Degradation and mineralization of erythromycin by heterogeneous photocatalysis using SnO 2-doped TiO<sub>2</sub> structured catalysts: activity and stability

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Journal



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17	
18	ABSTRACT
19	Heterogeneous photocatalysis was used for the degradation and mineralization of erythromycin
20	(ERY), with a consequent production of carboxylic acids. For that, a series of $TiO_2$ and $Ti_{1-x}Sn_xO_2$
21	structured catalysts, namely M1 to M5, was prepared using the washcoating method, with the
22	catalytic coatings being deposited onto stainless steel meshes. Besides, the catalytic activity of the
23	prepared systems was compared to that of the commercial mesh (CM). The results showed that the
24	prepared TiO <sub>2</sub> structured catalyst (M1) presented better ERY oxidation than the CM one, what was
25	associated to the higher catalyst load and to the anatase/rutile ratio. Considering the Sn-doped

structured catalysts, for M2, M4 and M5 catalysts, lower ERY mineralization and high formation of

carboxylic acids were found, when compared to the M3 catalyst. The improved M3 activity was 27 attributed to the formation of a staggered gap (type II heterojunction), providing better charge 28 separation. In this situation, a high generation of hydroxyl radicals is obtained, resulting on a higher 29 ERY mineralization. By the obtained results it is possible to determine that the addition order and 30 31 the type of Sn compound added in the washcoating process, affects the catalytic activity due to the formation of a solid solution and to the type of produced heterostructures. The M3 catalyst also 32 showed high stability in long-term tests up to 44 h of reaction. The results provide insights into the 33 development of an inexpensive structured catalyst production method and its influence in the 34 stability of the photocatalyst, as well as in its applicability on water/wastewater treatment. 35

36

37 KEYWORDS: Ti<sub>1-x</sub>Sn<sub>x</sub>O<sub>2</sub>; Washcoating; Photocatalysis; Erythromycin; Short carboxylic acids.
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#### 40 1 INTRODUCTION

41 Contaminants of emerging concern (CEC), whose effects on the ecosystem and on human 42 health are unknown or not well understood, have been found in different environments because they are not removed by conventional techniques (Barrios-Estrada et al., 2018; Gogoi et al., 2018; 43 Rodriguez-Narvaez et al., 2017). One example of the CEC is erythromycin (ERY), which is used by 44 people who are allergic to penicillin and it can remain in nature for up to one year, maintaining its 45 antibiotic activity (Patel et al., 2019). After its administration, the degradation within the human 46 body occurs via the biliary and renal tract, the first being the major route of excretion. However, 47 more than 60 % of ERY, as well as other macrolides, is excreted unchanged (Babić et al., 2017). 48

The United States Environmental Protection Agency in 2009 included ERY on its Contaminant Candidate List 3 (CCL 3), while the European Union through its Decision 2015/495/EU, included ERY as a high-risk priority substance (European Comission, 2017). According to Li et al. (2014), in a ranking developed in China, ERY was identified as a

pharmaceutical with a high priority for environmental control due to its recurrent detection in 53 effluents 54 sewage in water supplies or (Lin and Tsai, 2009). ERY was detected in water sources (Westerhoff et al., 2005), affluents of 55 wastewater treatment plants (WWTP) (Hapeshi et al., 2015), effluents of WWTP 56 57 (Rühmland et al., 2015); natural waters (Pico et al., 2019) and underground waters (Lin et al., 2015). Like other CEC, ERY is not well removed by conventional treatment processes; therefore, it 58 must be removed through more complex technologies like advanced oxidative processes (AOP) 59 (Stackelberg et al, 2007; Yang et al., 2017). Heterogeneous photocatalysis (HP) was developed with 60 this objective. The degradation by HP occurs due to the formation of species with high oxidation 61 potential (H0<sup>•</sup>,  $0_2^{-\bullet}$ ) that perform the oxidation to simpler compounds, leading to mineralization 62 (Andreozzi et al., 1999; Kanakaraju et al., 2018). 63

During the HP process, the irradiation of the catalyst surface leads to the adsorption of energy, transferring one electron  $(e_{vb}^-)$  of the valence band (VB) to the conduction band (CB)  $(e_{cb}^-)$ , generating a hole  $(h_{vb}^+)$  in the VB (Eq. (1)) (Vignesh et al., 2014; Voigt and Jaeger , 2017).

$$\operatorname{TiO}_{2} \xrightarrow{h\nu} \operatorname{TiO}_{2} \left( h_{vb}^{+} + e_{cb}^{-} \right)$$
(1)

After the formation of the pair  $e_{cb}^{-}/h_{vb}^{+}$ , two processes may occur: (i) an internal recombination, releasing thermal energy and/or luminance, bringing the catalyst back to its original condition; (ii) with the system excited, reactions 2 to 5 will occur in CB (Vignesh et al., 2014; Voigt and Jaeger , 2017), generating species with high oxidation potential.

$$\mathbf{e}_{cb}^{-} + \mathbf{0}_2 \rightarrow \mathbf{0}_2^{-\bullet} \tag{2}$$

$$O_2^{-\bullet} + H^+ \rightarrow HO_2^{\bullet} \tag{3}$$

$$\mathrm{HO}_{2}^{\bullet} + \mathrm{HO}_{2}^{\bullet} \to \mathrm{H}_{2}\mathrm{O}_{2} + \mathrm{O}_{2} \tag{4}$$

$$\bar{e_{cb}} + H_2 O_2 \rightarrow OH^- + HO^{\bullet}$$
(5)

Besides, in the VB direct oxidation can occur by transferring  $e^-$  from the molecules that are adsorbed on the catalyst surface to the  $h_{vb}^+$ . Due to the low concentrations of organic matter in solution, the main oxidation reactions that occur on the catalyst surface are from adsorbed water or

hydroxide anion molecules (Eq. 6 and 7). Nevertheless, the oxidation reaction of organic matter (M<sub>ads</sub>), also occurs on the catalyst surface (Eq. 8), providing another route for HO<sup>•</sup> generation

(Vignesh et al., 2014; Voigt and Jaeger, 2017). 76

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$$h_{vb}^{+} + H_2 O_{ads} \to HO_{ads}^{\bullet} + H^+$$
(6)

$$h_{vb}^{+} + OH_{ads}^{-} \to HO_{ads}^{\bullet}$$
(7)

$$h_{vb}^{+} + M_{ads} \rightarrow HO_{ads}^{\bullet} + M_{ads}^{\bullet}$$
(8)

TiO<sub>2</sub> Degussa P 25 is a semiconductor widely used in HP processes because of its high 77 stability, non-toxicity and high photocatalytic efficiency compared to other semiconductors 78 (Babić et al., 2017), due to its composition of 80 % anatase and 20 % rutile (Rui et al., 2014). 79 However, TiO<sub>2</sub> presents a high  $e_{cb}^{-}/h_{vb}^{+}$  recombination rate, decreasing the oxidation efficiency and 80 causing energy loss (Pesci et al., 2013; Shen et al., 2018). 81

Several materials are used as TiO<sub>2</sub> dopants aiming for the reduction of the bandgap and the 82 increase of the lifetime of the charges, leading to higher oxidation efficiencies. However, 83 conventional dopants such as ruthenium (Ru), tungsten (W), niobium (Nb) and cerium (Ce) are 84 classified as critical materials by the European Union (Choi et al., 1994; European Comission, 85 2017; Solís-Casados et al., 2017; Zhou et al., 2016). 86

Therefore, it is interesting to develop materials with dopants that are not considered critical 87 elements (European Comission, 2017). Tin (Sn) can be used for doping TiO<sub>2</sub> to decrease the 88 recombination of the  $e_{cb}^{-}/h_{vb}^{+}$  pair, allowing the degradation of complex contaminants 89 (Kusior et al., 2019; Pesci et al., 2013). Doping occurs by replacing a Ti atom with a Sn atom or by 90 inserting a Sn atom into an empty interstitial space in the TiO<sub>2</sub> unit cell. Both processes are favored 91 due to the similarity of the atomic radius sizes, electronic valence (+4) and crystalline structures, 92 93 allowing the formation of a  $Ti_{1-x}Sn_xO_2$  solid solution (Kusior et al., 2019) with the generation of a type II heterojunction, where an effective charge separation on the VB and CB can be generated 94 (Del Angel et al., 2018; Kusior et al., 2019). 95

Different studies performed the doping of SnO<sub>2</sub> in the TiO<sub>2</sub> unit cell using different coating preparation methodologies (hydrothermal, microwave-assisted and sol gel synthesis) and AOP 97 processes (heterogeneous photocatalysis and photoelectrochemical) in the degradation of different 98 CEC (methylene blue, diclofenac, methyl orange, zopiclone and acid orange 7). These studies 99 100 showed that there is an effective increase in the photocatalytic activity of TiO<sub>2</sub> when doped with SnO<sub>2</sub> 101

(Kusior et al., 2019, Mugunthan et al., 2019; Sangchay, 2016; Vinodgopal and Kamat 1995; 102 103 Yu et al., 2013).

However, Sn-doped TiO<sub>2</sub> structured catalysts prepared by washcoating of stainless steel 104 meshes, and their subsequent use in the mineralization and degradation of ERY through HP, have 105 106 not been reported in the literature to our knowledge. Therefore, this work presents different procedures of doping TiO<sub>2</sub> with SnO<sub>2</sub> through the washcoating method applied to AISI 304 meshes, 107 which ended up not only in different Sn/Ti distributions on the photocatalytic coating but also in 108 different Ti-Sn interactions. The main goal is focused in the evaluation of the photocatalytic activity 109 of these structured catalysts in the degradation of ERY with UV-A radiation. The quality and 110 111 efficiency of the coatings were assessed through long-term tests and by the analysis of the formation of carboxylic acids. Furthermore, a reaction mechanism was proposed. 112

113

#### **EXPERIMENTAL** 114 2

#### Materials, synthesis and characterization 2.1 115

A series of titanium and titanium/tin oxides structured catalysts with a PVA/TiO<sub>2</sub> mass ratio 116 of 0.37 were synthesized through the washcoating method applied to structured substrates (AISI 117 304 meshes) (Trindade et al. 2018). All solvents and reagents used were of analytical grade. 118 AEROXIDE<sup>®</sup> TiO<sub>2</sub> P 25 (Evonik), ZrO<sub>2</sub> (Zr10/15) and SnO<sub>2</sub> (SN15) from Nyacol<sup>®</sup>, tin (II) oxalate 119 and polyvinyl alcohol from Sigma-Aldrich were used to prepare catalysts by the washcoating 120 method. AISI 304 stainless steel meshes (opening 0.546 mm and 0.30 mm wire diameter) were used 121

as substrates for the catalyst coatings. In addition, a commercial mesh photocatalyst designated as CM with a  $Ti_{0.7}Ru_{0.3}O_2$ -Ti composition (with a geometrical surface area of 475.2 cm<sup>2</sup>) was used as a comparison to the prepared photocatalysts.

The substrates were cut into a rectangular shape with 6 cm in width  $\times$  16 cm in length with a geometrical surface area of 212.89 cm<sup>2</sup>. Due to the setup that was adopted for the photocatalytic tests, the substrates were shaped into a hemi cylindrical form with  $\emptyset = 10$  cm. The AISI 304 mesh pieces (structured substrates) were cleaned and pretreated through a calcination to generate an oxidic layer which allows the posterior coatings anchoring, according to Bortolozzi et al. (2010).

130 Subsequently, the washcoating method was used to immobilize the photocatalytic coatings onto the metallic mesh pieces, following four basic steps described elsewhere (Trindade et al., 131 2018): (i) dip, (ii) blowing, (iii) drying and (iv) calcination. The basic washcoating suspension 132 composition was: 121.2 g H<sub>2</sub>O, 3.6 g PVA, 40.8 g ZrO<sub>2</sub> and 9.6 g TiO<sub>2</sub>. Five different structured 133 catalysts were obtained: M1, M2, M3, M4 and M5. M1 was prepared with the basic suspension 134 composition (free of Sn). For the other structured catalysts, the preparation consisted in the 135 incorporation of Sn to the catalytic coating via different methods and Sn sources: 1) M2: after 136 obtaining the TiO<sub>2</sub> coating (M1), Sn was impregnated on M1 via its immersion in an aqueous 137 solution of Sn oxalate (0.5 g  $L^{-1}$ ); 2) M3: Sn oxalate was added to the basic washcoating suspension 138 along with the others components; 3) M4: powder microparticles of SnO<sub>2</sub> were incorporated to the 139 basic washcoating suspension; 4) M5: the same methodology as M3 and M4 was applied, but using 140 a suspension of SnO<sub>2</sub> nanoparticles (Nyacol SN15). A detailed experimental procedure is shown in 141 the supplementary material (Fig. S1). 142

Surface images were obtained after each calcination step for all structured catalysts during the coating process, as previously described and shown in Fig. S1. Optical microscopy was performed with a Leica S8 APO microscope equipped with a Leica LC3 digital camera and LAS EZ software. The surface images were analyzed to determine the quality of the coatings and taken into account to define the number of immersions and calcination cycles for each catalyst.

The surface features of the prepared systems were characterized by scanning electron microscopy (SEM) equipped with an energy dispersive X-ray (EDS) detector (Phenom ProX Desktop SEM equipment, ThermoFisher). The elemental mappings were performed on a Phenom ProX Desktop SEM software and operating at 15 kV. Several sectors were analyzed, and all the components were taken into account to estimate the Sn/Ti ratios and to obtain a better picture of the elements distribution.

154 The crystalline phases were identified using X-ray diffraction (XRD), the equipment being a 155 Shimadzu XD-D1 with Cu K $\alpha$  radiation. Every XRD experiment was ran at a scan rate of 2° min<sup>-1</sup>, 156 from 2 $\theta$  = 20° to 80°.

157 X-ray Photoelectron Spectroscopy (XPS) was used to analyze the surface Sn species. A 158 SPECS spectrometer equipment with a hemispherical PHOIBOS 150 analyzer operated in the FAT 159 mode (30 eV, 200W, Mg K $\alpha$  X-ray source power) was used. The samples were evacuated in 160 vacuum at 10<sup>-3</sup> mbar at 200 °C for 10 min. Then, they were evacuated for 120 min in ultra-high 161 vacuum. The peak fitting was performed with the CASAXPS software using C 1s at 284.6 eV as 162 reference.

163

#### 164 2.2 Photocatalytic evaluation

The performance of the structured catalysts was evaluated in the heterogeneous 165 photocatalysis (HP) for the oxidation of ERY. The ERY solution had a concentration of 50 mg  $L^{-1}$ 166 and was prepared by dissolving ERY estolate in deionized water. The tests were carried out adding 167 1 L of ERY solution - pH 5.4 - in the non-irradiated reservoir that fed the 0.3 L home-made photo-168 reactor with a flowrate of 1.2 L min<sup>-1</sup> (Fig. 1). A 9 W UV-A lamp (Dulux S BL UVA 9 W/78) was 169 placed in the center of the reactor, which was surrounded by two structured catalysts in a concentric 170 171 arrangement. The distances from the lamp to the catalyst as well as from the catalysts to the reactor walls were set at 2 cm. 172

To get better insights about the ERY removal mechanism, adsorption (ADS) and direct photolysis (DP) tests were also conducted. For ADS tests the UV-A lamp was turned off, while the structured catalysts were removed for the DP assays. In all cases (HP, ADS and DP), duplicate 240minute tests were performed and, if necessary, additional tests were carried out.

The stability of the structured catalyst that presented the best results in ERY mineralization was also evaluated. For that, the structured catalyst was subjected to HP experiments fourteen times in the same conditions and reactor, only replacing the ERY solution after each test. After the 14 experiments, the structured catalyst was evaluated to determine the catalyst stability.

181

#### Figure 1.

182

## 183 2.3 Analytical

Tests of 240 minutes were performed, and aliquots were collected at 0, 5, 15, 30, 60, 120, 180 and 240 minutes for measurements of pH, total organic carbon (TOC) and high-performance liquid chromatography (HPLC) analysis at room temperature. pH measurements were performed with a digital instrument (KASVI K39-0014PA) calibrated with standards of 4, 7 and 10. TOC analysis was made on a TOC-L CPH Shimadzu apparatus with the Non-Purgeable Organic Carbon (NPOC) method, according to the instructions of the TOC Shimadzu manual.

The ERY decay and the generation of carboxylic acids were detected in a HPLC Shimadzu 190 191 LC20A apparatus with a diode array detector (DAD) SPD-20AV and an autosampler SIL-20A. For ERY detection, the HPLC was fitted with a Shim-pack XR-ODS C18 (3.0 mm ID  $\times$  50 mm, 192 Shimadzu) column. As mobile phase-A a 0.025 M phosphate buffer (pH 2.5) was used and as 193 mobile phase-B acetonitrile was used. The analyses were performed in isocratic mode, with 40 % of 194 the mobile phase-A and 60 % of the mobile phase-B at a flow rate of 1.0 mL min<sup>-1</sup>. 20 µL of the 195 196 sample were injected and the DAD was set in  $\lambda = 210$  nm. In these conditions, the ERY retention time was 4.8 min. 197

The generated carboxylic acids were detected by ion-exclusion HPLC using a Rezex Roa-Organic acid H<sup>+</sup> (8 %, 100 × 4.6 mm) column and the DAD was set at  $\lambda = 210$  nm. These 199 measurements were performed by injecting 20 µL of the samples into the HPLC and using a 200 0.05 M H<sub>2</sub>SO<sub>4</sub> solution as mobile phase, at a flow rate of 0.1 mL min<sup>-1</sup>. At these conditions, ion 201 exclusion chromatography exhibited peaks related to oxalic, tartaric, formic, acetic, propionic and 202 203 isovaleric acids, at retention times of 6.16, 7.78, 11.65, 12.65, 14.75 and 20.82 min, respectively.

204

#### 3 **RESULTS AND DISCUSSION** 205

#### 3.1 Adsorption and photocatalytic tests 206

207 The ADS test is an important step in catalytic processes, considering that oxidation and reduction reactions will happen just for molecules that are in direct contact with the catalyst surface, 208 where the radicals are produced (Gaya and Abdullah, 2008; Humayun et al., 2018). Therefore, the 209 ADS tests in Fig. 2a indicate that the different adsorption behavior of the catalysts probably will 210 induce different ERY removal rates by photocatalysis. It was observed that the commercial mesh 211 catalyst (CM) presented the worst ADS results, when compared to all catalysts prepared by the 212 washcoating method. This infers that the method used in the catalysts preparation may have an 213 effect on the surface area, pore geometrical structure and catalyst loading (Thomas and Thomas, 214 215 2015), influencing the ADS process.

Besides, the M3 catalyst exhibited better ADS properties than the other catalysts prepared 216 by washcoating, indicating that the order of the addition or the tin source used in the washcoating 217 procedure have an influence on the ADS results. For the M3 catalyst, the addition of tin oxalate into 218 the washcoating suspension probably led to the formation of a high-quality solid solution which 219 results in a better ADS process. Furthermore, after 60 min of ADS tests the ERY concentration 220 presented little variation, which may indicate a saturation of the catalyst surface 221 (Konstantinou and Albani, 2004; Tong et al., 2012). 222

A study conducted by Karaolia et al. (2018) showed that the ERY adsorption onto TiO<sub>2</sub> Degussa P25 is low and only 7 % of ERY degradation occurs on the surface of the immobilized catalyst. The authors attributed the low ERY adsorption to the low electrostatic attraction of the TiO<sub>2</sub> Degussa P25 surface with ERY, because ERY does not have  $\pi - \pi$  bonds in its structure, a characteristic that would favor polarization and electrostatic attraction between the surface of TiO<sub>2</sub> Degussa P25 and ERY. The low specific surface area and porosity of TiO<sub>2</sub> are characteristics that may also explain the low ADS of ERY (Ayoub et al., 2019).

On the other hand, Sn-doped  $TiO_2$  shows better adsorption due to the fact that the addition of Sn in the crystalline network of titania causes an increase in the photocatalyst surface area and a height reduction of the grain boundary electron barrier, allowing a greater electron transfer from ERY into the photocatalyst (Krishnan et al., 2017). Therefore, the conductivity of this composite is highly enhanced, what should create a suitable surface chemistry, which could enable the photocatalyst surface to the ERY adsorption (Krishnan et al., 2017).

236

#### Figure 2.

237

The surface electrical charge of  $TiO_2$  and  $SnO_2$ -doped  $TiO_2$  catalysts present positive values in the same pH of the ADS and HP tests, as seen by the Zeta potential as a function of pH (Kusior et al., 2019) Similarly, at this pH, ERY presents a pKa = 8.89 (Schafhauser et al., 2018). This behavior negatively influences the approach and adsorption of ERY on the surface of these catalysts due to electrostatic repulsion. In this work it was decided not to perform the correction or to control the pH before and during testing in order to obtain results for natural pH values of ERY in water.

The specific load results (Table 1) show that the M3 catalyst has the highest value among all structured catalysts. The highest ADS value obtained by the M3 catalyst may also be related to its higher specific load value, because a higher ADS of organic compounds is related to the mass of catalyst (Kusior et al., 2019).

However, other characteristics of the surface, such as greater surface area and a reduction of the grain boundary electron barrier (Krishnan et al., 2017), may be related to ERY ADS, because it was observed that the M1 catalyst had a higher specific load value and lower ADS results than the M2 and M3 catalysts.

As already shown in the literature, depending on the emission spectrum of the artificial irradiation source (UV-A, UV-B or UV-C) and the energy of its photons, ERY can undergo DP, mainly with sources of UV-C radiation (Franzen Ramos et al., 2020; Hassib et al., 2011). Aiming to evaluate the possibility of ERY photolysis, tests were carried out in the reactor (Fig. 1) without catalysts, using the 9 W UV-A lamp which emits 12 W m<sup>-2</sup> at 365 nm (see supplementary material, Fig. S2).

Fig. 2b shows that DP plays a discrete role in the ERY oxidation, contributing to 29 % and 259 13 % in degradation and mineralization, respectively. This finding can be associated to the low 260 absorbance of UV-A radiation by ERY, as ERY is considered a weakly absorbing macrolide 261 antibiotic (Hassib et al., 2011). Studies conducted by Franzen Ramos et al. (2020) and 262 Rattanapoltaveechai et al. (2007) showed that ERY presents a small peak of absorbance at 285 nm 263 (UV-C), far from the radiation emitted by the UV-A lamp used in this work. In fact, it is known that 264 only 3-5 % of the solar radiation reaching the earth surface is composed by UV-A 265 (Del Angel et al., 2018; Wei et al., 2018). Therefore, ERY degradation in natural environments is 266 difficult, being, for this reason, considered as a contaminant of high photodegradation difficulty 267 (Batchu et al., 2014; Fernández et al., 2019; Karaolia et al., 2018; Li et al., 2014; 268 Palmisano et al., 2015; Franzen Ramos et al., 2020; Voigt and Jaeger, 2017). 269

Fig. 2b and 2c showed that the commercial mesh (CM) catalyst presented similar degradation and mineralization results to those found during the DP test. This result was not expected, since the CM should be excited by UV-A irradiation, generating the  $e_{cb}^{-}/h_{vb}^{+}$  pairs, and, as a consequence, radicals should be formed and act on the ERY oxidation. This infers that the generation of the pair  $e_{cb}^{-}/h_{vb}^{+}$  does not occur effectively, or that there are large electronic recombination, leading to a lower ERY oxidation.

On the other hand, all prepared catalysts, with or without tin, showed better ERY oxidation 276 results than CM. Possible causes for the lower photocatalytic activity of this commercial catalyst 277 may be due to the composition of 70 %  $TiO_2$  in the form of rutile, which has less photocatalytic 278 activity compared to the anatase form (Pelegrini et al., 2001). Another fact that can explain the 279 lower oxidation result is that TiO<sub>2</sub>/RuO<sub>2</sub> catalysts are considered active catalysts, which means that 280 they have a strong interaction between the HO' generated radical during photocatalysis and the 281 catalyst surface, which makes this radical less available for the oxidation of organic matter 282 283 (dos Santos et al., 2011).

The M1 catalyst (tin-free coverage) exhibited better results than the commercial mesh CM. The possible explanation can be related to the higher  $TiO_2$  load in M1 than in CM. Besides, the TiO<sub>2</sub> source used in M1 is Degussa P25, a known catalyst that has a specific surface area of 50 m<sup>2</sup> g<sup>-1</sup>, a proportion of the crystalline phase of 80 % anatase and 20 % rutile and a particle diameter of 21 nm. These properties turn Degussa P25 one of the most used catalysts. Other works conducted by Trindade et al. (2018) and da Silva et al. (2016) have also shown that the catalysts prepared by the washcoating method showed similar or better results when compared to the CM.

The prepared catalysts M2 and M3 presented better results than M1 for ERY degradation and mineralization, what is associated to the presence of Sn in their composition. Doping TiO<sub>2</sub> with other materials, such as metals, semiconductors or inorganic acids, aims to increase the lifetime of the  $e_{cb}^{-}/h_{vb}^{+}$  pair formed during the irradiation of the catalyst surface with UV or visible light, if the component used in doping absorbs this radiation, thus allowing higher degradation of the contaminants (Del Angel et al., 2018; Humayun et al., 2018; Kusior et al., 2019).

In this case, the titanium oxide doped with tin can result on the formation of a  $Ti_{1-x}Sn_xO_2$ solid solution, leading to a lower internal recombination of the  $e_{cb}^-/h_{vb}^+$  pairs and increasing the

photocatalytic activity (Kusior et al., 2019; Moniz et al., 2015). However, this improvement in
catalytic activity did not occur for catalysts M4 and M5 that also have tin in their composition.

Fig. 2b also shows an exponential decay, typical of pseudo-first order reactions, mainly for 301 the degradation of antibiotics (Franzen Ramos et al., 2020). Based on this assumption, the constants 302 303 were estimated for the first 60 min of reaction, using a well-known pseudo-first order equation to estimate the kinetic constants presented in the inset on Fig. 2b. The results show that the M3 304 catalyst had the highest kinetic constant value, which indicates that the process occurred more 305 quickly in this structured catalyst compared to other ones, a behavior that may be linked to the type 306 II heterostructure formed (Kusior et al., 2019). The kinetic constant of the CM showed a lower 307 result than the DP process, which indicates that the photocatalytic processes did not occur 308 309 effectively, probably due the high presence of the rutile form.

Tin-doped titanium oxide can lead to the formation of three different types of heterostructures, defined as the interfacial union of two or more components (Fig. 3) (Del Angel et al., 2018), and only one of them leads to an improvement in the photocatalytic activity.

A type I heterostructure, or straddling gap, is formed by the junction of two components 313 314 where the conduction band of a component A presents greater energy, while presenting a valence band with lower energy, when compared to the other component B (Del Angel et al., 2018; Moniz 315 et al., 2015). In this way the transfer of  $e_{cb}^-/h_{vb}^+$  occurs from one component to the other, causing the 316 accumulation of these loads in only one of them (Moniz et al., 2015). This accumulation in only one 317 component, besides not decreasing the internal recombination rate, provides the accumulation of 318 charges in the component that has a lower redox potential, what significantly decreases the 319 320 formation of HO<sup>•</sup> during heterogeneous photocatalysis (Low et al., 2017).

At the type II heterostructure, or staggered gap, photoinduced charge separation effectively occurs, since the lowest energy state for  $h_{vb}^+$  may be on one side of the junction, whereas the lowest energy for  $e_{cb}^-$  will be on the opposite side (Del Angel et al., 2018; Kusior et al., 2019). This separation of charges provides increased lifetime of the loads generated, that, through chain reactions, perform the degradation of organic compounds (Del Angel et al., 2018; Kusior et al.,2019).

The type III heterostructure, or broken gap, occurs at the junction of two components with a big difference between the components bands, which does not provide transfer of loads generated between components to another (Kusior et al., 2019). This heterojunction is achieved when solid Zschemes are built (Del Angel et al., 2018).

The M3 behavior may be linked to the formation of heterojunction staggered gap (type II) that increases the lifetime of the charges generated during the photocatalytic process (Fig. 3), by allowing the transfer of  $e_{cb}^-$  from TiO<sub>2</sub> to SnO<sub>2</sub> and  $h_{vb}^+$  from SnO<sub>2</sub> to TiO<sub>2</sub>, diminishing internal recombination (Kusior et al., 2019).

335

# Figure 3.

336

The pH values did not vary significantly during the HP tests, with an average initial value of 5.4  $\pm$  0.1 and a final one of 4.7  $\pm$  0.2. This decrease in the pH values during the HP tests can be associated to the formation of organic acids. Slightly acidic pH values (around 5) lead to better mineralization of ERY, since most of the by-products generated during HP have a negative charge in acidic pH solutions, what favors the adsorption on the positive surface of TiO<sub>2</sub> and TiO<sub>2</sub>/SnO<sub>2</sub> catalysts (Fernandez et al., 2019; Li et al., 2014).

343

#### 344 **3.2 Carboxylic acids generation**

Fig. 2b and 2c show a difference in removal values between degradation and mineralization, suggesting that ERY oxidation occurs in more than one step. During the ERY photocatalysis, first the cleavage of the C – C bonds of the ERY molecule occurs, mainly by the action of the  $HO_{ads}^{\bullet}$ , where, through the internal cyclization, the generation of by-products occurs, such as heterocyclic compounds, aromatic esters and aliphatic tertiary amines (Llorca et al., 2015; Pérez et al., 2017). These by-products then undergo catalytic degradation processes, also mainly due to the action of HO<sup>•</sup>, leading to the production of low-molecular-weight organic acids (Llorca et al., 2015;
Pérez et al., 2017).

During the photocatalytic tests, the presence of formic (1 carbon), acetic (2 carbons) and isovaleric (5 carbons) acids was not detected with any of the tested catalysts, as exhibited in Fig. 4. However, an intense production of oxalic (2 carbons, Fig. 4a), propionic (3 carbons, Fig. 4b) and tartaric (4 carbons, Fig. 4c) acids in the experiments carried out with all tested catalysts was observed. The proportion value (in %) of each carboxylic acid was calculated by dividing the C/C<sub>0</sub> value divided by the sum of the C/C<sub>0</sub> values of all the carboxylic acids detected.

The generation of lower chain organic acids, such as formic (1 carbon), oxalic and acetic (2 carbons) and propionic (3 carbons) acids, indicates that one more step is necessary to lead to mineralization (Serpone et al., 2005). On the other hand, the generation of tartaric (4 carbons) and isovaleric (5 carbons), or higher chain acids, indicates that one more degradation step must be taken to achieve the total mineralization, because acids with 4 or more carbons must be broken into smaller acids (1-3 carbons) (Gandhi et al., 2012; Pérez et al., 2017; Serpone et al., 2005).

M5 and CM lead to the formation of organic acids and their degradation in smaller amounts, when compared to the other catalysts (not shown). This result is expected, since M5 and CM present lower ERY adsorption, degradation and mineralization (Fig. 2a, 2b and 2c, respectively).

368

#### Figure 4.

369

For all catalysts, except M3, a high generation of tartaric acid during the HP tests was found. The production of carboxylic acid with 4 carbons may be linked to the lower generation of the HO<sup>•</sup> by these catalysts, reducing the ERY oxidation until mineralization. The production profile of tartaric acid during the HP evaluation with M3 was a typical for an intermediate product, having a maximum between 5 - 15 min (Fig. 4d). The different behavior of the M3 catalyst, resulting in lower production of carboxylic acids with more or equal 4 carbons, as well as in higher adsorption, degradation and mineralization, may be associated to a successful formation of heterojunction type 377 II (Fig. 4). This structure would increase the lifetime of the  $e_{cb}^-/h_{vb}^+$  pairs, favoring the ERY 378 oxidation by HO<sup>•</sup> and  $O_2^{-•}$  generated at the M3 surface.

379

#### 380 **3.3 Stability assessment**

After ADS and photocatalytic tests with all the prepared structured catalysts (M1, M2, M3, M4 and M5) and with the commercial mesh (CM), it was found that M3 exhibited the best results, resulting in 67 % of ERY degradation and 46 % of mineralization. Therefore, long-term tests were performed with this catalyst. For this purpose, the tests were carried out in the same conditions that the previously ones and in the same reactor (Fig. 1).

After 240 min (first test - Fig. 5a), 67 % and 47 % of ERY degradation and mineralization were obtained, respectively. After 2280 min (twelfth test), a decrease of 50 % in the degradation and 29 % in the mineralization of ERY was observed. This decrease may be related to the poisoning of the catalyst surface, caused by the adsorption of by-products generated in the ERY photocatalysis.

In a study conducted by da Silva et al. (2016), using a TiO<sub>2</sub>-foam, a reduction in the mineralization of nonylphenol ethoxylated was found after ten cycles (600 min), and it was caused by the degradation by-products deposition on the catalyst surface. The photocatalytic activity was restored after cleaning steps. Moreover, Mugunthan et al. (2019) studied the diclofenac degradation over a TiO<sub>2</sub>–SnO<sub>2</sub> catalyst and found a degradation reduction from 89 % to 53 % after 4 cycles (1200 min). The authors attributed the poisoning effect to the accumulation of by-products on the catalyst surface, which led to a decrease in the number of exposed active sites.

In order to try to restore the M3 catalytic activity, a cleaning step with a HNO<sub>3</sub> solution (10% v.v) and with deionized water was performed after the twelfth test. Subsequently, photocatalytic tests were carried out and the results are presented in Fig. 5a. These show that a great part of the activity of M3 was restored (57 % in degradation and 37 % in mineralization), indicating a high catalytic stability.

#### Figure 5.

404

To elucidate the behavior of the decrease in ERY degradation and mineralization found in the long-term tests (Fig. 5a), the organic acids analysis was also performed. Fig. 5b shows that from the sixth long-term test (1200 min) there is a decrease in the production of oxalic acid (2 carbons) and an increase in the generation of tartaric acid (4 carbons), in relation to the proportion of the analyzed acids. It is also noted, from the eleventh test (2400 min), the generation of formic (1 carbon), acetic (2 carbons) and isovaleric (5 carbons). The chromatograms of organic acids obtained through HPLC are shown in Fig. S3 (see supplementary material, Figure S3).

The results presented in Fig. 5b corroborate those shown in Fig. 5a. A loss of the photocatalytic activity of the M3 catalyst was observed. This may be related to the catalyst detaching from the substrate or to the poisoning of its surface. These problems lead to a decrease in the generation of HO<sup>•</sup>, and, as a direct consequence, to a higher production of organic acids, mainly with 5 carbons; also to less mineralization. However, after a cleaning step with nitric acid solution (10% v.v), the activity of the M3 catalyst was restored and formic, acetic and isovaleric acids were no longer detected.

Based on all the obtained information on adsorption, degradation, mineralization and formation of organic acids, a mechanism for charge transferring between  $TiO_2$  and  $SnO_2$ , and the corresponding generation of radicals and ERY degradation, was proposed in Fig. 6.

When the UV-A lamp is turned-on, there is photon absorption by TiO<sub>2</sub>, and one electron from the conduction band of TiO<sub>2</sub> is transferred to the conduction band of SnO<sub>2</sub> (presented in red color). At the same time,  $h_{vb}^+$  is transferred from the valence band of SnO<sub>2</sub> to the valence band of TiO<sub>2</sub> (blue color). This charge transfer in the heterojunction staggered gap (type II), as shown in Fig. 3, allows a decrease in the internal recombination (green color), favoring the generation of HO<sup>•</sup> and  $O_2^{-\bullet}$ .

- 428 The generation of HO<sup>•</sup>,  $O_2^{-\bullet}$  and  $h_{vb}^+$  at the surface of the M3 catalyst leads to ERY 429 oxidation. Its degradation generates mainly oxalic and propionic acids and mineralization products 430 (CO<sub>2</sub>, H<sub>2</sub>O and inorganic ions).
- 431

#### Figure 6.

432

## 433 **3.4 Morphology and physicochemical characterization of the photocatalytic coatings**

The photocatalytic coatings morphologies are shown in Table 1. The coating of M1 (without Sn) covered uniformly all the wire walls of the mesh, as was reported by Trindade et al. (2018). The same morphology was observed on M2, M3 and M4, despite the Sn addition. However, the use of SnO<sub>2</sub> nanoparticles (M5) had an undesirable effect on the coating morphology; some agglomerations on the surface and wire intersections were generated and those could affect its adherence. The coatings loadings, expressed as mg per cm<sup>2</sup> of wire, were quite similar for the five structured catalysts, being these values between 4.2 and 4.9 mg cm<sup>-2</sup>.

441

#### Table 1

Moreover, the elemental chemical composition of each Sn-Ti based coating was estimated via SEM/EDS in different regions. The bulk Sn/Ti ratios and the average weight percentages of Sn with their standard deviations (SD) are presented in Table 1. The Sn/Ti ratio of M2 resulted to be the highest value obtained for these coatings as a consequence of the method used for the Sn incorporation, which was a Sn oxalate impregnation. This procedure generated a high Sn loading and a heterogeneous distribution over the coating, as indicated by its standard deviation. Therefore, some regions with SnO<sub>2</sub> particles accumulations were generated on this structured catalyst.

Contrarily, the incorporation of SnO<sub>2</sub> in the washcoating suspension as microparticles (M4)
and nanoparticles (M5) drove to lower bulk Sn/Ti ratios and weight percentages of Sn (Table 1).
However, their standard deviations were high, indicating that the Sn distribution in those coatings
was not uniform.

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453 On the other hand, when the washcoating suspension contained tin oxalate together with the 454 other components, the obtained coating (M3) presented a homogeneous distribution of Sn along the 455 coating wires, with a low SD of the Sn wt. % (± 0.03%) and a Sn/Ti ratio of 0.025.

The weight composition of the CM catalyst is 21.5 % Ti and 18.3 % Ru (Table 2 and Fig. S4 at supplementary material), being the atomic percentage 70 % Ti and 30 % Ru. The obtained values were close to those reported by the manufacturer company (71.4 % Ti and 28.6 % Ru).

- 459
- 460

## Table 2

461

462 After three reaction tests, the CM catalyst retained a high percentage in weight of carbon 463 (39.0%), which can explain its lower catalytic activity compared to the Ti/Sn based catalysts.

The fresh M3 catalyst presented a tin weight percentage of  $0.20 \pm 0.03\%$  on the coating (Table 2). The presence of Sn in concentrations higher than 1.0 %, may not be beneficial for the photocatalytic activity (Lin et al., 1999). When this Sn concentration is exceeded, Sn is not inserted into Ti interstitial spaces, leading to the formation of free SnO<sub>2</sub>. In this situation, the photocatalytic activity will be impairing because SnO<sub>2</sub> has a larger bandgap than TiO<sub>2</sub>. Besides, the type II heterojunction between SnO<sub>2</sub> and TiO<sub>2</sub> will not be formed (Lin et al., 1999).

In addition, the deposition of organic content (presence of 9.05 % carbon) on the surface of the M3 catalyst after all tests (more than 400 h) was measured (Table 2), confirming the results found in Fig. 5a and 5b. The cleaning step of the M3 catalyst was successful in removing the organic content present on its surface, therefore restoring its catalytic activity. However, the catalytic activity recovery was not of 100 %. This fact can be linked to the presence of a 5.4 % of iron (Table 2), which is a component of the AISI 304 stainless steel used as a substrate, indicating a partial detaching of the catalyst anchored to the substrate surface.

The crystalline phases of the coatings were identified by XRD (Fig. 7). For all structured 477 catalysts (M1-M5), the main phase of TiO<sub>2</sub> was anatase (JCPDS Card nº 01-084-1285). However, 478 the contribution of TiO<sub>2</sub> in rutile (JCPDS Card nº 21-1276) form was also observed. Therefore, 479 after the washcoating procedure the TiO<sub>2</sub> phase structures remained as those of P25, as reported by 480 481 Trindade et al. 2018. The greater presence of anatase explains the higher activity of these catalysts in relation to the CM catalyst  $Ti_{0.7}Ru_{0.3}O_2 - Ti$ , in which  $TiO_2$  is under the rutile form, and that it 482 has less catalytic activity, due to greater internal recombination of  $e_{cb}^-/h_{vb}^+$  pair (Babic et al., 2017). 483 In addition to the presence of  $TiO_2$  in the rutile structure in the CM catalyst (Fig. 7), which has less 484 catalytic activity compared to the anatase form, carbon hinders the ability to generate radicals that 485 are characteristic of AOP processes. This suggests that the prepared structured catalysts (M1 to M5) 486 present better hydrodynamics and catalytic characteristics which result in less carbon accumulation 487 on the catalyst surface. 488

The diffraction signals of tetragonal ZrO<sub>2</sub> (JCPDS Card n<sup>o</sup> 79-1769) were also observed in 489 Figure 7. Nanoparticles of  $ZrO_2$  were added in the washcoating suspension as binder in order to 490 increase the anchorage among the catalytic particles and the structured substrate surface (Trindade 491 et al., 2018). Furthermore, two small diffraction signals at 43.67° and 44.76°, attributed to  $\gamma$ -Fe 492 (JCPDS Card n° 00-006-0696) and  $\alpha$ -Fe (JCPDS Card n° 01-087-0722), were distinguished in the 493 494 M2-M5 samples. These phases belong to the wire meshes used as substrates. Besides, no diffractions associated to Sn species were observed. This absence is due to the small bulk 495 concentration of Sn species with respect to  $TiO_2$  (Sn/Ti ratio: 0.012). 496

497

#### Figure 7

To evaluate the formation of the  $Ti_{1-x}Sn_xO_2$  solid solution the XRD results were used to calculate the lattice constants (a, b and c), unit cell volume and interplanar distance (Miller index 101) of the TiO<sub>2</sub> anatase, the main form of TiO<sub>2</sub> in the M1-M5 photocatalysts. To calculate the lattices values of the structured photocatalysts, the Bragg equation was used and compared with the TiO<sub>2</sub> anatase (JCPDS Card n<sup>o</sup> 01-084-1285) and cassiterite SnO<sub>2</sub> (JCPDS Card n<sup>o</sup> 00-041-1445) values (Yang et al., 2011). Table 3 shows the lattice values, unit cell volume and interplanar
distance for each structured photocatalyst, pure TiO<sub>2</sub> anatase and pure SnO<sub>2</sub> (Miller index 111).

505

#### Table 3

An increase in the values of the lattice constants, unit cell volume and interplanar distance 506 for the structured photocatalyst M3 in relation to the structured photocatalyst M1 (without Sn) and 507 to  $TiO_2$  pure anatase was observed (Table 3). This increase in the lattice constants of  $TiO_2$  anatase 508 suggests that some  $Ti^{4+}$  is replaced by  $Sn^{4+}$  in the crystalline network of the  $TiO_2$  anatase phase 509 (Yang et al., 2019). This substitution induced the effective formation of a Ti<sub>1-x</sub>Sn<sub>x</sub>O<sub>2</sub> solid solution 510 in M3 (Yang et al., 2019, Chen et al., 2013). For the other structured photocatalysts (M2, M4 and 511 M5) there were no significant changes in the values of the constant lattices and interplanar distances 512 in relation to M1 (without Sn) and TiO<sub>2</sub>, which indicates that in these photocatalyst structures the 513 formation of Ti<sub>1-x</sub>Sn<sub>x</sub>O<sub>2</sub> solid solution does not occur. Thus, the incorporation of Sn oxalate to the 514 washcoating suspension favors the insertion of  $Sn^{4+}$  in the TiO<sub>2</sub> structure. 515

The Sn-containing photocatalytic coatings obtained in this work presented crystallite sizes higher than that of M1 (Table 3). Maver et al. reported a similar effect on Ti-Sn samples prepared by the sol-gel method. The authors observed that at low Sn loadings the calcination process promoted the formation of larger crystallites of the crystalline phases, while at higher Sn contents this behavior was not verified (Maver et. al 2020).

Table 4 displays the obtained surface data for the Sn-doped structured photocatalysts. The Ti 2p, Zr 3d, Sn 3d and O 1s regions were analyzed. In anatase bulk TiO<sub>2</sub> the Ti  $2p_{3/2}$  and Ti  $2p_{1/2}$ peaks appear at 458.7 – 458.9 eV and 464.4 – 464.6 eV, respectively, indicating Ti<sup>4+</sup> in TiO<sub>2</sub> (Mahy et al., 2019; Mintcheva et al., 2019). In the case of the Sn-doped photocatalysts the peaks were shifted to lower binding energies – BEs – (458.4 – 458.5 eV), which could indicate a partial reduction of Ti<sup>4+</sup> to Ti<sup>3+</sup> and is associated to the presence of oxygen vacancies at the surface of these Sn-doped catalysts (Toloman et al., 2019; Zhao et al., 2020; Yang et al., 2019). Particularly,

the Ti  $2p_{3/2}$  peak for M4, whose Sn source was powder SnO<sub>2</sub>, was very close to that of pure TiO<sub>2</sub>, inferring that this method did not induce changes in the Ti surface environment. On the other hand, the Zr  $3d_{5/2}$  signal in all Sn-doped structured catalysts was found to be 182.0 - 182.1 eV, practically equal for all doped structured catalysts, with a spin-orbit splitting of 2.4 eV, characteristic of Zr<sup>4+</sup> in ZrO<sub>2</sub>

(Bronsato et al., 2020; Liu et al., 2019). The fact that the BEs of these catalytic systems were almost
the same for Zr but slightly different for Ti suggests that Sn incorporation affected the Ti surface
environment but not the Zr environment.

Some changes in the surface were also observed by the analysis of the Sn 3d region. Bulk 536 SnO<sub>2</sub> presents its Sn 3d<sub>5/2</sub> peak at 486.7 – 487.0 eV with a spin-orbit splitting of 8.4 eV 537 538 (Um et al. 2019). This peak was found at lower BEs than that of bulk  $SnO_2$ , 486.2 – 486.3 eV, for M2, M3 and M5. This shift to lower binding energies is due to the higher electronegativity of Sn 539 compared to Ti (Um et al. 2019; Duan et al., 2012). Furthermore, this value was very close to bulk 540 SnO<sub>2</sub> for M4, as it was the case with the Ti analysis. These results indicate that in M4 the 541 interaction between Sn and Ti is very weak. Also, all the catalysts presented a small shoulder at ~ 542 484 - 485 eV, assigned to Sn<sup>2+</sup> species (Toloman et al., 2019, Bjelajac et al., 2020). 543

Additionally, the O 1s region was investigated in order to study the surface oxygen species 544 associated with oxygen vacancies. It is reported in the literature that changes induced in TiO<sub>2</sub>, i. e. 545 Sn doping, can lead to the generation of defects in this compound associated to oxygen vacancies 546 (Zhao et al., 2020; Yang et al., 2019). Furthermore, several publications reported that oxygen 547 vacancies promote the reduction of the electron-hole pairs recombination and therefore enhance the 548 photocatalytic degradation performance for organic pollutants (Zhao et al., 2020, Li et al., 2016; 549 Tian et al. 2018). All Sn-doped O 1s spectra revealed two oxygen species: 529.7 - 529.9 eV, 550 associated to crystal lattice oxygen ( $O_L$ ), and 531.6 – 531.9 eV attributed to absorbed oxygen 551 species (O<sub>V</sub>, oxygen vacancies) [4,12]. The O<sub>V</sub>/O<sub>L</sub> ratios were obtained for the Sn-doped structured 552 553 catalysts and it was found that this value was the highest for M3 (0.17), slightly lower for M2 (0.15)

- and lower for M4 and M5 (0.11 and 0.12 respectively), in close agreement with their respective
- photocatalytic performances (Fig. 2).
- 556

## Table 4

557



#### 558 4 CONCLUSIONS

The degradation of ERY by heterogeneous photocatalysis was investigated using a series of TiO<sub>2</sub> and Ti<sub>1-x</sub>Sn<sub>x</sub>O<sub>2</sub> catalysts prepared by the washcoating method. Tests of adsorption, degradation and mineralization of ERY were done and the production of carboxylic acids was evaluated. Longterm tests and physicochemical characterization were carried out. A scheme demonstrating the formation of the heterojunction, its electron transfer, generation of radicals and the route of degradation and mineralization of ERY was also proposed.

It was found that the order and type of Sn sources incorporated in the synthesis procedure 565 affect the catalytic activity due to the formation of a solid solution with different type of 566 heterostructures. An improvement in the catalytic properties was associated to the incorporation of 567 568 tin into the titanium oxide matrix, which takes place in the M3 structured system. The characterization of this structured system suggested the Ti-Sn-O solid solution formation, due to the 569 utilization of tin oxalate for the generation of the catalytic film. This fact is also coupled with its 570 morphological features such as the staggered gap (type II) formation and with the optimized 571 titanium to tin molar ratio. In this situation, there is a better separation of the electron/hole pairs, 572 favoring the generation of hydroxyl radicals and the ERY oxidation. 573

The long-term tests showed a loss of catalytic activity which was related to the presence of organic compounds and to a partial loss of catalytic material. Nevertheless, after a cleaning step, the activity of the catalyst was almost completely restored. In fact, the catalyst with better results in terms of ERY degradation and mineralization (M3) showed high stability in long-term tests up to 3360 min. The obtained results show the possible use of Ti-Sn structured photocatalysts for water and wastewater treatment.

580

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**Fig. 1.** Scheme of the photocatalytic reaction system, where 1 is the non-irradiated reservoir, 2 is the photocatalytic reactor and 3 is the peristaltic pump (Masterflex<sup>®</sup>  $L/S^{®}$  Easy-Load<sup>®</sup>).

**Fig. 2.** Evaluation of the prepared catalysts M1, M2, M3, M4, M5 and commercial one (CM) on ERY (a) adsorption, (b) degradation and (c) mineralization. Experimental conditions: ERY = 50 mg  $L^{-1}$ , pH = 5.4 at room temperature.

**Fig. 3.** Scheme of electron transfer principle from (A)  $SnO_2$  into (B)  $TiO_2$  (a) straddling gap (type I), (b) staggered gap (type II) and (c) broken gap (type III).

**Fig. 4.** Short carboxylic acids detected during photocatalytic evaluation for all catalysts. Where (**a**) is oxalic acid , (**b**) is propionic acid and (**c**) is tartaric acid. The profile of the short carboxylic acids generated and consumed during the photocatalytic test for the M3 catalyst are presented in (**d**). Experimental conditions: ERY = 50 mg L<sup>-1</sup>, pH = 5,4 and room temperature.

**Fig. 5.** M3 long-term photocatalytic tests before (0 - 2880 min) and after cleaning step (2880 - 3360 min) for **(a)** degradation and mineralization and **(b)** short carboxylic acid proportion of propionic (in red), tartaric (in green), oxalic (in pink), isovaleric (in orange), acetic (in magenta) and propionic (in blue) acids during the M3 long-term tests. Last 2 tests were carried out after cleaning the photocatalyst with HNO<sub>3</sub>. Experimental conditions: ERY = 50 mg L<sup>-1</sup>, pH = 5.4 and room temperature.

**Fig. 6.** Possible heterojunction staggered gap (type II) scheme formed between  $TiO_2$  and  $SnO_2$  in the prepared catalysts M3, and its action in the ERY oxidation. Adapted from Moniz *et al.* (2015).

**Fig. 7.** X-Ray diffractograms for the structured catalysts, the commercial one, SnO<sub>2</sub> and TiO<sub>2</sub> Degussa P25. Symbols:  $\blacksquare$  TiO<sub>2</sub> – Rutile,  $\blacktriangle$  TiO<sub>2</sub> – Anatase,  $\bigoplus$  ZrO<sub>2</sub> – Tetragonal,  $\blacklozenge$  SnO<sub>2</sub>,  $\blacktriangleleft \gamma$ -Fe,  $\triangleright \alpha$ -Fe.

# Table 1. Morphology and loadings of the M1 to M5 structured photocatalysts and physicochemical

Structured catalyst	Method of Sn Addition	Specific loading (mg/cm <sup>2</sup> )	Bulk Sn/Ti	Bulk Sn % (SD)
M1	-	4.5	-	-
M2				
	Impregnation of Sn-oxalate	4.2	0.180	2.90 (0.90)
M3				
	Sn-oxalate added to washcoating suspension	4.9	0.025	0.20 (0.03)
M4	$\mathcal{O}_{\mathcal{I}}$			
	SnO <sub>2</sub> particles added to washcoating suspension	4.2	0.002	0.03 (0.02)
M5				
	SnO <sub>2</sub> nanoparticles added to washcoating suspension	4.3	0.013	0.22 (0.10)

characterization of the SnO<sub>2</sub>-TiO<sub>2</sub> based photocatalytic coatings.

Table 2. Elemental mapping, in weight %, obtained by SEM/EDS of the fresh M3 catalyst, used

Element	Fresh	After 400 h	Commercial mesh (CM)
Oxygen	$70.90\pm2.10$	$53.29 \pm 6.65$	$20.66 \pm 16.41$
Zirconium	$9.20\pm0.40$	$11.01 \pm 0.06$	n. d.
Titanium	$19.60 \pm 1.90$	$19.28\pm3.80$	$21.53 \pm 8.53$
Tin	$0.20\pm0.03$	n. d.	n. d.
Carbon	n. d.	$9.05\pm3.94$	$38.98 \pm 3.62$
Iron	n. d.	5.44 ± 2.22	n. d.
Ruthenium	n. d.	n. d.	$18.28 \pm 6.55$

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## M3 catalyst after all tests (> 400 h) and commercial mesh (CM).

n.d. - not detected

Sample	Lattice constants			Unit cell volume	Interplanar distance	Crystallite size
Sample	a (Å)	b (Å)	c (Å)	(Å <sup>3</sup> )	d (Å)	(nm)
M1	3.786	3.786	9.509	136.303	3.531	13.82
M2	3.785	3.785	9.501	136.088	3.537	20.98
M3	3.791	3.791	9.521	136.856	3.542	18.02
M4	3.779	3.779	9.480	135.385	3.650	19.84
M5	3.781	3.781	9.500	135.809	3.541	20.54
TiO <sub>2</sub> Anatase <sup>a</sup>	3.785	3.785	9.512	136.262	3.516	-
SnO <sub>2</sub> cassiterite <sup>b</sup>	4.738	4.738	3.187	71.55	3.347	_

## **Table 3.** $TiO_2$ crystallite sizes of the different coatings and their lattice parameters.

<sup>a</sup> Data from JCPDS Card nº 01-084-1285

<sup>b</sup> Data drom JCPDS Card nº 00-041-1445

	Main peak BE of Sn	Main peak BE of Ti	Main peak BE of Zr
Structured catalyst	$3d_{5/2}$	2p <sub>3/2</sub>	3d <sub>5/2</sub>
	(eV)	(eV)	(eV)
M2	486.3 (1.9) <sup>a</sup>	458.5 (1.5)	182.0 (1.8)
M3	486.2 (1.9)	458.4 (1.5)	182.1 (1.8)
M4	486.6 (1.7)	458.6 (1.5)	182.1 (2.2)
M5	486.3 (1.9)	458.4 (1.5)	182.1 (1.9)

## **Table 4.** Surface data of the Sn-doped structured photocatalysts.

<sup>a</sup> FWHM in parenthesis.





Fig. 2.





(b) Type II

(c) Type III

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**Fig. 4.** 



Fig. 5.





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## **HIGHLIGHTS**

- SnO<sub>2</sub>-doped TiO<sub>2</sub> increases the mineralization and degradation of ERY in relation to TiO<sub>2</sub>. •
- Sn addition sources and methods affected the catalyst performance. •
- Formation of low molecular weight carboxylic acids were detected. •
- ERY oxidation pathway onto Ti<sub>1-x</sub>Sn<sub>x</sub>O<sub>2</sub> staggered gap are proposed. •
- The prepared catalyst showed high catalytic activity after more than 400 h of use. •

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#### **Declaration of interests**

 $\boxtimes$  The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

□The authors declare the following financial interests/personal relationships which may be considered as potential competing interests: