of these methods, the measured parameter must be able to be transformed into the change in extent of reaction ( $\alpha$ ), which can be used in the kinetics analysis by either iso-conversional (model-free) or model-fitting (Khawam and Flanagan 2006). The combination of both methods can result in a more complete kinetics analysis (Lv et al. 2018; Khawam and Flanagan 2005; Pratap et al. 2007). The most common analytical method used in kinetic analysis is TGA due its simplicity and good repeatability (Khawam and Flanagan 2006; Ghuge and Mandal 2017; Ebrahimi-Kahrizsangi and Abbasi 2008; Jiang and Wei 2018; Liu et al. 2020; Marinović-Cincović et al. 2013). It has been involved in the study, only by model-fitting method, of the reaction kinetics for the synthesis of other Li-based ceramics such as  $\text{Li}_2\text{TiO}_3$  (Mandal 2014),  $\text{LiDyO}_2$  (Ghugue and Mandal 2017), and  $\text{LiNiO}_2$  (Lu and Wei-Cheng 2000).

In this context, the aim of this work is to study the reaction mechanism and kinetics analysis of  $\text{m-Li}_2\text{ZrO}_3$  in a solid-state reaction of  $\text{Li}_2\text{CO}_3$  and  $\text{ZrO}_2$  by TGA, along with DTA, XRD, dynamic light scattering (DLS), and high-resolution transmission electron microscopy HRTEM, by both isoconversional (model-free) and model-fitting methods, considering the relationship between  $\alpha$  and reaction temperature during heating. For this purpose, the kinetic parameters (activation energy:  $E_a$ , and pre-exponential factor:  $A$ ) were calculated by two types of isoconversional methods: Flynn-Wall-Ozawa (FWO) and Kissinger-Akahira-Sunose (KAS) (Vyazovkin et al. 2011; Khawam and Flanagan 2006; Jiang and Wei 2018). Moreover, the reaction kinetics was determined by the model-fitting method, applying the Coats-Redfern (CR) approximation to the different solid-state reaction models (nucleation, diffusion, geometrical contraction, and reaction order model) (Khawam and Flanagan 2006; Ghuge and Mandal 2017; Lv et al. 2018; Miličević et al. 2017). To the best of our knowledge, this is the first report on the non-isothermal reaction mechanism and kinetic analysis for the synthesis of  $\text{m-Li}_2\text{ZrO}_3$ .

## Experimental procedure

### Materials preparation and characterization

$\text{m-Li}_2\text{ZrO}_3$  was prepared by using  $\text{Li}_2\text{CO}_3$  (Cicarelli, 99%) and  $\text{ZrO}_2$  (Tosoh, 99.9%) as the starting materials. Both the reactants were ball-milled with ethanol ( $\text{C}_2\text{H}_6\text{O}$ ) for 20 h at 60 rpm using  $\text{ZrO}_2$  balls (2 cm in diameter). The obtained mixture was dried in an oven at 110 °C, and homogenized by grinding and sieving (#100) processes. Finally, the reaction was conducted by TG-DTA (Rigaku, Evo2) from room temperature to 1100 °C, at three different heating rates (10, 20, and 30 °C/min) under air atmosphere. The measurement conditions were as follows: sample weight 80–82 mg, gas flow 50

ml/min, and alumina pan. For the analysis of phase formation, the reaction of the precursor was also conducted by heating in an electrical furnace at different temperatures under similar conditions to TG-DTA experiments. After cooling at room temperature, the samples were characterized by XRD (Philips, PW3710) with  $\text{Cu-K}\alpha$  radiation ( $\lambda = 0.154$  nm), operating at 35 kV and 40 mA, in the  $2\theta$  range of 15–80° with a step width of 0.04°. The average particle size ( $D$ ) of the as-prepared samples was obtained by DLS (Brookhaven, 90Plus) with a solid-state laser ( $\lambda = 658$  nm) and scattering angle of 90°. For this purpose, sample suspensions were prepared using  $10^{-3}$  M KCl solutions and sonicated for 30 min. The morphology and microstructure of pure  $\text{m-Li}_2\text{ZrO}_3$  were examined by HRTEM (FEI Talos, F200X).

### Kinetic analysis

Based on TGA, the change in extent of reaction or conversion rate ( $\alpha$ ), and the non-isothermal rate of the solid-state reaction ( $d\alpha/dT$ ) can be described by Eqs. (2) and (3), respectively (Vyazovkin et al. 2011; Li et al. 2020; Trawiński et al. 2020; Vyazovkin et al. 2014).

$$\alpha = \frac{m_i - m_t}{m_i - m_\infty} \quad (2)$$

Where,  $m_i$ ,  $m_t$ , and  $m_\infty$  are initial weight of the  $\text{Li}_2\text{CO}_3$ - $\text{ZrO}_2$  mixture, the reactant weight at time  $t$ , and the final weight at the end of reaction, respectively. This data was obtained from TGA results.

$$\frac{d\alpha}{dT} = \frac{A}{\beta} e^{-\frac{E_a}{RT}} f(\alpha) \quad (3)$$

Where,  $A$ ,  $\beta$ ,  $E_a$ ,  $R$ , and  $f(\alpha)$  are the pre-exponential factor, the heating rate, the activation energy, the universal gas constant, and the differential form of the kinetic model, respectively. Equation (3) can be expressed in integral form by Eq. (4), considering the integral reaction model  $g(\alpha)$ , which is defined by Eq. (5) (Vyazovkin et al. 2011; Khawam and Flanagan 2006; Ebrahimi-Kahrizsangi and Abbasi 2008).

$$g(\alpha) = \frac{A}{\beta} \int_0^T e^{-\frac{E_a}{RT}} dT \quad (4)$$

$$g(\alpha) = \int_0^T \frac{d\alpha}{f(\alpha)} \quad (5)$$

Kinetic analysis can be used to describe a thermally active process by determining three factors: activation energy, pre-exponential factor, and reaction model (Jiang and Wei 2018). Two methods, that is, the isoconversional (model-free) and model-fitting can be used to study the kinetics of a solid-state reaction. Typically, isoconversional methods have been used to determine the

activation energy and pre-exponential factor without assuming any particular form of the reaction model, while model fitting method is used to determine the reaction model (Vyazovkin et al. 2011; Khawam and Flanagan 2006; Lee et al. 2016). Therefore, the combination of both methods was used in this work in order to obtain a complete description of the solid-state reaction of  $\text{Li}_2\text{CO}_3$  and  $\text{ZrO}_2$  to form  $m\text{-Li}_2\text{ZrO}_3$ .

#### Isoconversional (model-free) methods

All the isoconversional methods assume that the activation energy corresponding to the same conversion rate remains the same under different conditions of temperature rise. Here, the kinetic parameters are obtained without assuming the reaction model. Because the integral in Eq. (4) does not have an analytical solution, a number of approximate solutions were developed. Many of these approximations give rise to linear equations, such as the Flynn-Wall-Ozawa (FWO) and Kissinger-Akahira-Sunose (KAS) methods, which are described by Eq. (6) and (7), respectively (Vyazovkin et al. 2011; Jiang and Wei 2018).

$$\ln \beta = -1.052 \frac{E_a}{R.T} + \ln \left( \frac{A.E_a}{R.g(\alpha)} \right) - 5.331 \quad (6)$$

$$\ln \left( \frac{\beta}{T^2} \right) = -\frac{E_a}{R.T} + \ln \left( \frac{A.R}{E_a.g(\alpha)} \right) \quad (7)$$

These equations are relatively simple to solve by applying linear regression analysis (Vyazovkin et al. 2011), making it possible to calculate the kinetic parameters involved in every equation. This procedure was as follows:

- $\alpha$  versus  $T$  was obtained from TGA results at three different heating rates (10, 20, and 30 °C/min). The values of  $\alpha$  were chosen between 0.1 and 0.9 (Vyazovkin et al. 2020) with a step of 0.05.
- By using the slope-intercept form of a linear equation ( $y=mx+b$ , where  $m$  is the slope and  $b$  is the  $y$ -intercept), Eq. (6) and (7) can be expressed by Eq. (8) and (9), respectively.

$$\ln \beta = y_{\text{FWO}} = m_{\text{FWO}} \left( \frac{1}{T} \right) + b_{\text{FWO}} \quad (8)$$

$$\ln \left( \frac{\beta}{T^2} \right) = y_{\text{KAS}} = m_{\text{KAS}} \left( \frac{1}{T} \right) + b_{\text{KAS}} \quad (9)$$

Therefore, the values of  $\ln \beta$  (FWO method) and  $\ln(\beta/T^2)$  (KAS method) versus  $(1/T)$  were plotted at the same

value of  $\alpha$  (from  $\alpha$  versus  $T$  relationships obtained at different heating rates), respectively.

- The activation energy and pre-exponential factor were determined from the slopes and intercepts, in each case (Lv et al. 2018; Jiang and Wei 2018), which, according to Eqs. (6)–(9), can be described as follows:

$$Ea_{\text{FWO}} = -\frac{R}{1.052} m_{\text{FWO}} \quad (10)$$

$$Ea_{\text{KAS}} = -R.m_{\text{KAS}} \quad (11)$$

$$A_{\text{FWO}} = -R.e^{(b_{\text{FWO}}+5.331)} .g(\alpha) \frac{1}{Ea_{\text{FWO}}} \quad (12)$$

$$A_{\text{KAS}} = \frac{e^{b_{\text{KAS}}} .g(\alpha)}{R} Ea_{\text{KAS}} \quad (13)$$

#### Model-fitting method

Different reaction models used in the solid-state kinetics are listed in Table 1.

All model-fitting methods assume that a particular reaction model represents the conversion dependence of the reaction rate (Vyazovkin et al. 2011). The most commonly used model-fitting methods is Coats-Redfern (CR) approximation, described by Eq. (14) (Ghughe and Mandal 2017; Lv et al. 2018; Pratap et al. 2007). This approximation was applied on the different reactions models listed in Table 1, and the best suited model for fitting was defined as the solid-state reaction mechanism.

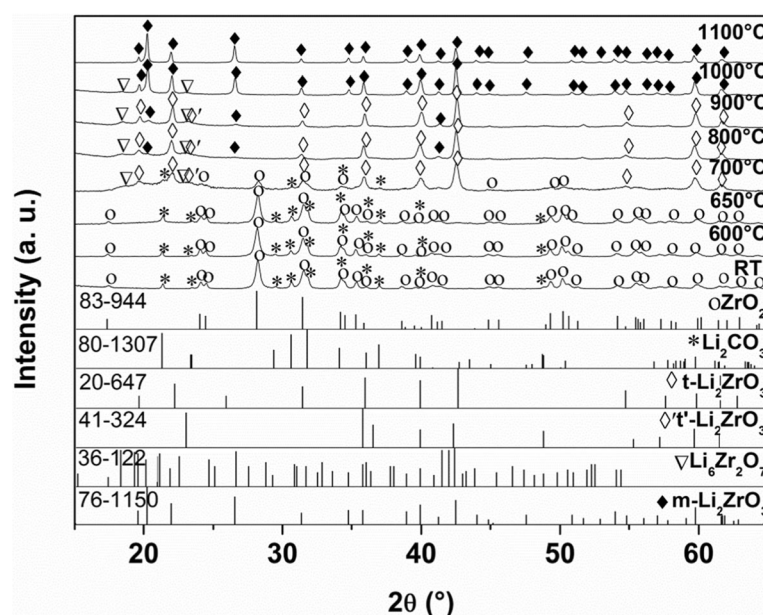
$$\ln \left( \frac{g(\alpha)}{T^2} \right) = \ln \left( \frac{AR}{\beta E_a} \left( 1 - \frac{2R\bar{T}}{E_a} \right) \right) - \frac{E_a}{RT} \quad (14)$$

## Results and discussion

XRD patterns of  $\text{Li}_2\text{CO}_3\text{-ZrO}_2$  mixtures heated at temperatures from 600 °C to 1100 °C are shown in Fig. 1. XRD pattern of the precursor (at room temperature) was included for comparison. As can be seen in Fig. 1, the samples obtained after heat treatment at 600 °C and 650 °C do not exhibit a significant difference when compared with the precursor, suggesting that  $\text{Li}_2\text{CO}_3$  (JCPDS 80-1307) did not react with  $\text{ZrO}_2$  (JCPDS 83-944) at temperatures below 650 °C. When the temperature was increased to 700 °C, tetragonal  $\text{Li}_2\text{ZrO}_3$  (mainly  $t\text{-Li}_2\text{ZrO}_3$  (JCPDS 20-647), along with  $t'\text{-Li}_2\text{ZrO}_3$  traces (JCPDS 41-324)), and hexa-lithium zirconate ( $\text{Li}_6\text{Zr}_2\text{O}_7$ , JCPDS 36-122) were formed, while  $\text{ZrO}_2$  and  $\text{Li}_2\text{CO}_3$  peaks decreased significantly. This implies that a large amount

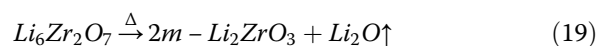
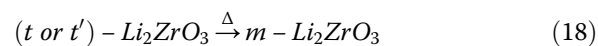
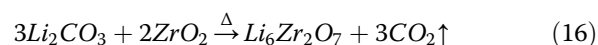
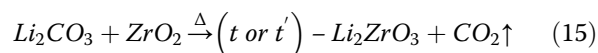
**Table 1** Different reaction models used in the solid-state kinetics (Vyazovkin et al. 2011; Khawam and Flanagan 2006; Milićević et al. 2017; Vyazovkin et al. 2014)

#	Reaction model	f(a)	g(a)
<b>Nucleation models</b>			
1	Power law (P2)	$2a^{1/2}$	$a^{1/2}$
2	Power law (P3)	$3a^{2/3}$	$a^{1/3}$
3	Power law (P4)	$4a^{3/4}$	$a^{1/4}$
4	Avrami-Erofeyev (A2)	$2(1-a)[-ln(1-a)]^{1/2}$	$[-ln(1-a)]^{1/2}$
5	Avrami-Erofeyev (A3)	$3(1-a)[-ln(1-a)]^{2/3}$	$[-ln(1-a)]^{1/3}$
6	Avrami-Erofeyev (A4)	$4(1-a)[-ln(1-a)]^{3/4}$	$[-ln(1-a)]^{1/4}$
7	Modified Prout-Tompkins (B1)	$a(1-a)$	$ln[a/(1-a)]$
<b>Geometrical contraction models</b>			
8	Contracting area (R2)	$2(1-a)^{1/2}$	$1-(1-a)^{1/2}$
9	Contracting volume (R3)	$3(1-a)^{2/3}$	$1-(1-a)^{1/3}$
<b>Diffusion models</b>			
10	One-dimensional diffusion (D1)	$1/(2a)$	$a^2$
11	Two-dimensional diffusion (D2)	$-[1/ln(1-a)]$	$((1-a)ln(1-a))+a$
12	Three-dimensional diffusion (D3)	$[3(1-a)^{2/3}/[2(1-(1-a)^{1/3})]]$	$(1-(1-a)^{1/3})^2$
13	Ginstling-Brounshtein (D4)	$3/[2(1-(1-a)^{-1/3}-1)]$	$1-(2/3)a-(1-a)^{2/3}$
<b>Reaction-order models</b>			
14	Zero-order (F0/R1)	1	a
15	First-order (F1)	(1-a)	-ln(1-a)
16	Second-order (F2)	(1-a) <sup>2</sup>	[1/(1-a)] - 1
17	Third-order (F3)	(1-a) <sup>3</sup>	(1/2)[(1-a) <sup>-2</sup> -1]

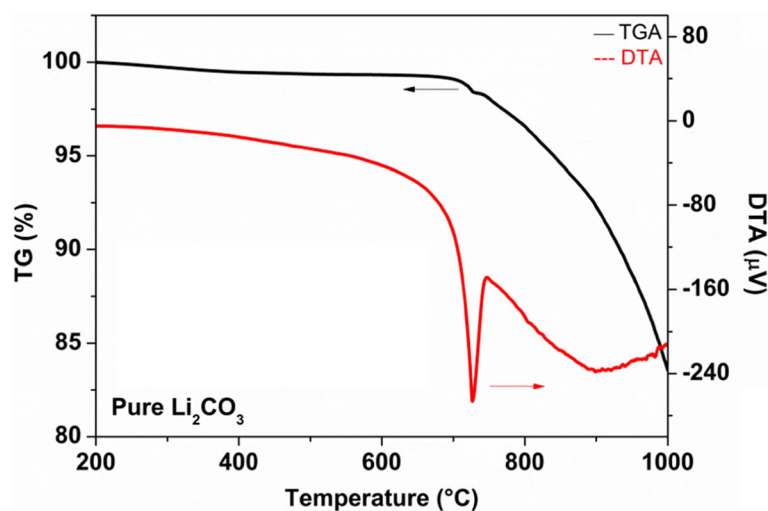
**Fig. 1** XRD patterns of  $\text{Li}_2\text{CO}_3\text{-ZrO}_2$  mixtures at room temperature (RT) and heated at different temperatures

of  $\text{Li}_2\text{CO}_3$  can be consumed by both the direct reaction with  $\text{ZrO}_2$  in order to form Li-Zr-O compounds, and its decomposition. The reaction between  $\text{Li}_2\text{CO}_3$  and  $\text{ZrO}_2$  can result in the formation of tetragonal  $\text{Li}_2\text{ZrO}_3$  (see Eq. (15)) since this symmetry can exist as a metastable polymorph at temperature below 900 °C (Wang et al. 2013). The formation of  $\text{Li}_6\text{Zr}_2\text{O}_7$  can be attributed to small heterogeneities in the sample that result in a local variation of the stoichiometry, favoring the reaction described by Eq. (16) (Pfeiffer and Knowles 2004; Wang et al. 2014). In order to confirm the decomposition of  $\text{Li}_2\text{CO}_3$  in this temperature range, TG-DTA for pure  $\text{Li}_2\text{CO}_3$  was performed (see Fig. 2). According to the results shown in Fig. 2, it was indeed found that  $\text{Li}_2\text{CO}_3$  melts and decomposes at temperatures above 700 °C (see Eq. (17)), in accordance with those results found in literature (Ida and Lin 2003; Mandal 2014; Lu and Wei-Cheng 2000). When the temperature reached 800 °C, a small amount of m- $\text{Li}_2\text{ZrO}_3$  (JCPDS 76-1150) was formed, while  $\text{ZrO}_2$  and  $\text{Li}_2\text{CO}_3$  were not detected. Tetragonal  $\text{Li}_2\text{ZrO}_3$  and  $\text{Li}_6\text{Zr}_2\text{O}_7$  phases remain in the sample. This implies that at this temperature the remaining  $\text{ZrO}_2$  and  $\text{Li}_2\text{CO}_3$  were consumed to form  $\text{Li}_2\text{ZrO}_3$  (tetragonal and monoclinic) and  $\text{Li}_6\text{Zr}_2\text{O}_7$ . At 900 °C, the XRD pattern was not significantly modified, the only difference is a small increase in the amount of m- $\text{Li}_2\text{ZrO}_3$ , which can be attributed to a partial phase transition from tetragonal to monoclinic  $\text{Li}_2\text{ZrO}_3$  (see Eq. (18)). This transition was favored at higher temperatures, being completed at 1000 °C, as shown in Fig. 1, where only the monoclinic polymorph of  $\text{Li}_2\text{ZrO}_3$  is observed. In this XRD pattern, m- $\text{Li}_2\text{ZrO}_3$  became the main crystalline phase, along with  $\text{Li}_6\text{Zr}_2\text{O}_7$  traces. Finally, when the temperature reached 1100 °C, pure m- $\text{Li}_2\text{ZrO}_3$  was obtained,

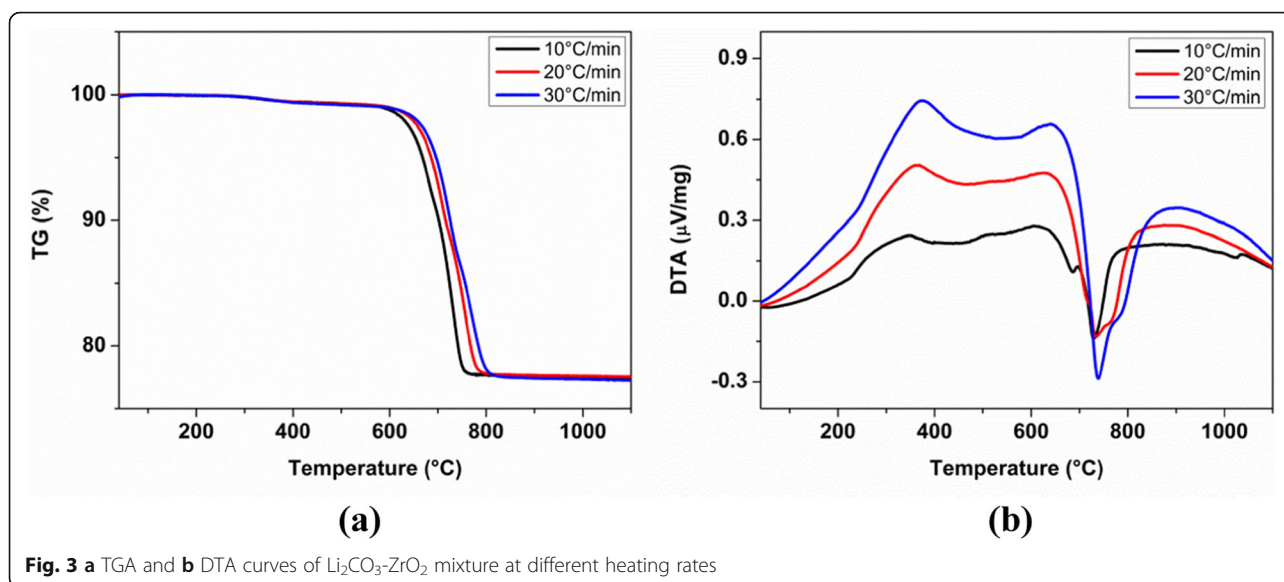
implying the decomposition of  $\text{Li}_6\text{Zr}_2\text{O}_7$  traces according to Eq. (19) (Pfeiffer and Knowles 2004).



TGA and DTA curves of  $\text{Li}_2\text{CO}_3$ - $\text{ZrO}_2$  mixtures at different heating rates (10, 20, and 30 °C/min) are shown in Fig. 3a, b, respectively. Figure 3a shows that in TGA curve obtained at 10 °C/min, the weight loss was greatly affected by increasing temperature approximately between 600 °C and 750 °C. This weight loss can be attributed to  $\text{CO}_2$  losses though both the direct reaction of  $\text{Li}_2\text{CO}_3$  with  $\text{ZrO}_2$  to form Li-Zr-O compounds, and the decomposition of  $\text{Li}_2\text{CO}_3$ , as explained above (see Eq. 15–17). The overall weight loss was about 23%, which is consistent with the values found in the literature for this type of reaction (Pfeiffer and Knowles 2004; Woo et al. 2006). When the heating rate was increased, the trend of the TGA curves was similar, but with a slight shift towards higher temperatures, as can be observed in Fig. 3a. This can be associated with heat transfer limitations during the analysis, since, even if a slow heating rate is favorable to approach thermal equilibrium due to a larger instantaneous thermal energy is provided to the sample, a fast heating rate can generate a thermal lag between the heating source and the sample, therefore, the



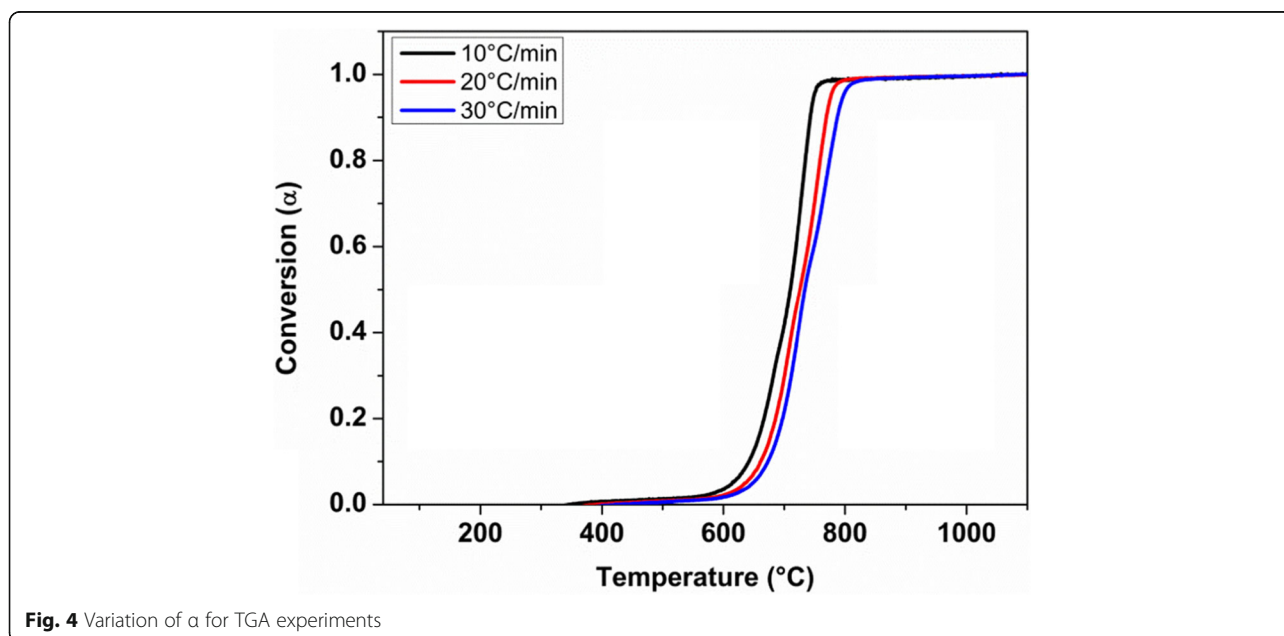
**Fig. 2** TG-DTA curves of pure  $\text{Li}_2\text{CO}_3$  at 10 °C/min



temperature gradient across the sample is more pronounced (Leng 2013; Kongkaew et al. 2015). That is why slightly higher temperatures were required to complete the reactions of decomposition of  $\text{Li}_2\text{CO}_3$  and formation of Li-Zr-O compounds at faster heating rates. On the other hand, Fig. 3b shows that the DTA curve obtained at 10 °C/min presents a dual endothermic effect between 650 °C and 800 °C, which can be attributed to reactive  $\text{Li}_2\text{CO}_3$  reacting with  $\text{ZrO}_2$ , and the melting and decomposition of  $\text{Li}_2\text{CO}_3$ , in accordance with the XRD and TG-DTA results shown above. When the heating rate was increased, this region became broader. This can be due to that when the thermal equilibrium was reached

at slow heating rate, the sample stayed long time at this temperature, favoring the reactions in all of the material and the formation of endothermic peaks in the DTA, while at faster heating rates a temperature gradient was generated; therefore, this region was extended to higher temperatures until the reactions were completed.

Figure 4 shows the variation of  $\alpha$  as a function of temperature at different heating rates for TGA experiments. As can be seen, the trend of the variation of  $\alpha$  as a function of temperature was similar for the different heating rates. In general, it can be observed that  $\alpha$  increased significantly at temperatures approximately between 600 °C and 750–800 °C, implying the formation of



Li-Zr-O compounds. The slightly shift to the right in the curves obtained at higher heating rates is associated to that higher temperatures were required to complete the reactions, as explained for TG-DTA curves in Fig. 2. Then, the conversion degree continued to increase slowly with increasing temperature till the end of the reaction at about 1100 °C.

In order to determine the kinetic parameters through the isoconversional methods, the results obtained from Fig. 4 were used. The kinetic data of the reaction for the formation of m-Li<sub>2</sub>ZrO<sub>3</sub> were calculated by FWO and KAS methods from "ln β versus (1/T)", and "ln( $\frac{\beta}{T^2}$ ) versus (1/T)" plots, which are shown in Figs. 5 and 6, respectively. In each case, the slopes and intercepts of fitted lines were used to calculate the apparent activation energy and pre-exponential factor, respectively, for a given value of α.

Figure 7 shows the activation energy (E<sub>a</sub>) as a function of α. As it can be noted, the values of activation energy estimated by FWO method are similar with those obtained by KAS method, demonstrating a good agreement in the calculation of the kinetic data. According to these results, the overall reaction process can be divided into two stages, where the activation energy increased initially (0 < α ≤ 0.5), and then decreased gradually (0.5 < α < 1). The values of the average activation energy were 293.25 kJ/mol (FWO) and 292.42 kJ/mol (KAS) for the first stage; and 256.21 kJ/mol (FWO) and 252.58 kJ/mol (KAS) for the second stage. The first stage can be due to that Li<sub>2</sub>CO<sub>3</sub> reacted with ZrO<sub>2</sub> to form tetragonal Li<sub>2</sub>ZrO<sub>3</sub> and Li<sub>6</sub>Zr<sub>2</sub>O<sub>7</sub> on the surface of ZrO<sub>2</sub> particles.

With increasing temperature reaction, Li<sup>+</sup> diffused through the shell to the core of ZrO<sub>2</sub> to thicken the product layer; therefore, the activation energy was increased. The final stage can be associated with the formation of m-Li<sub>2</sub>ZrO<sub>3</sub> by transformation of tetragonal Li<sub>2</sub>ZrO<sub>3</sub>, and decomposition of Li<sub>6</sub>Zr<sub>2</sub>O<sub>7</sub> at higher temperatures, which result in a decrease in the activation energy. Thus, the average activation energy of the overall reaction process estimated by FWO and KAS methods were 274.73 kJ/mol and 272.50 kJ/mol, respectively. In the case of the pre-exponential factor, the average values estimated by FWO and KAS methods were 2.63 × 10<sup>20</sup>/min and 3.16 × 10<sup>14</sup>/min, respectively, indicating a highly reactive system (A ≥ 10<sup>10</sup>/min) (Dhyani et al. 2017).

In order to determine the most probable reaction model, the Coats-Redfern (CR) approximation described by Eq. (14) was used. For this purpose, this approximation was applied on the different reactions models listed in Table 1 using the TGA data shown in Fig. 2a. The CR data (ln(g<sub>(α)</sub>/T<sup>2</sup>) versus 1/T) for the reaction models of the solid-state reaction heated at different heating rates was fitted, and the values of the obtained R<sup>2</sup> are presented in Table 2.

A practical way to determine the best suitable solid-state reaction model was to look the model corresponding to maximum R<sup>2</sup> (Ghughe and Mandal 2017; Khawam and Flanagan 2005), according to the results obtained in Table 2. By applying this criterion for the analyzed data several equivalent models based on goodness of fit can be chosen; however, the three-dimensional diffusion model (D3, see Fig. 8) is found to more suitable for the

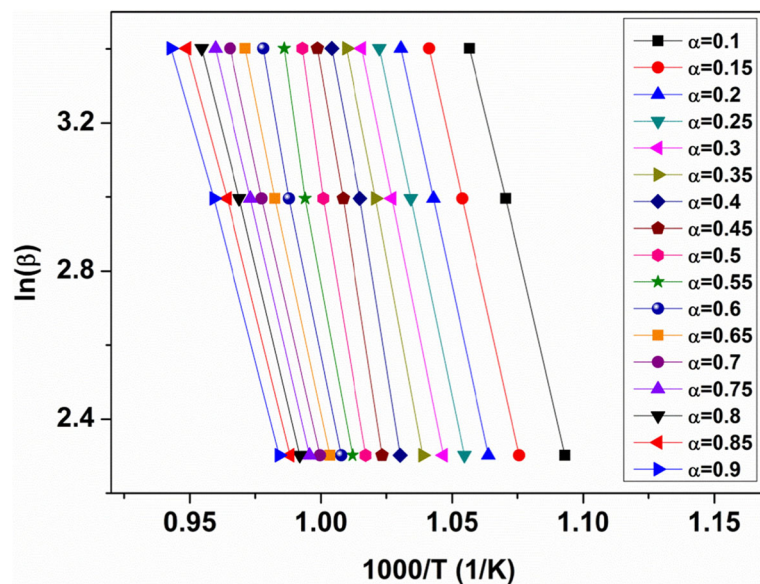
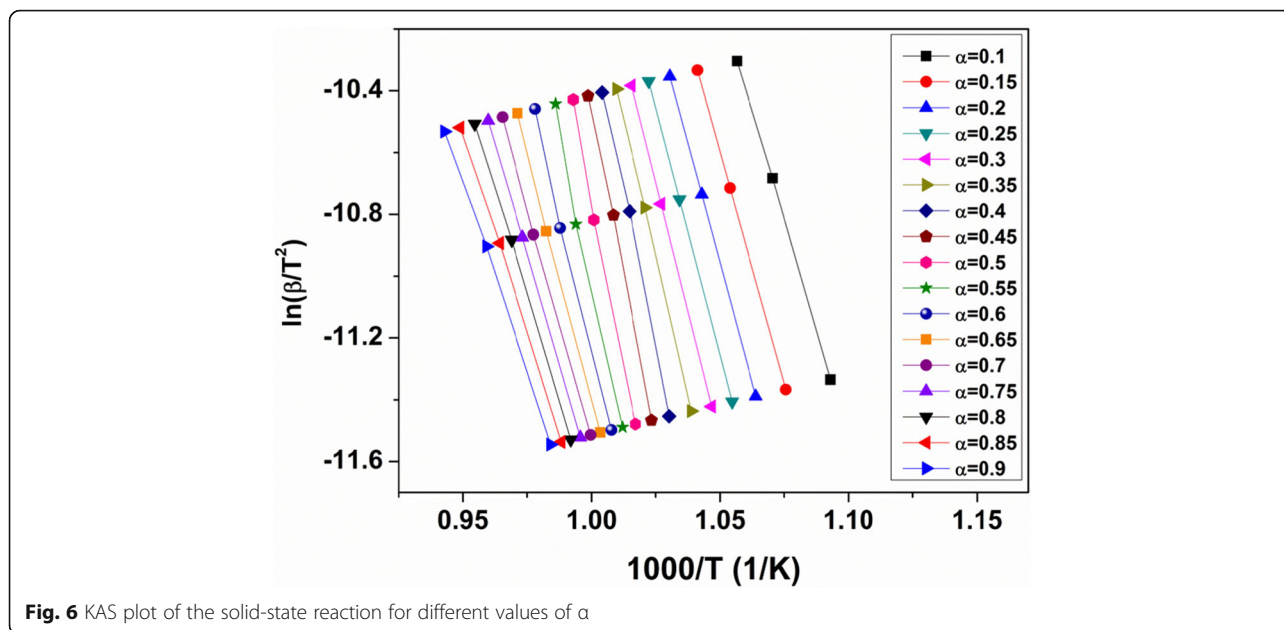


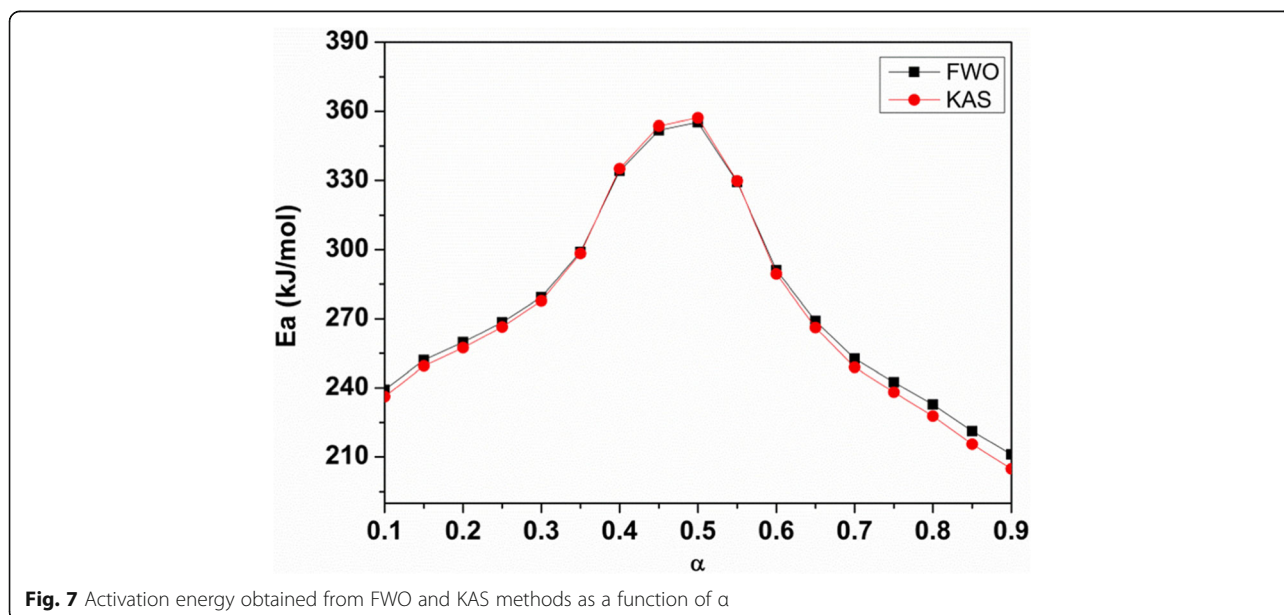
Fig. 5 FWO plot of the solid-state reaction for different values of α



description of the solid-state reaction not only because  $R^2$  was a maximum for this model at each heating rate, but also because  $E_a$  for D3 obtained by CR method is consistent with the range of values obtained by FWO and KAS methods and near to their average values (~ 273 kJ/mol), considering that the reaction model can be determined from  $E_a$  for a single  $\alpha = \alpha(T)$  curve that equals  $E_a$  obtained by means of isoconversional methods (Khawam and Flanagan 2005; Pratap et al. 2007). This suggests that the reaction of  $\text{Li}_2\text{CO}_3$  with  $\text{ZrO}_2$  is governed by a diffusion-controlled mechanism, implying that the rate of formation of  $m\text{-Li}_2\text{ZrO}_3$  decreases

proportionally with the thickness of its barrier layer (Khawam and Flanagan 2006).

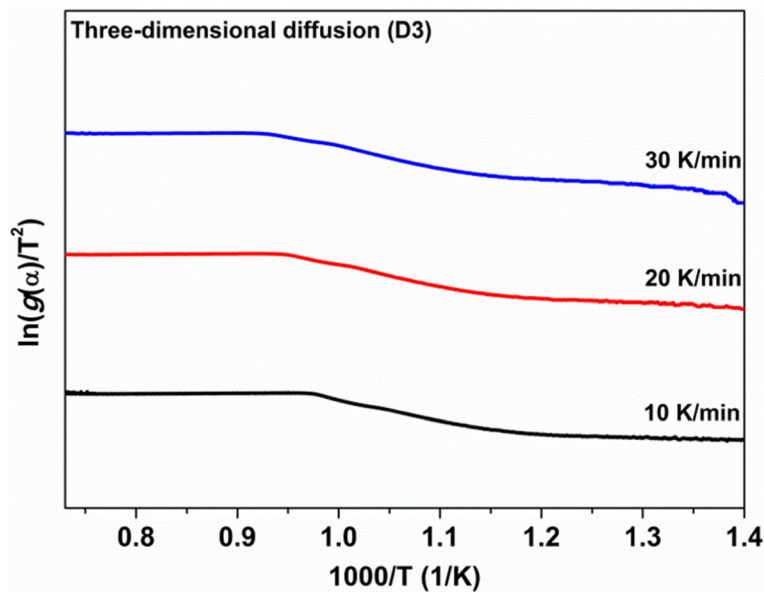
The average particle size of the samples prepared at different temperatures was examined by DLS (see Fig. 9). As shown in Fig. 9, the average particle size of the sample obtained at 600 °C was 325 nm which, according to Fig. 1, is composed by  $\text{Li}_2\text{CO}_3$  and  $\text{ZrO}_2$  particles. When the temperature was increased to 700 °C, the average particle size increased slightly, probably due to the partial reaction of reactive  $\text{Li}_2\text{CO}_3$  with  $\text{ZrO}_2$  (see Fig. 1), resulting in partial nucleation of lithium-containing zirconates ( $\text{Li}_x\text{Zr}_y\text{O}_z$ ) on the surface of  $\text{ZrO}_2$  particles. When the temperature

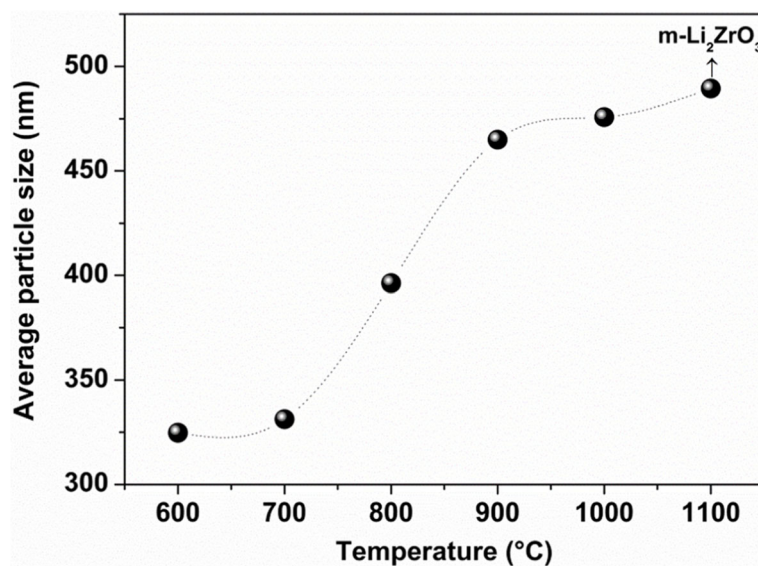




**Table 2** Solid-state curve fitting parameter ( $R^2$ ) by CR method for TGA experiments at different heating rates

#	Reaction model	$R^2$		
		10 °C/min	20 °C/min	30 °C/min
<b>Nucleation models</b>				
1	Power law (P2)	0.75187	0.795460	0.79543
2	Power law (P3)	0.52183	0.64315	0.65993
3	Power law (P4)	0.13	0.3616	0.41986
4	Avrami-Erofeyev (A2)	0.85286	0.88944	0.91076
5	Avrami-Erofeyev (A3)	0.77171	0.83513	0.86886
6	Avrami-Erofeyev (A4)	0.61573	0.73777	0.79591
7	Modified Prout-Tompkins (B1)	0.22116	0.2703	0.42012
<b>Geometrical contraction models</b>				
8	Contracting area (R2)	0.87958	0.89781	0.89985
9	Contracting volume (R3)	0.88562	0.90587	0.91142
<b>Diffusion models</b>				
10	One-dimensional diffusion (D1)	0.89002	0.8995	0.89459
11	Two-dimensional diffusion (D2)	0.89712	0.90829	0.90618
12	Three-dimensional diffusion (D3)	<b>0.90603</b>	<b>0.92164</b>	<b>0.93858</b>
13	Ginstling-Brounshtein (D4)	0.90018	0.91292	0.91269
<b>Reaction-order models</b>				
14	Zero-order (F0/R1)	0.85917	0.87468	0.87021
15	First-order (F1)	0.89800	0.92163	0.9363
16	Second-order (F2)	0.8773	0.91932	0.93746
17	Third-order (F3)	0.75608	0.86045	0.89113

**Fig. 8** CR plot for the three-dimensional diffusion (D3) reaction model of the solid-state reaction heated at different heating rates

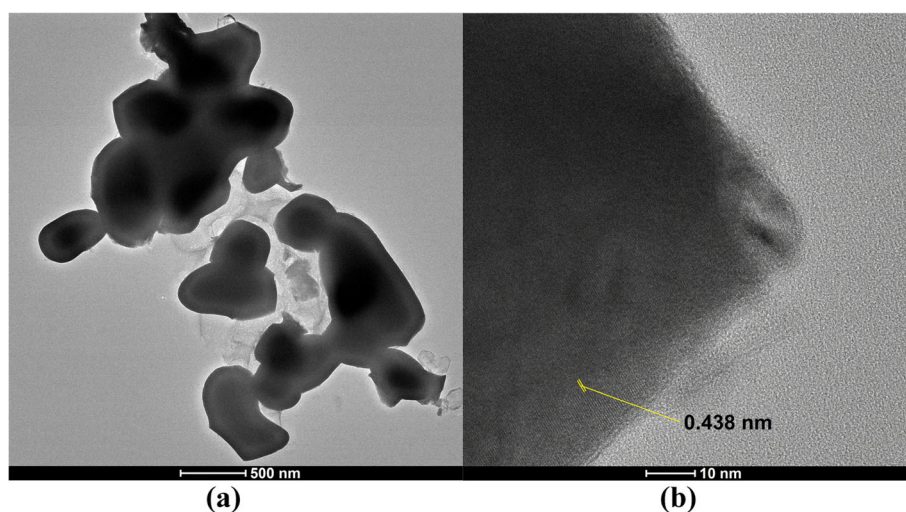


**Fig. 9** Average particle size of samples prepared at different temperatures

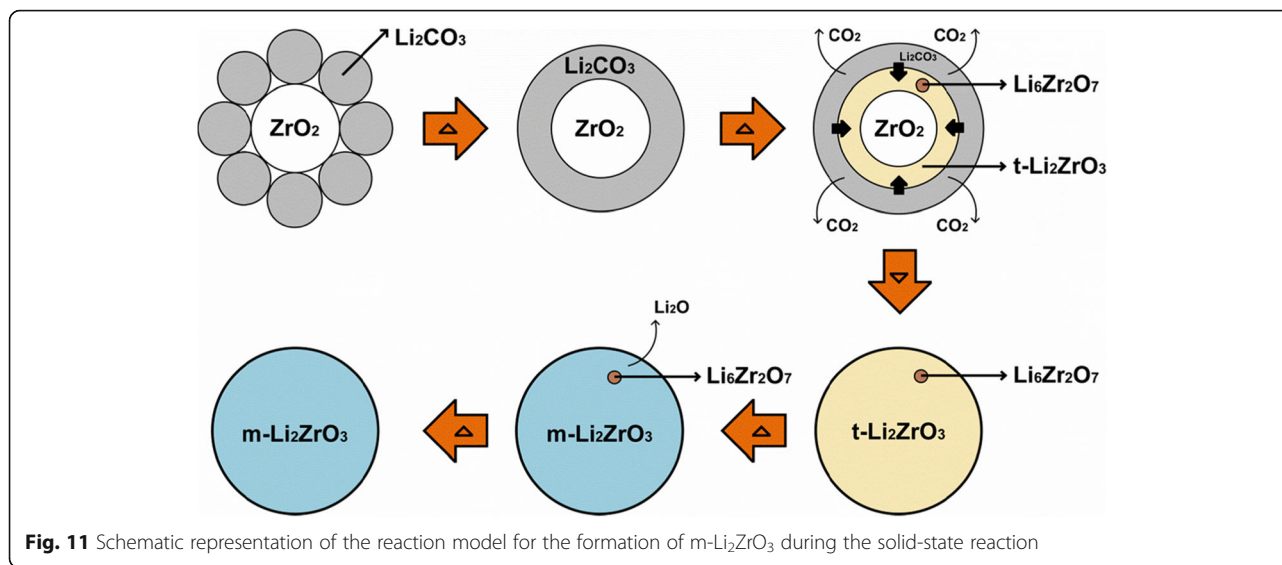
was increased to 800 °C, the average particle size increased to 396 nm, suggesting both the nucleation and growth of  $\text{Li}_x\text{Zr}_y\text{O}_z$  particles, because the reaction between the starting materials had been completed at this temperature (see Fig. 1). Further temperature increases resulted in increases in the average particle size due both to growth of  $\text{Li}_x\text{Zr}_y\text{O}_z$  particles and formation of agglomerates, because of high temperatures. Thus, the average particle size of the sample obtained at 1100 °C was 490 nm, which corresponds to pure  $m\text{-Li}_2\text{ZrO}_3$ , according to XRD results.

Particle morphology of pure  $m\text{-Li}_2\text{ZrO}_3$  was also confirmed by TEM and HRTEM analysis. As shown in Fig. 10a, TEM image reveals that  $m\text{-Li}_2\text{ZrO}_3$  is composed

of semispherical particles showing sizes of around 500 nm. It is also possible to observe the formation of agglomerates, because of high temperature. These results are in accordance with the DLS results described above. Figure 10b shows the crystallographic structure of the as-synthesized  $m\text{-Li}_2\text{ZrO}_3$  at an atomic scale, with an interlayer spacing of 0.438 nm. This result is matched with the interplanar distance of (110) plane for the standard  $m\text{-Li}_2\text{ZrO}_3$  (JCPDS 76-1150). When compared with other reports on the solid-state reaction (Sherstobitova et al. 2016; Pfeiffer and Knowles 2004; Yin et al. 2009; Hernández-Pérez et al. 2018), the present work succeeded in reducing from micron to submicron scale the average particle size of pure



**Fig. 10** a TEM and b HRTEM images of pure  $m\text{-Li}_2\text{ZrO}_3$  powders prepared by solid-state reaction



**Fig. 11** Schematic representation of the reaction model for the formation of  $m\text{-Li}_2\text{ZrO}_3$  during the solid-state reaction

$m\text{-Li}_2\text{ZrO}_3$ . This can be attributed to the very short reaction time of less than a minute used at high temperature.

Based on the results obtained in this work, along with the three-dimensional diffusion-controlled mechanism, a microscopic reaction model of the formation of  $m\text{-Li}_2\text{ZrO}_3$  is proposed. During the heating process,  $\text{Li}_2\text{CO}_3$  melts and encloses the  $\text{ZrO}_2$  particles. Thus, the melted  $\text{Li}_2\text{CO}_3$  reacts with  $\text{ZrO}_2$  to form a shell of tetragonal  $\text{Li}_2\text{ZrO}_3$  and  $\text{Li}_6\text{Zr}_2\text{O}_7$  on the surface, accompanied by release of  $\text{CO}_2$ , which diffuses out through the melted  $\text{Li}_2\text{CO}_3$ . This process continues with the decomposition of the melted  $\text{Li}_2\text{CO}_3$  and  $\text{Li}^+$  diffusion through the shell to the core of  $\text{ZrO}_2$  to thicken the product layer, in order to complete the formation of lithium-containing zirconates. This confirms that  $\text{CO}_2$  desorption plays an important role in this type of reaction [4]. With increasing reaction temperature, the phase transition of tetragonal to monoclinic  $\text{Li}_2\text{ZrO}_3$ , and the decomposition of  $\text{Li}_6\text{Zr}_2\text{O}_7$  to release  $\text{Li}_2\text{O}$  are favored, resulting in the formation of pure  $m\text{-Li}_2\text{ZrO}_3$  in the sample. A schematic representation of the proposed microscopic reaction model is shown in Fig. 11.

## Conclusions

Non-isothermal reaction mechanism and kinetic parameters have been determined for the first time for the synthesis of monoclinic lithium zirconate ( $m\text{-Li}_2\text{ZrO}_3$ ) via solid-state reaction of  $\text{Li}_2\text{CO}_3$  with  $\text{ZrO}_2$ . Kinetic analysis was investigated by processing of TG-DTA, along with XRD, DLS, and HRTEM. Pure  $m\text{-Li}_2\text{ZrO}_3$  powders of about 490 nm and semispherical morphology were obtained at 1100 °C. This method succeeded in reducing from micron to submicron scale the average particle size of pure  $m\text{-Li}_2\text{ZrO}_3$  synthesized by using conventional solid-state reaction, because of the very short reaction

time of less than a minute used at high temperature. Kinetics parameters were calculated and compared through two different isoconversional methods: FWO and KAS. The average value of activation energy obtained from the FWO method (274.73 kJ/mol) was very near to those obtained from KAS (272.50 kJ/mol), which demonstrates a good agreement in the calculation of the kinetic parameters. On the other hand, the reaction mechanism was determined by model-fitting method using CR approximation. It was found that the reaction between  $\text{Li}_2\text{CO}_3$  and  $\text{ZrO}_2$  follows the diffusion mechanism, being the three-dimensional diffusion-controlled reaction the best fitted model for the formation of  $m\text{-Li}_2\text{ZrO}_3$ . This analysis is very important in order to optimize the solid-state process for large-scale production, and advanced applications of  $m\text{-Li}_2\text{ZrO}_3$ .

## Abbreviations

A: Pre-exponential factor; CR: Coats-Redfern approximation; DLS: Dynamic light scattering; Ea: Activation energy; FWO: Flynn-Wall-Ozawa method; HRTEM: High-resolution transmission electron microscopy; KAS: Kissinger-Akahira-Sunose method;  $m\text{-Li}_2\text{ZrO}_3$ : Monoclinic lithium zirconate; TG-DTA: Thermogravimetric and differential-thermal analysis; XRD: X-ray diffraction

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## Authors' contributions

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## Availability of data and materials

All raw data used in this manuscript are available and could be supplied upon request.

## Declarations

### Competing interests

The authors declare that they have no competing interests.

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