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10 Abstract

11 This manuscript reports a systematic study of encapsulation of fish oil into soybean microparticles by emulsification 12 and subsequent spray drying in order to protect it from lipid autoxidation and/or facilitate its handling for 13 incorporation into healthy food products. In particular, the effect of the formulation and the emulsification 14 technique on the physicochemical properties of the resulting emulsions and encapsulates was evaluated. Two 15 emulsifying processes and four protein: oil ratios were analyzed. Soy proteins managed to encapsulate the fish oil, 16 masking its characteristic odor and its oily texture into matrix type microcapsules, as was observed by confocal 17 microscopy. The emulsification process was determinant in the efficiency of drying and encapsulation as well as in 18 the protection exerted on the oil oxidative stability. Although both, emulsifying and drying processes caused certain 19 initial oil oxidation (verified by peroxide and TBA indexes), some of the studied systems showed a good perspective 20 of oxidative stability over time(studied by accelerated rancimat test). 21 22 23

- 24 *Keywords*: microencapsulation, fish oil, soybean protein, O/W emulsion, spray drying, lipid oxidation.
- 25

26 **1. Introduction**

27

It is well established that omega-3 polyunsaturated fatty acids (PUFAs), especially eicosapentaenoic acid (EPA) and docosahexaenoic acid (DHA), provide important health benefits (Arab-Tehrany et al., 2012; Valenzuela, Tapia, González, & Valenzuela, 2011). Numerous clinical studies and *in vitro* and *in vivo* experiments have confirmed their beneficial effect against cancer (De Deckere, 1999; Hull, 2011), cardiovascular and inflammatory diseases (Bays, 2008; Wang et al., 2006; Yokoyama et al., 2007; Goldberg & Katz, 2007; Kim, 1996; Wall, Ross, Fitzgerald, & Stanton, 2010), and immune and neurological disorders (Damsgaard et al., 2007; Dyall & Michael-Titus, 2008; Amminger et al., 2010).

35 Endogenous synthesis of EPA and DHA from α -linolenic acid (ALA) occurs at a very slow rate (Kralovec, Zhang, Zhang, 36 & Barrow, 2012), therefore their incorporation through diet is recommended (Lands, 2005; Valenzuela et al., 2011) 37 and healthy foods supplemented with these acids are gaining importance in the food market. Marine oils contain 38 large amounts of omega-3 polyunsaturated fatty acids (Bakry et al., 2016). However, due to their low solubility in 39 aqueous solvents, undesirable aroma and high susceptibility to oxidative deterioration, their incorporation into food 40 is a significant challenge (Aghbashlo, Mobli, Madadlou, & Rafiee, 2012, 2013; Aghbashlo, Mobli, Rafiee, & Madadlou, 41 2012). Microencapsulation of fish oil deals to protect unsaturated fatty acids against oxidation and other unwanted 42 reactions caused by environmental conditions (light, temperature, oxygen, humidity), masking of the unpleasant fish 43 oil flavours and improving the stabilization and delivery of omega-3 fatty acids in foods (Ixtaina, Julio, Wagner, 44 Nolasco, & Tomás, 2015; Encina, Vergara, Giménez, Oyarzún-Ampuero, & Robert, 2016, Bakry et al., 2016). 45 Various processes such as spray drying, coacervation and extrusion (Drusch & Berg, 2008; Jiménez-Martín,

Gharsallaoui, Pérez-Palacios, Carrascal, & Rojas, 2015), and shell materials such as chitosan, maltodextrin, sugars,
starch, milk, alginates, plant gums, whey proteins and gelatin have been used to encapsulate fish oil (Garrett, 1965;
McClements, 2012).

Spray-drying technique is extensive used in food industry as it is simple, low-cost, reproducible and easy to scale up.
 Moreover, it is useful for encapsulating heat-sensitive materials such as fish oil because of its short drying times (5-

51 30 s) (Encina et al., 2016) but some active compounds remain exposed on the microparticle surface (de Vos, Faas, 52 Spasojevic, & Sikkema, 2010). Lipophilic molecules of fish oil requires the previous formation of oil-in-water 53 emulsions, whose stability during spray-drying process plays an important role in the retention and stability of fish oil 54 (Drusch, Serfert, Van Den Heuvel, & Schwarz, 2006; Drusch, 2007; Keogh et al., 2001). Proteins have good 55 emulsifying and film-forming properties (Encina et al., 2016) and consequently they are potential encapsulating 56 agents. During emulsion formation, protein molecules are rapidly adsorbed at the newly formed oil-water interface, 57 and the resulting steric-stabilizing layer prevents oil droplet coalescence and provides physical stability to the 58 emulsion (Vega & Ross, 2006). Protein nature determines the strength and flexibility of the layer. Milk proteins 59 (whey and caseins) (Vega, Dalgleish, & Goff, 2005) and gelatin (Bruschi, Cardoso, Lucchesi, & Gremião, 2003) have 60 been the most used in encapsulation but those of plant origin such as soybean, wheat, sunflower begun to be more 61 and more frequently used (Nesterenko, Alric, Silvestre, & Durrie, 2013). Soybean proteins appear to be suitable for 62 the encapsulation of fish oil since they have acceptable water solubility, good adsorption at the water/oil 63 interfaceandadvantageous gelling and film forming properties (Gu, Campbell, & Euston, 2009). Soybean protein 64 concentrates and isolates have been used as encapsulating material of orange oil, palm oil, paprika oleoresin and 65 others (Kim & Morr, 1996; Rusli, Sanguansri, & Augustin, 2006 and Rascón, Beristain, García, & Salgado, 2011) alone 66 or in blends with other biopolymers such as maltodextrin, gelatin, pectin, and others (Yu, Wang, Yao, & Liu, 2007; 67 Favaro-Trindade, Santana, Monterrey-Quintero, Trindade, & Netto, 2010; Mendanha et. al., 2009). As far as we 68 know, only Nasrin & Anal (2015) encapsulated fish oil in culled banana resistant starch-soy protein isolate based 69 microcapsulesdried by lyophilization.

The aim of this work was to encapsulate fish oil with soybean protein isolate by emulsification and subsequent spray drying in order to protect it from lipid **oxidation** and/or facilitate its handling for incorporation into healthy food products. In particular, the effect of the formulation and the emulsification technique on the physicochemical properties of the resulting emulsions and encapsulates was evaluated.

74

75 **2. Materials and Methods**

76 **2.1. Materials**

A commercial soybean protein isolate (**SPI**) SUPRO 500E, kindly supplied by DuPont N & H (Brazil), was used as encapsulating material. The protein content of SPI, as measured by the Kjeldahl method, was 85 ± 2% (w/w on dry basis; N x 5.71). Fish oil (C22:6 docosahexaenoic acid, DHA, >22%, C20:5eicosapentaenoic acid, EPA, >7% with vitamin E, rosemary extract and BHA as antioxidant)was kindly supplied by OmegaSur (Argentina). All the other reagents used in this study were of analytical grade.

82

83 **2.2. Emulsions preparation**

- 84 Oil in water emulsions with different protein:oilmass ratio: 1:1, 2:1, 3:1 and 4:1 were prepared from an aqueous 85 dispersion of SPI (5% w/v) and fish oil addition. They were prepared by two different process: i) using only the high-86 shear probe mixer Ultra-Turrax T-25 (IKA®, Werke GmbH & Co. KG, Germany) with a dispersion tool S25N-18G (rotor 87 diameter 13.4mm) operated at 13,500 rpm for 90 s; and ii) with a second additional step performed with an 88 ultrasonic homogenizer (SONICS Vibra Cell VCX 750, Vibra Cell Sonics Materials Inc., USA) with a standard tip (13 89 mm diameter) immersed 2/3 in a beaker of 70 mm diameter (250 ml volume) in agitation with a magnetic stirrer 90 and in an ice bath. Each formula was sonicated at an output intensity of 50% (375 W) with 30-second on and 30-91 second off pulse for 5 min. 92 Two individually prepared replicates were at least assayed for each condition to confirm the repeatability of the
- 93 process.
- 94 Sodium azide (0.1%, w/v) was added to the emulsions to prevent microbial growth.
- 95
- 96 **2.3.** Emulsion characterization
- 97
- 98 **2.3.1.***Morphology of the droplets*

99 Morphology of the droplets was observed by opticalmicroscopy. Each emulsion (20 µL) was placed on a slidewith a

100 cover and immediately examined with an optical microscope equipped with a Leica DC100 digital camera (Bensheim,

- 101 Germany) using a 100X magnification.
- 102

103 **2.3.2.** Particle size distribution and mean diameters

104 Particle size distribution, and De Broucker (d_{4,3}) and Sauter (d_{3,2}) (Jafari, He, & Bhandari, 2007b) mean diameters of

105 particles of the emulsions were determined by static light scattering (SLS) with a particle size analyzer Malvern

106 Mastersizer 2000E (Malvern Instruments, Worcestershire, UK) at room temperature (20°C). About 1 mL of sample

107 was diluted to 600 mL of water and the pump rate in dispersion unit was set at 2000 rpm (Hydro 2000MU, Malvern

108 Instruments, UK). The refractive indexes of the dispersed and continuous phases were 1.47 and 1.33 respectively.

109 Also, specific surface area was calculated according Equation 1:

110
$$SSA = \frac{6 \varphi}{d_{22}}$$
 (Equation 1)

111 Where: SSA is the specific surface area, ϕ is the phases ratio, $d_{3,2}$ is the Sauter mean diameter(μ m).

112 Measurements were carried out in sixfold.

113

114 **2.3.3.** Rheological behaviour

115 Rheological measurements were carried out with a Haake RS600 controlled stress oscillatory rheometer (Haake, 116 Germany) using a plate-plate sensor system with 1.0 mm gap between plates. Measurements were performed in 117 triplicate at constant temperature ($25 \pm 0.5^{\circ}$ C). The samples were subjected to a logarithmic increasing shear rate 118 with a continuous ramp from 1 to 500 s⁻¹ in 2 min, followed by a steady shear at 500 s⁻¹ for 1 min, and finally a 119 decreasing shear rate from 500 to 1 s⁻¹ in 2 min. 120 Flow behavior of emulsions was described by fitting the experimentally measured data to the Newton model: 121 $\tau = \eta D$ (Equation 2) 122 Where: τ is the shear stress (Pa), *D* is the shear rate (s⁻¹), and η is the viscosity (Pa.s).

123

124 **2.3.4.** Emulsion stability

- 125 Stability of emulsions was determined by measurements of dispersed light with a Vertical Scan Analyzer (Quick Scan)
- 126 (Coulter Corp., Miami, FL, USA) according to Cabezas, Madoery, Diehl & Tomás (2012). The emulsions were
- 127 transferred to cylindrical glass measurement cells immediately after the emulsification. The backscattering of
- 128 monochromatic light (λ = 850 nm) from the emulsions was determined every 1 min for 2 h as a function of the height
- 129 of the sample tube (*ca*. 65mm), at room temperature (20°C).
- 130 Determinations were conducted at least in duplicate.
- 131
- 132 **2.4.** Preparation of microcapsules by spray-drying
- 133 The spray-drying process was performed in a laboratory-scale Mini Spray Dryer Büchi B-290 (BüchiLabortechnik AG,
- 134 Switzerland) equipped with an atomizer nozzle of 700 μm diameter. The emulsions were fed into the main chamber
- 135 (70 cm diameter) through a peristaltic pump and the feed flow rate was controlled by the pump rotation speed (3.1
- 136 mL/min). Drying air flow rate was 357 L/h and compressor air pressure was 6-8 bars. Inlet and outlet air temperature
- 137 were 180±2°C and 96±8°C, respectively.
- 138 The spray-dried microcapsules were collected and stored in caramel colored glass containers and wrapped with
- aluminum foil in the dark at room temperature (20°C) for further analysis.
- 140 Two individually prepared replicates were assayed for each condition.
- 141
- 142 **2.5.** Characterization of microcapsules

143 **2.5.1.** Moisture content and recovered solid yield

- 144 Moisture content (MC) of microcapsules was determined gravimetrically by drying in a vacuum oven (Arcano,
- 145 Argentina) at 70°C and 20 mmHg until constant weight (for 48 h). The sample moisture content analysis was carried
- 146 out immediately after the drying process.

147	The recovered solid yield (SY) was calculated as the ratio of the powder weight collected after each drying
148	experiment (W _f , in dry basis) and the initial amount of components in the prepared emulsions (except water) (W _i , in
149	dry basis), as indicated in Equation 3:
150	$SY(\%) = \frac{W_f}{W_i} 100\%$ (Equation 3)
151	Where: SY is the recovery solid yield (%), W_i is the initial weight of emulsion (except water) (g, in dry basis), and W_f is
152	the powder weight collected after each drying experiment (g, in dry basis).
153	Determinations were carried out in duplicate.
154	
155	2.5.2. Protein content
156	The percentage of protein content of microcapsules was determined according to the Kjeldahl method (f = 5.7)(AOAC
157	920.53). Determinations were carried out in duplicate.
158	
159	2.5.3. Total oil content, free oil content and encapsulation efficiency
160	Total oil (TO) content of microcapsules was based on the Soxhlet method (AOAC Method 920.39) using ethyl ether as
161	extraction solvent. The TO extracted was weighed and expressed as a percentage of oil with respect to the weight
162	(dry basis) of the microcapsules.
163	The free oil (FO) content (non-encapsulated oil fraction) of microcapsules was determined according to Bae & Lee
164	(2008) with some modifications. Briefly, ethyl ether (7.5 mL) was added to 0.5 g powder and the mixture stirred in a
165	glass jar with a lid for 2 min at room temperature (20°C). The mixture was filtered through a Whatman filter paper
166	nº1 and the powder collected on the filter was rinsed three times with 10 mL of ethyl ether. Then, the solvent was
167	left to evaporate at room temperature until constant weight. The FO extracted was weighed and expressed as a
168	percentage of oil with respect to the weight (dry basis) of the microcapsules.
169	Encapsulation efficiency (EE) was determined by calculating the ratio of the total oil contained in the microcapsules
170	(TO) and the free oil (FO) located on its surface, according to Equation 4:

171 $EE(\%) = \frac{(TO - FO)}{TO} 100\%$ (Equation 4)

8

- 172 Where: EE is the encapsulation efficiency (%), TO is the total oil content of microcapsules (%) and FO is the free oil
- 173 content of microcapsules (%), determined as previously described.
- 174 All determinations were performed at least in duplicate.
- 175

176 **2.5.4.***Morphology*

- 177 The spray-dried microcapsules obtained were photographed with a digital camera (Kodak M853, USA)in order to
- 178 reveal their macroscopic aspects.
- Particle size and morphology were evaluated by scanning electronmicroscopy (SEM). Powders were mounted on aluminum stubs using a double-sided tape and were coated with a thin gold layer using a cool sputter system (SCD 005, BAL–TEC, Switzerland). SEM images were acquired with a scanning electron microscope (SEM 505, Philips, Netherlands) under high vacuum with a 20 kV acceleration voltage. Samples were observed with magnifications of 500x and 1000x. ImageJ (ImageJ, National Institutes of Health, USA) was used to determine microcapsules size.
- 184 The structure and morphology of the fish oil powders were observed using a confocal scanning laser microscope 185 (CSLM) (LEICA TCS SP5, Mannheim, Germany). Fluorescein and nile red were used as fluorescent probes to stain 186 protein and oil respectively. For labeling, a 5% w/v SPI solution was prepared and fluorescein, FITC, (10 mg/ml) 187 solution was slowly added into the protein solution while gently stirring. Staining of the oil was done by dissolving 188 Nile red in the oil at 0.2 mg/ml. Then, they were mixed to form the emulsion and obtain the micro-particles for spray 189 drying. The system was equipped with an Argon laser. Samples containing FITC and Nile red were excited at 488 nm 190 and detected sequentially at 500-550 (FITC green channel), to detect the protein phase, and 600-700 nm (Nile red 191 channel) to detect the oil phase. The powders were placed in a cover slip and observed with a 63x oil immersion
- 192 objective.
- 193

194 **2.5.5.** Oxidative stability of fish oil

195 Lipid oxidation was evaluated by determination of the peroxide value and Thiobarbituric acid assay (TBA) and by 196 analysis of the oxidative stability under accelerated conditions through a RANCIMAT test.

197 Peroxide value. The oil was extracted according to the method described by Partanen, Hakala, Sjövall, Kallio & 198 Forssell (2005). A sample of each powder (0.5 g) wasweighed into a test tube and suspended in 5mL of 199 distilledwater. The tubewas shaken until complete powder dissolution. A 300 µL portion was taken and vortexed 3 200 times for 10 s with 1.5 mL of an isooctane/isopropanol (3:1 v:v) mixture. The phases were separated and the upper 201 phase was taken for analysis. Fish oil (300 µL) was used as control. Peroxide value was determined 202 spectrophotometrically, according to Mancuso, McClements & Decker (1999) method. A portion of the extraction 203 medium (10–200 µL) was added to 2.8 mL of a methanol/butanol (2:1 v:v), followed by 15 µL of thiocynate solution 204 (3.94 mol/L) and 15 μ L ferrous iron (0.072 mol/L acidic solution). The sample was briefly vortexed, reacted in the 205 dark for 20 min, and the absorbance was measured at 510 nm with a Beckman DU650 spectrophotometer (Beckman, 206 Germany). Lipid hydroperoxide concentrations were determined using cumene hydroperoxide (Sigma-Aldrich Inc., St. 207 Louis, USA) standard curve. Measurements were done in duplicate.

208

Thiobarbituric acid assay (TBA). The number of 2-thiobarbituric acid (TBA) was determined according to the method proposed by Tironi, Tomás, & Añón (2007) with some modifications. A sample of powder (0.22 g) was homogenized with 1.78 mL of 5% w/v trichloroacetic acid (TCA, Cicarelli, Argentina), and after 30 min it was centrifuged at 10000 xg, 10 min, 20°C (HERMLE Z 326 K, Germany). Supernatant (0.5 mL) was mixed with 0.5 mL of 0.5% w/v TBA (Sigma-Aldrich, USA) aqueous solution in closed tubes. The mixture was incubated 30 min at 70°C with gently agitation, and then absorbance at 532 nm was determined using Beckman DU650 spectrophotometer (Fullerton, CA, USA).TBA values were expressed as mg of malondialdehyde/kg of oil according to Equation 5:

216 $TBA = \frac{AbsMVsVe\ 1000}{\varepsilon lm}$ (Equation 5)

217 Where: TBA is the TBA number (mg of malondialdehyde/kg of oil); Abs is the absorbance at 532 nm; M is the 218 malondialdehyde molar mass (72 g/mol); Vs is the sample volume (0.5 mL); Ve is the extract volume (1.78 mL); ε is 219 the molar extinction coefficient of the colored complex (1.56 x10⁵ M⁻¹); I is the optical path (1 cm); and m is the 220 sample mass (g).

221 Measurements were done in duplicate.

222

- 223 Oxidative stability analysis under accelerated conditions (RANCIMAT test). An accelerated oxidation test of the bulk
- fish oil and the microcapsules was performed in a Rancimat (Metrohm743, Switzerland) apparat using 1 g of fish oil
- or microcapsules at 90°C with continuous bubbling of an air stream at 20 L/h. Stability was expressed as induction
- time (IT). This assay was performed in duplicate for each sample.
- 227

228 **2.6 Statistical analysis**

- 229 Results were expressed as mean ± standard deviation and were analyzed by analysis of variance (ANOVA). Means
- 230 were tested with the Tukey's HSD (Honestly Significant Difference) test for paired comparison, with a significance
- 231 level α =0.05, using the Statgraphics Plus version 5.1 software (Statgraphics, USA).
- 232

3. Results and Discussion

234

235 **3.1.** Effect of protein:oil ratio and emulsifying process on emulsion characteristics

236 The protein: oil mass ratio and the emulsification techniques determined the initial characteristics and the stability of 237 the corresponding O/W emulsions. Figure 1 shows optical microscope images of the studied emulsions. It is worth 238 noting that, as in all cases a SPI dispersion 5% w/v was used as aqueous phase, the emulsions with a higher 239 protein: oil mass ratio have a lower amount of oil. Those processed only by Ultra-Turrax (UT) showed a lower number 240 of droplets but of higher size than those prepared by Ultra-Turrax and Ultrasound (UT+US), and seemed to have 241 different size distributions. This was confirmed by SLS analysis, shown in Figure 2 and Table 1. The emulsions 242 prepared by UT presented different behaviors according to their protein: oil mass ratio. Emulsions with lower protein 243 proportions (1:1 and 2:1) showed bimodal size distributions with two defined populations, a predominant one with 244 dp \approx 20 µm and another minority with dp \approx 0.2 µm; while those with higher protein proportions (3:1 and 4:1) 245 presented monomodal size distributions with dp \approx 28 μ m. Likewise, the 1:1 and 2:1 emulsions showed a greater 246 difference between De Brouckere (d_{4,3}) and Sauter (d_{3,2}) mean diameters (Table 1), evidencingthat they were

composed bymore heterogeneous droplets in size than the 3:1 and 4:1 emulsions. The specific surface areas(SSA) in these emulsions were minimal (Table 1). In these cases, the amount of protein seems to be enough to cover the new generated interface. This not occurred for lower protein:oil mass ratio (1:1 and 2:1 emulsions), in which the generated interfacial area increased about twenty times.

251 On the other hand, all emulsions prepared by UT+US presented bimodal particle size distributions with two defined 252 populations with dp \approx 0.25 µm and 2.5 µm respectively (Figure 2), regardless of the emulsions formulation. These 253 particle size distributions were considerably narrower than those of the emulsions prepared only by UT as had the 254 lowest difference between $d_{4,3}$ and $d_{3,2}$, indicating greater uniformity in the droplet sizes. More energy (as 255 mechanical work) was applied to the system when adding the US emulsification step, and a greater SSA than that 256 obtained for the corresponding emulsions prepared by UT was generated (Table 1). These results could be explained 257 taking into account differences between both emulsification mechanisms. Drops are formed by shear stress in 258 laminar flow and/or shear and inertial stress in turbulent flow when emulsifying by UT. Meanwhile acoustic 259 cavitation and power dissipation can break droplets during ultrasound emulsification and yield emulsions with 260 particles in the sub-micron range (Gavahian, Chen, Khaneghah, Barba, & Yang, 2018). In this sense, Jafari, He, & 261 Bhandari (2007a) also described that fish oil emulsions using mixtures of maltodextrin and whey proteins as 262 surfactant (4:1 wall/core ratio) obtained by UT+US showed lower particle diameters than those prepared only by UT. 263 The emulsions rheological behavior conditions their stability and further processing. Table 1 also summarizes the 264 rheological characteristics for fish oil-in-water emulsions prepared with different SPI protein:oil mass ratios 265 processed by UT and UT+US. The experimental values for the shear stress as a function of strain rate gradient were 266 satisfactorily adjusted to the Newton model (R>0.97). The emulsions prepared by UT almost doubled the viscosities 267 of those prepared by UT+US, regardless to the emulsion formulations. Tatar, Sumnu, & Sahin (2017) describe the 268 effect of several factors, including volume fraction, droplet size, and colloidal interactions on emulsions rheology. It 269 seems that emulsions containing smaller droplets (UT+US) have the ability to pack more efficiently than those with 270 larger droplets (UT), decreasing their viscosity. But no correlation between emulsion viscosity and volume fractions

were found in this work, possibly due to that the studied volume fraction correspond with dilute emulsions $(0.01 < \Phi < 0.05)$.

273 The emulsions stability, shown in Figure 3, was determined by comparing the percentages of initial backscattered 274 light (immediately after the emulsion was formed) and after two hours in order to ensure the necessary time to 275 process them by spray. The emulsions prepared by UT showed ≈50-55 % of BSo regardless of the formulation; while 276 in those processed by UT+US, the % BSo decreased from 70 to 50% when increasing protein:oil mass ratio. Thus those emulsions with highest oil proportions (1:1 and 2:1) and the smallest oil droplets size (prepared by UT+US) 277 278 showed the highest % BSo (> 60%), according to the dependency of BS with the oil droplet size and their 279 concentration. On the other hand, in the emulsions with lower oil concentration (3:1 and 4:1), the effect of droplet 280 size due to different processes was not observed in the % BSo.

281 After two hours, all the emulsions prepared by UT diminished their BS ≈10-20%, suggesting the occurrence of 282 creaming-flocculation mechanisms although no evidence of phase separation was observed. The migration of oil 283 droplets from the bottom to the top of the emulsion sample could lead to a progressive reduction of oil droplet 284 concentration at the bottom of the emulsion sample, and a concurrent decrease in the intensity of backscattered 285 light. But no evidence of phase separation was observed even on the top of the tube. On the other hand, the 286 emulsions prepared by UT+US remained stable after 2 h without significantly modifying their % BSo value. Taking 287 into account Stokes' law, differences in the emulsion stability could be attributed mainly to droplets sizes that in this 288 work would be determined by the emulsification processes (Wang, Liu, Chen, & Selomulya, 2016; Wang, Liu, Chen, & 289 Selomulya, 2016; Day, Xu, Hoobin, Burgar, & Augustin, 2007).

290

3.2. Characterization of fish oil-soybean protein microencapsulates

The emulsion characteristic and the encapsulating agent affect the properties of fish oil microparticles, such as the encapsulation efficiency, peroxide value, particle size, morphology and moisture content (Encina et al., 2016).

295 3.2.1. Chemical composition and encapsulation efficiency

All the studied emulsions could be spray dried. The drying conditions were set in preliminary tests, using an inlet air temperature of 180°C (Jafari, Assadpoor, Bhandari, & He, 2008) and outlet temperatures of 96±5°C. In all cases, light yellowish powders were obtained, which did not present an oily appearance at touch nor the characteristic odor of the fish oil. Table 2 shows their color parameters. Emulsifying process seemed not to influence the powder coloration as the formulation did. When increasing the protein proportion, encapsulates clarity increased (greater L*), and their yellowish coloration (lower b*) and total coloration change (Δ E*) decreased.

302 Table 3 shows the chemical composition of microencapsulates, recovered solid yield (SY) and encapsulation 303 efficiency (EE) of each process. Moisture content also seemed to be dependent only by formulation as, for both 304 emulsifying process, encapsulates prepared with 3:1 protein:oil mass ratio showed the highest MC value. The 305 protein:oil mass ratio resulting after drying remains similar to that of the initial formulation only for samples 306 emulsified by both UT+US. Those processed only by UT, showed higher protein:oil ratios (1.8:1; 2.8:1; 4:1 and 5.6:1) 307 than their corresponding emulsions (1:1; 2:1; 3:1 and 4:1 respectively), implying that during drying lipids were lost 308 to a greater extent than proteins. Probably due to the lower stability of emulsions formed by higher oil droplets. 309 These results were reflected in SY values. Emulsions prepared by UT+US presented the highest SY (>46%), regardless 310 of their protein: oil mass ratio while those processed only by UT showed a lower SY that increased with the 311 protein:oil mass ratio from \approx 23to \approx 43% (being this last value statistically similar to those treated by UT+US). In all 312 cases mass losses occurred by the product adhesion to the drying chamber walls and later to the cyclone's, 313 according to Sosnik & Seremeta (2015) who reported typical SY for the spray drying process from 20% to70% 314 depending on both process conditions and sample characteristics.

On the other hand, the encapsulation efficiency for all the studied formulations was maintained between 57% and 69% except for the 4:1 emulsion prepared by UT+US, which presented the highest encapsulation efficiency (EE≈ 90%). It is evident that the protein:oil mass ratio and the emulsifying process played a fundamental role, as the same formulations treated only by UT or lower protein:oil mass ratios processed by UT+US showed significantly lower EE. Indirectly, droplets size, emulsion viscosities and oil and protein concentration are responsible of these results. Thus, increasing protein concentration, lower free oil was present in the products. Wang et al. (2016), also observed

14

higher EE when increasing whey proteins concentration that attributed to the increased oil retention principally by reducing the time to forma semi-permeable crust at the droplet-air interface during spray drying, making it difficult for the oil to diffuse to the particle surface during drying. Jafari et al. (2008) also observed that increasing whey protein isolate content led to the increase of the emulsion viscosity, thus reducing the circulation movement inside the droplets during drying and resulting in higher oil retention. Although in this work the viscosity increase was not observed, the samples with highest protein concentrations emulsified by UT+US showed the highest encapsulation efficiency.

328

329 3.2.2. Morphology of the fish oil-soybean protein microencapsulates

330 Figure 4 shows SEM images of the spray-dried fish oil-soybean protein microcapsules. Their mean apparent 331 diameters -estimated from the images- were 15-20 µm for all samples. However, wide size distributions were 332 observed (from 5 to 40 µm). These size dispersions are typically found in spray dried particles (Carneiro, Tonon, 333 Grosso, & Hubinger, 2013). Protein: oil mass ratio and emulsions characteristics such as particle size distribution and 334 stability, seemed not to influence the microcapsules size, which was mainly determined by the spray-dryer nozzle 335 diameter used. Differences in emulsions viscosities observed in this work seemed not to affect particle size either, 336 even though it has been reported the increase in particle size due to the formation of larger droplets during 337 atomization when working with emulsions of higher viscosity (Drusch, Serfert, Scampicchio, Schmidt-Hansberg, & 338 Schwarz, 2007).

Particles showed a smooth spherical shape characterized by the presence of surface dents (indentations) (Figure 4). According to I Ré (1998), such dents/indentations are formed with slow processes of film formation during drying of the atomized droplets, being these surface depressions the consequence of droplets collapse during the early stages of drying process. In our study, the formation of these dents on the outer surfaces seemed to increase with protein:oil mass ratio, according to Fäldt & Bergenståhl (1996), who reported that this morphology is typical of oil encapsulates with high protein concentrations.

345 No evidence of cracks, fissures or holes was found by SEM observations (Figure 4), which is an advantage and 346 suggests that soybean proteins were efficient to encapsulate the fish oil. However, it was possible to find a few 347 broken microcapsules, as that prepared from 3:1 UT+US emulsion shown in Figure 4, that allowed to observe the 348 typical inner topography of the studied particles. Inside, the microcapsules were hollow and the fish oil droplets 349 were adhered to the surface or embedded in the wall materials matrix. The formation of central voids in spray-dried 350 particles was attributed to the microcapsule expansion (or "ballooning") which is caused by fast fixing of the particle 351 structure in the early stage of drying with subsequent steam formation in the interior of the particle and inflation of 352 the particle (Rosenberg, Talmon & Kopelman, 1988; Nijdam & Langrish, 2006; Jafari et al., 2008). Wang et al. (2016) 353 also observed hollow particles with irregular dents appearing on the surfaces when encapsulating DHA-containing 354 fish oil with whey protein isolate, and related the mechanisms for the formation of the central hollow structure to 355 the expansion of the particles during the later periods of the drying process, and the dents to shrinkage at the early 356 stages of the drying process (Botrel, de Barros Fernandes, Borges, & Yoshida, 2014).

Fish oil was dispersed within the wall of the microcapsule in the form of small droplets with, similar size ($\approx 1.4 \mu m$) than those dispersed in the parent-emulsion as observed in Table 1 and Figure 2. This may be attributed to both, the fast crust formation (or solidification) that prevents the coalescence of the dispersed droplets and to the good emulsion stability during atomization and subsequent drying (I Re, 1998). Jafari et al. (2008) reported that a fast crust formation could be associated with low levels of surface oil content as it was difficult for the fish oil droplets to come onto the surface of particles.

The location of each component in the microcapsules was tried to be elucidated y CLSM using specific fluorescent probes that differentially stained proteins and lipids (Figure 5). Soybean proteins were co-localized with the fish oil drops, suggesting that the resulting microcapsules should be matrix-type where the oil and the wall material were integrated (Raybaudi-Massilia & Mosqueda-Melgar, 2012; Bakry et al., 2016). Central voids into the particles also could be observed. These results agree with SEM observations and those reported by Wang et al. (2016) who described similar matrix-type microcapsules composed of fish oil and whey proteins.

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370 3.2.3. Oxidative stability of fish oil-soybean protein microencapsulates

371 The oxidation state of both, the original fish oil and the resulting powder encapsulates was analyzed. Lipid 372 autoxidation is a chemical alteration reaction that occurs by free radicals through chain reactions. Peroxides are the 373 primary products produced at the beginning of this alteration that then are degraded into other products, such as 374 alcohols, ketones, aldehydes and volatile compounds, responsible for undesirable odors in food (Barrow, Wang, 375 Adhikari, & Liu, 2013). These secondary oxidation compounds can be measured by thiobarbituric acid reactive 376 compounds (Jiménez-Martín et al., 2015; Shaw, McClements, & Decker, 2007) among other methods. Figure 6 shows 377 the peroxide index and, thiobarbituric acid value for the studied samples. Fish oil had a low peroxide content (PI = 1 378 meq /kg) and absence of self-oxidation byproducts, indicating that lipid autoxidation had not begun or was in its 379 early stages. This could probably be attributed to the presence of antioxidants in the commercial fish oil 380 sample. Emulsifying and spray drying processes as well as the formulation used for encapsulation affected the 381 oxidative stability of fish oil. Unexpectedly all encapsulating systems showed a higher peroxide index and TBA values 382 than those corresponding to free fish oil. Encina et al. (2016) mentioned that although manystudies have reported an 383 improvement in fish oil stability when it is microencapsulated, there are some works where a lower fish oil stability 384 from microparticles has been described when compared to bulk oil. Thus, Kolanowski & Laufenberg 2006 found that 385 the encapsulation of fish oil with methylcellulose did not significantly improve its oxidative stability with respect to 386 bulk fish oil, as evaluated by peroxide value measurements, despite high encapsulation efficiency (over 80%), and 387 attributed itto the higher surface area of the microparticles than bulk fish oil. Serfert, Drusch, & Schwarz, (2009) 388 reported that fish oil encapsulated with modified starch and glucose syrup added with different antioxidants showed 389 higher peroxide indexes thanthose of bulk oil.

Wang et al. (2016) also observed higher peroxide values of whey encapsulates than the oil blank in the initial storage stage that attributed to the oxidation of the particle surface/near surface oil duringpreparation when it was exposed to air; and mentioned previous researches that suggested that the auto-oxidation of encapsulated and nonencapsulated core oil likely occurred during the drying process if a wall material with strong film forming properties was used, which could catalyze further oxidation during storage (Drusch & Berg, 2008; Wang, Tian, & Chen, 2011).

And they explained that quick formed shell possibly increased the resistance of evaporation, resulting in the rapid increaseof particle temperature during drying. Thus, the period of particle free oil exposure in the high temperature was prolonged; resulting in peroxides increased, above than the unprocessed crude fish oil at the early stage of storage. Furthermore, other authors observed that particle ballooning during drying leads to air inclusion in the particle and oxidation reactions (Drusch et al., 2006; Keogh et al., 2001).

400 Encapsulates emulsified by UT presented a significantly higher peroxide index and TBA values than those processed 401 by UT+US, with the exception of those with a protein:oil mass ratio of 4:1 processed only by UT that showed a similar 402 PI than those processed by UT+US. But as this sample showed the highest TBA value, these PI value would 403 correspond to an advanced period of oxidation reaction, when unstable peroxides oxidized themselves to form other 404 compounds, such as aldehydes and ketones (Drusch et al., 2007). During UT emulsification a certain amount of air is 405 incorporated into the dispersion, and together with light it would facilitate the beginning of the oxidation reaction. 406 Then the US stage could remove part of the incorporated oxygen, delaying the autoxidation. Oxidation could also be 407 accelerated with the increase oftemperature during spray drying. But although the drying T was set at 180°C, the 408 effective temperature of the drops was lower (\cong 60°C) and the residence time in the equipment was minimal (\cong 1-2 409 s).

Furthermore all the formulations prepared by UT + US showed PI values lower than 10 meq / Kg oil that is the maximum PI allowed by the Argentine Food Code (CAA) for the commercialization of fish oil (www.anmat.gov.ar).

412 Also unexpectively, for both processing technologies PI and TBA indexes increased with the protein:oil mass ratio. 413 When reducing the proportion of fish oil in the encapsulates, TBARS values increased markedly (≈200% for UT vs. 414 \approx 300% for UT+US). It should be expected that the 4:1 sample processed by UT+US that showed significantly higher 415 encapsulation efficiency would show an improvement in the oxidative stability of fish oil. In this sense, Drusch & 416 Schwarz (2006) reported that the amount of surface oil, which probably represented a high proportion of the non-417 encapsulated oil was less significant on oil oxidation and shelf-life stability than the particle structure and shell 418 properties. Wang et al. (2016) observed that encapsulates with higher protein concentration showed a lower 419 oxidation stability before 20 days, indespite of higher encapsulation efficiency, and attributed it to the faster shell

formation process of the high protein content emulsions, that possibly increased the resistance of evaporation, resulting in the increase of particle temperatureduring drying and to the fact that the lower protein contentin the high oil samples somehowavoided the free oil being exposed in high temperature for such long period; producing higher initial oxidation rates as the protein:oil mass ratio increased.

424 Furthermore soy protein isolates contains low amounts of divalent cations, such as copper and iron 425 (http://www.guia-nutricion.com), which could catalyze the autoxidation of unsaturated fatty acids in fish oil. 426 Working with other biopolymers, other authors tried to improve the stability of the encapsulated oil by incorporation 427 of chelating agents like citric acid (Drusch & Berg, 2008).

428 In order to study the oxidative stability of encapsulates during storage, the Induction Time (IT) obtained from 429 Rancimat accelerated oxidation test was determined and showed in Figure 7. The accelerated Rancimat test has 430 gained acceptance as an indirect measure of oil stability, as the oily sample is treated under controlled conditions in 431 which the lipoperoxidative process reaches its final steps and lipids are oxidized to short-chain volatile acids which 432 are collected in distilled water increasing its conductivity. Finally, the sample turns out to be more stable as the 433 time required to increase the conductivity increases. The induction time (IT) for control fish oil was 3.9 h. All 434 encapsulated samples processed by UT were more susceptible to oxidation than those processed by UT+US, since 435 they had the shortest induction times. For both emulsification techniques, formulations 1: 1 and 4:1 presented the 436 longest induction times; being only the one prepared by UT+US similar to that of non-encapsulated fish oil. It seemed 437 that protein:oil mass ratio 1:1 samples prepared by UT+US manage to protect the fish oil during its 438 microencapsulation (by the initial values of peroxides and TBA) and also maintain its oxidative stability; while the 4:1 439 samples prepared by UT+US, which showed the highest EE, also maintain their oxidative stability, despite presenting 440 the highest values of PI and TBARS for the samples processed by UT+US.

441

442 **4.** Conclusions

443 Soy proteins managed to encapsulate the fish oil, masking its characteristic odor and its oily texture. The 444 emulsification process was determinant in the efficiency of encapsulation as well as in the protection exerted on the

445 oil oxidative stability. Although emulsifying and drying processes caused certain initial oil oxidation (verified by

446 peroxide and TBA indexes), some of the studied systems showed a good perspective of oxidative stability over time.

447 Microparticles prepared with a protein: oil ratio of 4: 1, emulsified by UT + US to oildrop sizes smaller than 2.5 μm

448 and good stability showed encapsulation efficiencies of 88% and managed to maintain the oil oxidative stability, as

449 presented similar induction times (measured by rancimat test) than free oil. This microparticles should be use to

450 vehiculate healthy fish oil, rich in omega 3 fatty acids, into functional foods.

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Figure 1. Optical microscope images (100X) of the fish oil-in-water emulsions with different protein:oil mass ratios (1:1, 2:1, 3:1, and 4:1 w/w) and processed by Ultraturrax (UT) and Ultraturrax+Ultrasound (UT+US).



Figure 2. Profiles of particle size distributions of the fish oil-in-water emulsions prepared with different protein:oil mass ratios: 1:1 (----), 2:1 (...), 3:1 (----), and 4:1 (____) w/w) and processed by Ultraturrax (UT) (_____) and Ultraturrax+Ultrasound (UT+US) (_____). Distributions were expressed in percentage of oil volume.



Figure 3. Destabilization kinetics (clarification, zone 10–15 mm of test tube), corresponding to fish oil-in-water emulsions prepared with different protein:oil mass ratios (1:1, 2:1, 3:1, and 4:1 w/w) prepared by Ultraturrax (UT) and Ultraturrax+Ultrasound (UT+US). Figure shows the initial Backscattering (and) and its value after 2 h of storage at room temperature (and), corresponding to the maximum time for spray drying of emulsions.



Figure 4. A) Scanning electron micrographs (SEM) of the outer morphology (topography) of the fish oil microcapsules obtained after spray-drying of fish oil in water emulsions prepared with different protein:oil mass ratios (1:1, 2:1, 3:1, and 4:1 w/w) and processed by Ultraturrax (UT) and Ultraturrax+Ultrasound (UT+US). SEM at 500x magnification. **B)** Typical inner morphology (topography) of the fish oil microcapsules obtained after spray-drying of fish oil in water emulsions prepared with protein:oil mass ratios of 3:1 w/w and processed by Ultraturrax+Ultrasound (UT+US). SEM at 1000x magnification.



Figure 5. Confocal laser scanning micrograph (CLSM) of fish oil microcapsules obtained after spray-drying of fish oil in water emulsions prepared with protein:oil mass ratio of 4:1 w/w and processed by Ultraturrax+Ultrasound. CLSM at 63x magnification. Double staining of O/W emulsion with: (A) Green colour represents the soybean protein stained by Fluorescein. (B) Red colour represents the fish oil stained by Red

Nile. (C) Represent the colocalization of both colorants.



Figure 6. Peroxide value (A) and TBA number (B) of the fish oil-soybean proteins encapsulates prepared from spray dried O/W emulsions with different protein:oil mass ratios (1:1, 2:1, 3:1, and 4:1 w/w) and processed by Ultraturrax (UT) () and Ultraturrax+Ultrasound (UT+US) (). Peroxide value of the fish oil: 1,067±0,009 PV/Kg oil.



Figure 7. Induction time of the fish oil encapsulates in soybean protein matrices prepared from spray dried O/W emulsions with different oil:protein mass ratios (1:1, 2:1, 3:1, and 4:1 p/p) and processed by Ultraturrax (UT) (\square) and Ultraturrax+Ultrasound (UT+US) (\square). Induction time of the fish oil: 3,91 ± 0,25 h.

Highlights

 Soy proteins managed to encapsulate fish oil masking its characteristic odor and oily texture.

Or: Soy proteins managed to encapsulate fish oil.

- These microparticles would facilitate fish oil incorporation into healthy food products.
- The effect of emulsifying process and protein : oil ratio on capsules properties and oil stability were studied or Two emulsification procedures and several protein-to-oil ratios were analyzed.
- Some systems showed a good perspective of oil oxidative stability over time.



 Table 1. Initial parameters of the fish oil-in-water emulsions prepared with different protein:oil mass ratios (1:1, 2:1, 3:1, and 4:1 w/w) and processed by Ultraturrax (UT) and Ultraturrax+Ultrasound (UT+US).

Emulsifying process	Protein:oil mass ratio	<mark>d</mark> 4, 3 (μm)	<mark>d</mark> 3, 2 (μm)	Difference (d _{4, 3} - d _{3, 2})	Specific surface area (µm ⁻¹)	η (mPa.s)
	1:1	$26.44\pm0.86^{\text{c}}$	$3.21 \pm 0.21^{\circ}$	23.23	0.093 ± 0.006^{b}	$7\text{.}20\pm0\text{.}40^{\text{b}}$
UT	2:1	$22.54\pm0.51^{\text{b}}$	1.62 ± 0.13^{b}	20.92	$0.093\pm0.008^{\text{b}}$	5.80 ± 1.50^{b}
	3:1	$32.45\pm0.85^{\text{e}}$	18.22 ± 0.27^{e}	14.23	$0.005\pm0.001^{\text{a}}$	$6\textbf{.}00\pm0\textbf{.}50^{b}$
	4:1	$28.64 \pm 1.09^{\text{d}}$	17.04 ± 0.58^{d}	11.60	$0.004\pm0.001^{\text{a}}$	7.60 ± 0.60^{b}
	1:1	$1.56\pm0.01^{\text{a}}$	0.47 ± 0.01^{a}	1.09	$0.633\pm0.001^{\mathrm{f}}$	3.60 ± 0.50^{a}
UT+US	2:1	$1.14\pm0.01^{\text{a}}$	$0.38\pm0.01^{\text{a}}$	0.76	$0.399\pm0.001^{\text{e}}$	2.60 ± 0.30^{a}
	3:1	$1.42\pm0.07^{\text{a}}$	0.35 ± 0.01^{a}	1.07	$0.282\pm0.005^{\text{d}}$	2.80 ± 0.10^{a}
	4:1	$1.03\pm0.02^{\text{a}}$	$0.32\pm0.01^{\text{a}}$	0.71	$0.232 \pm 0.002^{\circ}$	3.40 ± 0.20^{a}

Reported values for each emulsion are means \pm standard deviation (*n*=4). Different letters in the same column indicate significant differences between samples (p<0.05),

according to Tukey's test.

Table 2. CIE-Lab color parameters (L^* , a^* and b^*), total color difference (ΔE^*) of the fish oil microcapsules obtained after spray-drying of fish oil in water emulsions prepared with different protein:oil mass ratios (1:1, 2:1, 3:1, and 4:1 w/w) and processed by Ultraturrax (UT) and Ultraturrax+Ultrasound (UT+US).

Emulsification technique	Protein:oil ratio	ΔE^*	L^*	a*	<i>b</i> *	
	1:1	$10.46 \pm 1.21^{\circ}$	92.81 ± 1.22^{a}	$-0.46 \pm 0.13^{\circ}$	$11.10 \pm 0.86^{c,d,e}$	
UT -	2:1	$9.94 \pm 1.81^{b,c}$	92.90 ± 1.72^{a}	$-0.58 \pm 0.12^{b,c}$	$10.54 \pm 1.17^{b,c,d}$	
	3:1	$9.49 \pm 1.63^{b,c}$	93.35 ± 1.71 ^{a,b}	$-0.43 \pm 0.18^{\circ}$	$10.25 \pm 1.04^{b,c}$	
-	4:1	7.38 ± 0.56^{a}	$94.95 \pm 0.62^{b,c}$	$\textbf{-0.69} \pm \textbf{0.03}^{a,b}$	8.64 ± 0.48^{a}	
	1:1	$10.78 \pm 0.65^{\circ}$	92.77 ± 1.06^{a}	$\textbf{-0.69} \pm 0.08^{a,b}$	$11_{\bullet}39\pm0_{\bullet}80^{\text{d,e}}$	
- UT+US	2:1	$8.80 \pm 0.56^{a,b}$	$93.71 \pm 0.49^{a,b,c}$	$\textbf{-0.83} \pm 0.06^{a}$	$9\textbf{.}67\pm0\textbf{.}62^{a,b}$	
01105 -	3:1	$10.79 \pm 0.51^{\circ}$	$94.22 \pm 0.57^{a,b,c}$	$\textbf{-0.63} \pm \textbf{0.08}^{b}$	12.01 ± 0.43^{e}	
	4:1	$8.50 \pm 0.33^{a,b}$	$95.31 \pm 0.38^{\circ}$	-0.82 ± 0.05^{a}	9.91 ± 0.34^{b}	

Reported values for each encapsulate are means \pm standard deviation (*n*=9). Different letters in the same column indicate significant differences between samples (p<0.05). according to Tukey's test.

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Table 3. Moisture (MC), protein (PC), total oil (TO) and free oil (FO) contents, recovered solid yield (SY) and encapsulation efficiency (EE) of the fish oil microcapsules obtained after spray-drying of fish oil in water emulsions prepared with different protein:oil mass ratios (1:1, 2:1, 3:1, and 4:1 w/w) and processed by Ultraturrax (UT) and Ultraturrax+Ultrasound (UT+US).

Emulsifying process	Protein:oil mass ratio	MC (%)	Protein (%)	Total Oil (%)	Free Oil (%)	SY(%)	EE(%)
	1:1	$5.10 \pm 1.21^{b,c}$	$52.36 \pm 1.12^{b,c}$	$27.82 \pm 2.43^{\circ}$	$11.57 \pm 1.79^{\circ}$	$23.24\pm3.65^{\text{a}}$	57.82 ± 6.27^{a}
UT	2:1	$2.32\pm0.01^{\text{a,b}}$	$62.95\pm0.09^{\text{d}}$	$21.84 \pm 2.39^{b,c}$	$6.65\pm0.95^{\text{c}}$	$31.04\pm3.57^{\text{a,b}}$	$69.20\pm5.50^{\text{a,b}}$
	3:1	$8.29 \pm 1.21^{\text{d}}$	$64.27\pm0.94^{\text{d,e}}$	15.69 ± 0.67^{a}	$4.86\pm0.80^{\text{b}}$	$29.15 \pm 5.31^{a,b}$	$69.10 \pm 5.56^{a,b}$
	4:1	$3.88\pm0.55^{\text{a,b}}$	68.24 ± 2.35^{e}	12.14 ± 1.94^{a}	4.35 ± 1.82^{b}	$42.60 \pm 4.22^{b,c}$	$65.19\pm11.04^{\text{a}}$
	1:1	$3.92\pm0.08^{\text{a,b}}$	38.78 ± 0.39^{a}	$48.77 \pm 1.20^{\text{d}}$	$16.06 \pm 2.46^{\circ}$	$50.22 \pm 4.90^{\circ}$	$66.93 \pm 4.55^{a,b}$
UT+US	2:1	1.62 ± 0.49^{a}	49.63 ± 1.34^{b}	$28.94 \pm 1.49^{\circ}$	$12.23 \pm 1.48^{\circ}$	$50.26 \pm 2.22^{\circ}$	57.73 ± 1.83^{a}
01.00	3:1	$9.23\pm0.25^{\text{d}}$	$56.10 \pm 0.39^{\circ}$	$20.16\pm0.85^{\text{a,b}}$	$6.06\pm0.71^{\text{b}}$	$47.21\pm0.78^{\text{b,c}}$	$69.82\pm4.89^{\text{a,b}}$
	4:1	$6.80\pm0.79^{\text{c,d}}$	60.64 ± 0.23^{d}	15.21 ± 1.49^{a}	$1.26\pm0.42^{\text{a}}$	$46.04\pm0.38^{\text{b,c}}$	88.74 ± 3.15^{b}

Reported values for each encapsulate are means \pm standard deviation (*n*=2). Different letters in the same column indicate significant differences between samples (p<0.05),

according to Tukey's test.