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# Tuning catalytic acidity in Al<sub>2</sub>O<sub>3</sub> nanofibers with mordenite nanocrystals for dehydration reactions

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21 **Abstract**View Article Online  
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22 Alumina ( $\text{Al}_2\text{O}_3$ ) is one of the most used supports in the chemical industry due to its exceptional  
23 thermal stability, surface area, and acidic properties. Mesoscopic structured alumina with  
24 adequate acidic properties is important in catalysis to enhance selectivity and conversion of  
25 certain reactions and processes. This study introduces a synthetic method based on  
26 electrospinning to produce  $\text{Al}_2\text{O}_3$  nanofibers (ANFs) with zeolite mordenite (MOR)  
27 nanocrystals (hereafter, hybrid ANFs) to tune the textural and surface acidity properties. The  
28 hybrid ANFs with electrospinning form a non-woven network with macropores. ANF-HMOR,  
29 i.e., ANFs containing protonated mordenite (HMOR), shows the highest total acidity of ca. 276  
30  $\mu\text{mol/g}$  as determined with infrared spectroscopy using pyridine as a molecular probe (IR-Py).  
31 IR-Py results reveal that Lewis acid sites are prominently present in the hybrid ANFs. Brønsted  
32 acid sites are also observed in the hybrid ANFs and are associated with HMOR presence. The  
33 hybrid ANFs functionality is evaluated during the methanol dehydration to dimethyl ether  
34 (DME). The proof of concept reaction reveals that ANF-HMOR is the more active and selective  
35 catalyst with 87% conversion and nearly 100% selectivity to DME at 573 K. The results  
36 demonstrate that the textural properties and the acid site type and content can be modulated in  
37 hybrid ANF structures, end-synergistically improving selectivity and conversion during the  
38 methanol dehydration reaction. From a broader perspective, our results promote the utilization  
39 of hybrid structural materials as a means to tune chemical reactions selectively.

40 **Keywords:** electrospinning,  $\text{Al}_2\text{O}_3$ , nanofibers, mordenite, acidity, methanol dehydration,  
41 DME



## 42 Introduction

43  $\text{Al}_2\text{O}_3$  in heterogeneous catalysis has been used to support alkali metals, noble metals, and metal  
44 oxides with a wide range of applications in biomass upgrading, oil industry, and automotive  
45 sector.<sup>1–8</sup> Such a wide range of applications is due to the various  $\text{Al}_2\text{O}_3$  polymorphs,<sup>9,10</sup> each  
46 with unique properties, such as thermal stability, acidity, and high specific surface area, targeted  
47 for specific reactions.<sup>11–16</sup> Besides the current synthetic approaches in  $\text{Al}_2\text{O}_3$ ,<sup>16–24</sup> structuring of  
48 mesoscopic scale  $\text{Al}_2\text{O}_3$  remains a challenge. Typical methods to structure  $\text{Al}_2\text{O}_3$  are extrusion<sup>8</sup>,  
49 injection molding,<sup>25</sup> and 3D printing.<sup>25,26</sup> These methods search to improve reaction rates via  
50 mass transfer and diffusivity varying the  $\text{Al}_2\text{O}_3$  geometries. Although such  $\text{Al}_2\text{O}_3$  structures are  
51 often relevant in catalysis, sufficient attention should be paid to the chemical properties of  
52  $\text{Al}_2\text{O}_3$ , such as the nature of the acid sites to promote acidity in structural acid catalysts.

53 Electrospinning is a convenient method that provides sufficient versatility to optimize chemical  
54 properties in structured materials.<sup>27–36</sup> The method produces nanofiber-like structures formed  
55 during the withdrawal of a jet from a droplet subjected to an external electric field, which later  
56 is deposited over a collector plate for further treatment.<sup>37–39</sup> Although the approach has been  
57 primarily used in the biomedical field,<sup>40</sup> it is increasingly used for energy storage, energy  
58 conversion, and catalysis.<sup>41,42,43</sup> In the past, ceramic materials, including alumina, have been  
59 subject to modifications that have led them to have one-dimensional (1-D) configurations, such  
60 as nanofibers.<sup>44</sup> These arrangements have attracted attention due to the unique functionality  
61 provided by nanofibers. For example, high mechanical strength, high surface-area/weight ratio,  
62 chemical composition, and stability.<sup>44,45,46</sup> Recently, M.A. Rodriguez-Olguin et al.<sup>43</sup>  
63 demonstrated that acid site content can be enhanced in ANFs. The authors use various  
64 aluminum precursors during electrospinning. From the precursor assessment, Aluminum  
65 Di(sec-butoxide)acetoacetic Ester Chelate (ASB) is identified as the ideal precursor to  
66 obtaining ANFs with a large amount of weak and medium strength Lewis acid sites (LAS).



67 Furthermore, ASB chelate promotes mesopores of 2-50 nm in size.<sup>47-51</sup> Macropores (i.e. >50  
68 nm), especially relevant in catalysts, can also be observed between the fiber-to-fiber  
69 interspaces.<sup>43</sup> From this perspective, it is fair to say that the benefit of nanofibers relies on its  
70 hierarchy having multiple levels of porosity that combine meso-/macro-pores.

71 Similarly, multilevel porosity can be found in hierarchical catalysts, such as zeolites. Zeolite  
72 has pore sizes ranging from micropores to mesopores and macropores.<sup>52,53,54</sup> These pores are  
73 composed of Si and Al atoms coordinated with oxygen, forming channel networks of diverse  
74 sizes. However, if the zeolite pores are too small, the reaction might be diffusion or mass  
75 transport limited. Synthetic methods to increase the meso-/macropores availability have been  
76 established to reduce transport issues. A widely applied approach in zeolites is leaching.<sup>55</sup>  
77 However, leaching involves several synthetic steps that are composition and zeolite type  
78 dependent. An interesting alternative is providing structure to existing catalysts, such as  
79 zeolites. Zeolites are compatible with synthetic approaches, such as electrospinning.<sup>56-62</sup> A key  
80 aspect of electrospinning is that it can facilitate the formation of macropores without limiting  
81 mesopore formation.<sup>43</sup>

82 Reports have demonstrated advantages for shaped zeolites as either single or hollow  
83 nanofiber.<sup>56,57</sup> This includes crystalline fibers of zeolite Y,<sup>58,59</sup> ZSM-5,<sup>60,61</sup> and SUZ-4.<sup>62</sup> Other  
84 approaches used to structure zeolites involve templates or zeolite mixtures with more materials  
85 to create composites. For example, F. Ocampo et al.<sup>63</sup> developed a multimodal pore size  
86 distribution using a zeolite and a glass monolith. The authors demonstrate the HZSM-5/glass  
87 monolith functionality during n-hexane cracking. Following a similar concept, zeolite Y, MFI,  
88 or Beta on  $\alpha$ -SiC foams, carbon nanotubes, or TiO<sub>2</sub> nanofibers have been synthesized and tested  
89 during a catalytic reaction.<sup>64,65,66</sup> From the previous examples, MOR shaped as nanofibers or  
90 MOR composites within a nanofiber are limited but increasingly recognized as an effective way



91 to enhance conversion and selectivity in chemical reactions, such as CO<sub>2</sub> methanation using a  
92 silica MOR composite.<sup>67</sup>

93 The rationale behind using MOR in structured materials as composite is to find more  
94 dimensionally refined systems that allow easy access to molecules to adsorb, react and desorb  
95 over LAS and Brønsted acid sites (BAS).<sup>68</sup> This is the case for acid catalysts, widely used for  
96 alcohol dehydration reactions, such as methanol dehydration to DME.<sup>69,70</sup> An accepted  
97 mechanism for the mentioned reaction occurs with the adsorption of the alcohols over a LAS  
98 or BAS, and an adjacent LAS forming two species, which produce DME and water upon  
99 condensation.<sup>71</sup> However, in this reaction, a tradeoff between the LAS and BAS strength has to  
100 be found because it can significantly alter methanol dehydration products.<sup>72</sup> It is generally  
101 accepted that the DME synthesis preferably proceeds on a solid acid catalyst with weak and  
102 moderate acidic sites. For strong BAS commonly found in MOR,<sup>73,74</sup> a considerable amount of  
103 side-products can be formed. The products consist predominantly of hydrocarbons or coke,  
104 which affect the selectivity and lifespan of the catalyst. An alternative that can compensate for  
105 high BAS contents is a composite, for example, MOR with Al<sub>2</sub>O<sub>3</sub> shaped as nanofiber.<sup>75</sup>  
106 Al<sub>2</sub>O<sub>3</sub><sup>76–81</sup> is a known catalyst used to dehydrate methanol and produce DME by following a  
107 proposed mechanism based purely on LAS.<sup>82,83</sup> From this perspective, a synergy between acid  
108 catalysts containing LAS and BAS has to be found to tune chemical reactions like DME  
109 selectively.

110 The present work synthesized nanofibers composed of amorphous Al<sub>2</sub>O<sub>3</sub> and MOR with  
111 electrospinning. The synergy of MOR and amorphous Al<sub>2</sub>O<sub>3</sub> is demonstrated by comparing the  
112 hybrid ANFs with Al<sub>2</sub>O<sub>3</sub> shaped as nanofiber. The added value of the structured fibers is  
113 assessed by comparing hybrid ANFs against Al<sub>2</sub>O<sub>3</sub> and MOR without nanofiber shape.  
114 Structural and morphological analysis indicates the presence of MOR in the ANFs. Textural  
115 analysis corroborates our findings, where a decrease in the surface area for hybrid fibers is



116 observed. Furthermore, hybrid ANFs show the highest acidity as determined with IR-Py. The  
117 acid sites present in the hybrid ANFs are LAS and BAS, while for the control samples of Al<sub>2</sub>O<sub>3</sub>,  
118 only LAS has been found. The hybrid ANFs functionality is assessed during methanol  
119 dehydration to DME as a proof of concept reaction. The results reveal a synergetic effect  
120 between Al<sub>2</sub>O<sub>3</sub> and MOR in the nanofibers and demonstrate the added value of hybrid materials  
121 in chemical reactions.

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## 123 **Methodology**

### 124 **Microwave-assisted zeolite synthesis**

125 Microwave-assisted hydrothermal synthesis was carried out to produce NaMOR nanocrystals.  
126 Colloidal silica (Ludox HS-40, 40% w/w, Aldrich), Al(OH)<sub>3</sub> (98%, Aldrich), and NaOH (98%,  
127 Sigma-Aldrich) were used as precursors to obtain an initial gel with the ratio 6 NaOH: Al<sub>2</sub>O<sub>3</sub>:30  
128 SiO<sub>2</sub>: 780 H<sub>2</sub>O. In a typical run, 1.6 g of Al(OH)<sub>3</sub> were dissolved in 2.2 g of NaOH (98%,  
129 Sigma-Aldrich) and 61 g of deionized water. Then, 11.4 g of colloidal silica were added until  
130 complete dissolution, and 3g of MOR nanocrystals from Zeolyst were used as seeds to enhance  
131 the crystallization rate. The resulting suspension was stirred for 1 h at 450 rpm. After, the  
132 obtained gel was placed in a Teflon autoclave belonging to the Milestone Flexiwave  
133 microwave. The crystallization conditions followed a ramp of 20 K/min to reach 453 K and  
134 used 600 W as maximum power for the synthesis time (1 h). This strategy allows the reduction  
135 of the synthesis time that has traditionally been reported from 24-48 h. Finally, the material was  
136 recovered by filtration, washed to a pH lower than 9, and dried at 343 K for 24 h in air. The  
137 final Si/Al ratio as determined with EDX is 10.5 for all NaMOR, which are then used during  
138 the ionic exchange (see below).

### 139 **Protonation of zeolite mordenite**

140 The protonation of the NaMOR nanocrystals follows a post-treatment using 1 M NH<sub>4</sub>NO<sub>3</sub> (ACS  
141 grade, Sigma Aldrich) solution in deionized water. First, NaMOR nanocrystals were dispersed  
142 in the NH<sub>4</sub>NO<sub>3</sub> solution, 1 g of solid per 10 ml of solution, and stirred at 353 K for 2 h. Then,  
143 the material was washed and filtered once the time had elapsed. The product obtained was  
144 placed in the oven for 12 h, and once the time finished, the ion exchange was repeated 3 times.  
145 At the end of the ion exchanges, the samples were calcined at 773 K for 3 h in air. The material  
146 obtained was labeled as HMOR.





## 147 **Hybrid fibers synthesis**

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148 The hybrid ANFs containing either NaMOR or HMOR were prepared by electrospinning using  
149 a commercial electrospinning system from IME Technologies (The Netherlands). The IME  
150 system was operated utilizing a stainless-steel needle of 0.4 mm inner diameter at a separation  
151 distance of 12 cm from the aluminum collector plate. First, a mixture consisting of 4 %p/v  
152  $C_{14}H_{27}AlO_5$  (ASB) technical grade from Alpha Aesar, 6 %p/v polyvinylpyrrolidone (PVP, MW  
153  $\sim 1,300,000$ ), and 0.26 %p/v *t*-octylphenoxypolyethoxyethanol (Triton x100, Sigma-Aldrich)  
154 dissolved in ethanol (100% Tech. grade, BOOM B.V., The Netherlands) was used as the  
155 aluminum precursor solution to generate ANFs. To make the hybrid ANFs, the synthesized  
156 NaMOR, or HMOR nanocrystals, were incorporated into the ASB solution, reaching a final  
157 concentration of 0.33 %p/v in each case. The prepared solutions were electrospun at  
158 environmental temperature and humidity using a potential of 18 kV and at an 8 mL/h infusion  
159 rate. After fiber deposition, all-fiber samples were dried in an oven at 353 K for 12 h to remove  
160 the excess solvent. Subsequently, they were calcined (Nabertherm LH 15/12) in air with a  
161 temperature ramp of 0.5 K/min to 623 K for 3 h and then 1 K/min until reaching 773 K for 4 h  
162 to ensure the production of amorphous alumina.<sup>43</sup> Hereafter, the obtained hybrid ANFs are  
163 named ANF-NaMOR and ANF-HMOR for simplicity. It should be noted that commercial  
164 MOR (CBV 10A, Zeolyst) was also used following the previously described hybrid nanofiber  
165 preparation. Control samples of particulate alumina ( $Al_2O_3$ -NP) and particulate alumina  
166 containing HMOR ( $Al_2O_3$ -HMOR-NP) were prepared by drop-casting using the same ASB,  
167 NaMOR, HMOR precursor solutions in crucibles. These samples were annealed following the  
168 same procedure as ANF-NaMOR and ANF-HMOR samples.

## 169 **Characterization**

### 170 **Morphological characterization**



171 High-resolution (HR)-SEM images of samples were taken using a Zeiss MERLIN SEM Article Online  
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172 microscope operated at 1.40 kV coupled with High-Efficiency Secondary Electron Detector  
173 (HE-SE2). SEM-scanning transmission electron microscope (STEM) was recorded at 20kV.  
174 Prior to STEM analysis, samples were sonicated in ethanol, which led to the fragmentation of  
175 the fibers into smaller fiber pieces.

### 176 **Structural characterization**

177 The crystalline structure of NaMOR and HMOR nanocrystals was analyzed by a Siemens  
178 (D5000, E04-0012 series) diffractometer, using CuK $\alpha$  radiation ( $\lambda = 1.5418 \text{ \AA}$ ) operated at 35  
179 kV, 25 mA, in the  $2\theta$  range between 5-50°, employing a step size of 0.02°/min and step time of  
180 4 s. The hybrid fibers were analyzed by X-ray powder diffraction (D2 PHASER, Bruker) using  
181 Cu K $\alpha$  radiation ( $\lambda = 1.5418 \text{ \AA}$ ) operated at 30 kV, 10mA, in the  $2\theta$  range between 7-45°,  
182 employing a step size of 0.05° and a scan speed of 0.1°/s. A Si low background sample holder  
183 (Bruker) was used for the hybrid samples.

### 184 **Chemical characterization**

185 X-ray photoelectron spectroscopy (XPS) general survey analysis was performed in a Quantera  
186 SXM machine from Physical Electronics using monochromated Al K $\alpha$  (1486.6 eV). All  
187 samples were fixed in a stainless-steel holder. Low energy electron flood gun was used to  
188 supply the missing photo- and Auger electrons. The electron binding energies were referenced  
189 to aliphatic carbon C 1s at 284.8 eV. The obtained peak analysis was made using the PHI  
190 Multipak V9.9.0.8 software (Physical Electronics, Inc.).

### 191 **Textural analysis**

192 BET surface area, pore-volume, and pore diameter of the samples were determined from the  
193 nitrogen adsorption/desorption isotherms at 77K on a Micrometrics ASAP 2010 instrument.



194 Before the measurement, each sample was evacuated at 473K for 4 h. The pore size distributions  
195 were calculated from the desorption branch of the isotherm using the Barrett-Joyner-Halenda  
196 (BJH) model.<sup>54</sup>

### 197 **NH<sub>3</sub>-TPD**

198 To determine the total acidity properties of the samples, NH<sub>3</sub>-TPD analysis was performed  
199 using a Micromeritics Autochem II 2910 instrument. Prior to NH<sub>3</sub> adsorption, 150 mg of the  
200 sample was loaded into a U-shaped quartz reactor and heated from RT to 673 K with 10 K/min  
201 in a flow of He (50 ml/min), held for 30 min at 673 K (to remove any adsorbed species on the  
202 surface). After that, the reactor was cooled to 373K. The sample was saturated with 1% NH<sub>3</sub> in  
203 He (50 ml/min) for 120 min at 373 K, followed by helium flushing (50 ml/min) for 60 min at  
204 373 K to remove physisorbed NH<sub>3</sub>. The sample was then heated to 1073 K at a rate of 10 K/min  
205 in He flowed (50 mL/min) and held at 1073K for 30 min for NH<sub>3</sub> desorption. The effluent gasses  
206 were analyzed with a Quadrupole mass spectrometer (Balzers Omnistar) using  $m/z = 15$ .

### 207 **IR measurements and Pyridine adsorption**

208 The nature and strength of acid sites were determined through pyridine (Py) adsorption over  
209 the materials and subsequent temperature-programmed desorption (TPD-Py). The samples  
210 were analyzed with IR spectroscopy through in situ transmission on self-supported wafers (10-  
211 15 mg, 13 mm of diameter) pressed at 5 t cm<sup>-2</sup> (490 MPa). The wafers were placed in a Pyrex  
212 IR cell fitted with water-cooled NaCl windows. More details of the experimental setup can be  
213 found elsewhere.<sup>84</sup> Before the adsorption experiments, each sample was pretreated in situ at  
214 723K (10 K/min) for 30 min under N<sub>2</sub> flow (50 sccm), then cooled down to 303K, and the  
215 reference IR spectra of the “clean wafer” were taken. The samples were exposed to a flow of  
216 N<sub>2</sub> containing evaporated Py. The physisorbed Py was further removed under flowing N<sub>2</sub> until  
217 the spectra of the adsorbed Py remained stable (about 60 min). The thermal desorption of Py



218 was measured from 303K to 723K with 5 K/min in a flow of N<sub>2</sub> (50 ml/min). The spectra were  
219 acquired with a Nicolet Magna 550 FTIR spectrometer with a cryogenic MCT detector (4 cm<sup>-1</sup>  
220 resolution, 25 scans). The gas used in this study was high purity grade N<sub>2</sub> (INDURA UHP  
221 99.999%) and was further purified through a molecular sieve (3 Å), and MnO/Al<sub>2</sub>O<sub>3</sub> traps to  
222 remove water and oxygen impurities, respectively.

### 223 **Catalytic test**

224 The synthesized materials were tested for the dehydration of methanol to dimethyl ether (DME)  
225 between 423 and 723 K (heating ramp of 1K/min) in a fixed bed glass tubular microreactor (i.d.  
226 = 5.3 mm). The reactor was loaded with 50 mg of catalyst diluted (1:5) with milled quartz (200  
227 mesh). The methanol concentration was 7% v/v in Ar obtained from a gas saturator filled with  
228 pure methanol immersed into a thermostatic bath. The total flow rate was set to 20 mL/min,  
229 giving a weight hourly space velocity (WHSV) of 2.3 g<sub>methanol</sub>/g<sub>cat</sub> h. The pipelines were  
230 heated to prevent methanol and products condensation. Before the catalytic test, the samples  
231 were pretreated at 673 K under the flow of Ar (50 mL/min) for 1 h. The outlet gas stream was  
232 analyzed continuously with a mass spectrometer Prisma QMG220 (Pfeiffer). The following  
233 mass/charge signals were recorded: 2(H<sub>2</sub>), 16 (CH<sub>4</sub>), 18 (H<sub>2</sub>O), 28 (CO), 29, 31 and 32  
234 (methanol), 40 (Ar), 44 (CO<sub>2</sub>), 45 (DME), 58 and 59 (olefins).

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## 235 Results and discussions

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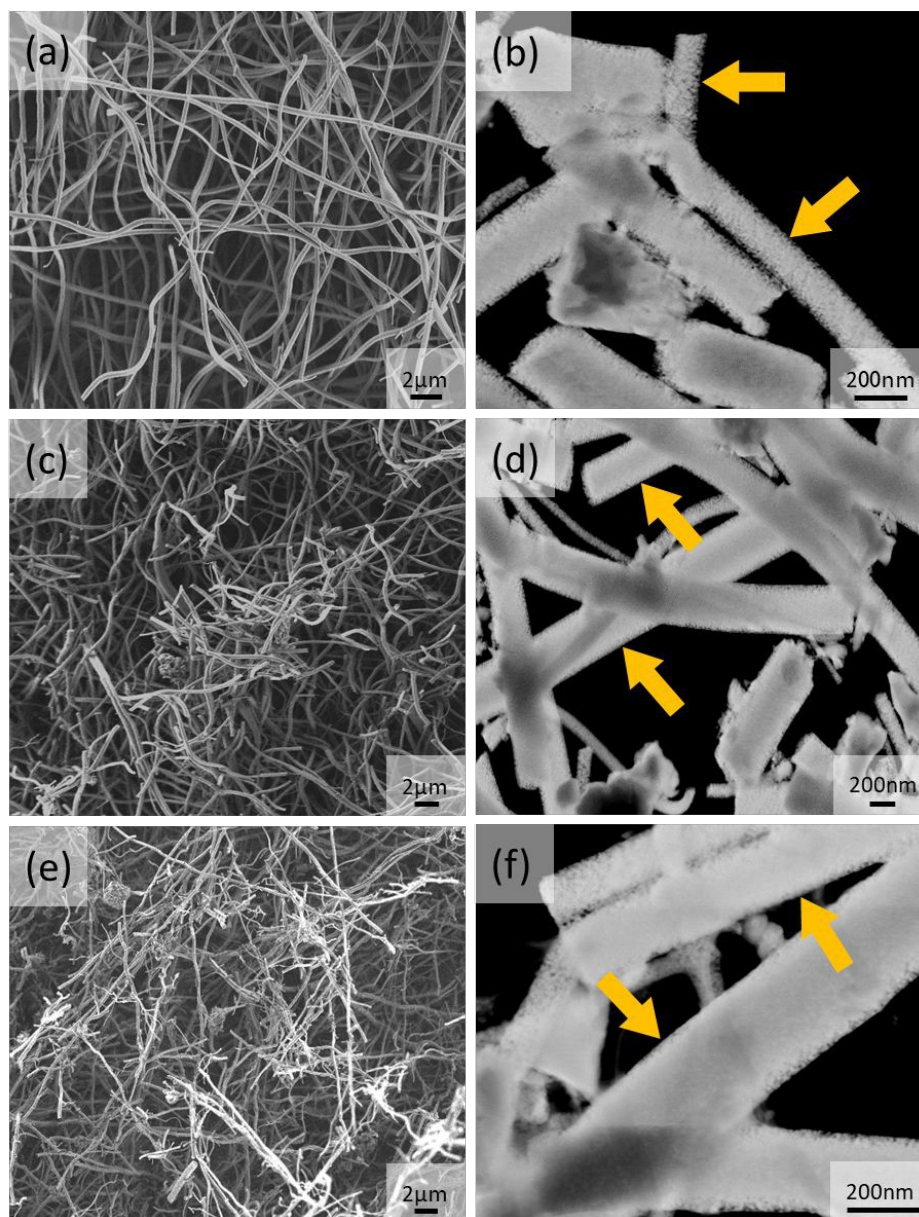
### 236 Hybrid ANFs containing MOR

237 The synthesis of the hybrid ANFs started by selecting the MOR crystallite size. Commercial  
238 NaMOR, which has an average crystallite size of 220 nm (**Figure S1a**), has been used during  
239 electrospinning. However, it is found that this leads to severe heterogeneities after annealing  
240 (**Figure S1b**). These heterogeneities are attributed to the relatively large (compared to the  
241 nanofiber dimensions) crystallite size of NaMOR, which upon annealing, promotes nanofiber  
242 instability leading to hybrid ANFs without shape (**Figure S1b**). In contrast to the commercial  
243 NaMOR, the synthesized NaMOR shown in **Figure S2** has smaller crystallite sizes ranging  
244 between 110 and 118 nm. The crystallite size is nearly half of the nanofiber diameter. From the  
245 results, small MOR crystallite can lead to fewer heterogeneities in ANFs, as shown in **Figure**  
246 **1**. In this Figure, the hybrid ANFs (**Figure 1c**) and (**Figure 1e**) retain their nanofiber shape,  
247 similar to ANFs in **Figure 1a**) that show a non-woven fiber morphology. The estimated  
248 nanofiber diameters are  $321 \pm 74$  nm for ANFs,  $315 \pm 120$  nm for ANFs containing NaMOR  
249 (ANF-NaMOR), and  $241 \pm 76$  nm for ANFs containing HMOR (ANF-HMOR).

250 A detailed structural analysis using dark-field STEM images is also presented in **Figures 1b**),  
251 **1d**), and **1f**) to provide insights into the hybrid ANFs morphology. From the images, less dense  
252 ANFs nanofibers are found in **Figure 1b**). The effect becomes evident at the edges of the ANFs,  
253 with small pore openings (see yellow arrows). In contrast, STEM images of ANF-NaMOR and  
254 ANF-HMOR in **Figures 1d**) and **1f**) show denser areas at the borders and center of the fiber  
255 structure, possibly due to MOR nanocrystals inside the fibers, which could act as a ‘filler’  
256 material densifying the nanofibers. It should be noted that the high amount of broken fibers is  
257 due to the sonication used during specimen preparation for STEM. To this end, EDS mapping  
258 in **Figure S3** is used to verify the hybrid nanofiber constitution and generate insights into the



259 MOR distribution by looking at the silicon  $K\alpha_1$  signal. Silicon signal has been found in the  
 260 non-woven structure and specific densified areas.



261  
 262 **Figure 1.** SEM and dark-field STEM images of (a,b) ANFs, (c,d) ANF-NaMOR and (e,f) ANF-  
 263 HMOR. The yellow arrows highlight the pore openings in the fibers.

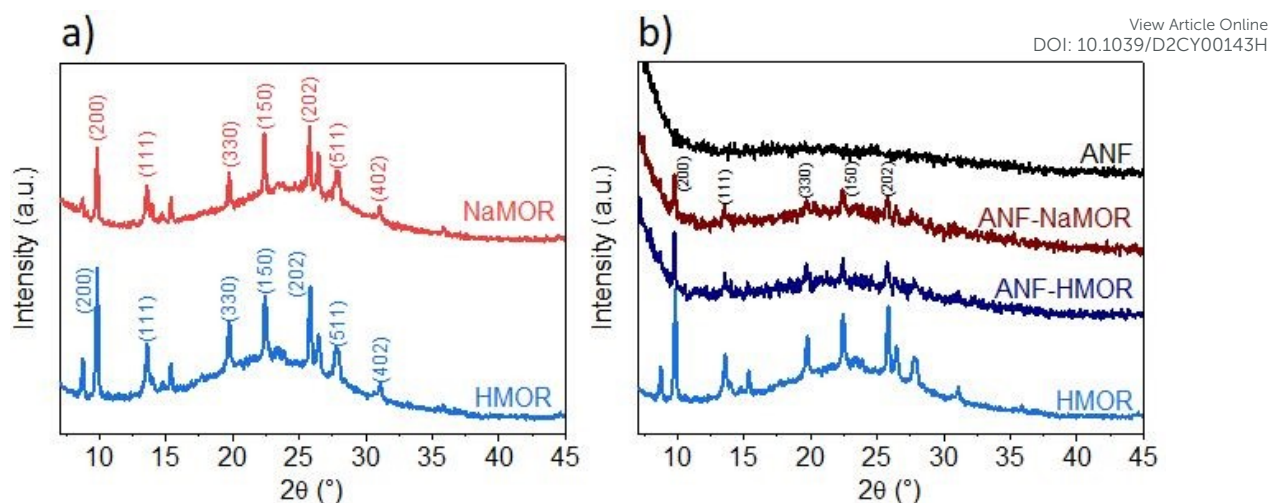
264 The chemical composition at the surface of the hybrid ANFs from **Figure 1** is analyzed with  
 265 XPS to determine the types of species present on the hybrid ANFs (**Figure S4** and **Table S1**).  
 266 In short, elemental analysis with XPS in **Table S1** reveals nitrogen presence in MOR. The  
 267 results suggest that  $\text{NH}_4^+$  has exchanged with NaMOR to form the acidic form of MOR after



268 calcination. Temperature desorption carried out for HMOR demonstrates that at 773 K,  $\text{NH}_4^+$  could be retained at the catalyst.<sup>85</sup> For temperatures 823 K, the  $\text{NH}_4^+$  in the form of  $\text{NH}_3$  has  
269 not been detected.<sup>85</sup> For ANF-HMOR in **Table S1**, no nitrogen has been observed.  $\text{NH}_3$ -TPD  
270 is carried out for ANF-NaMOR and ANF-HMOR to demonstrate an increase in acidity in ANF-  
271 HMOR, most probably from the HMOR. In this case, ANF-NaMOR is used as a control. ANF-  
272 NaMOR show 112  $\mu\text{mol/g}$  of  $\text{NH}_3$  desorbed, whereas ANF-HMOR has 216  $\mu\text{mol/g}$  of  $\text{NH}_3$   
273 desorbed. The general survey of the nanofibers revealed only the presence of aluminum and  
274 oxygen. Therefore, we can ensure that neither the ANFs nor hybrid fibers contain impurities  
275 from the electrospinning precursors. Additionally, to verify the MOR content in ANFs, XRD is  
276 assessed. The XRD diffraction patterns of NaMOR and HMOR nanocrystals and the hybrid  
277 ANFs are presented in **Figure 2**. First, we investigate the crystallographic features of the  
278 NaMOR before and after ion exchange with  $\text{NH}_4^+$ . The XRD diffraction patterns of NaMOR  
279 and HMOR are presented in **Figure 2a**). The XRD for NaMOR shows diffraction peaks at  $2\theta$   
280 =  $9.8^\circ$  (200),  $13.5^\circ$  (111),  $19.7^\circ$  (330),  $22.3^\circ$  (150),  $25.7^\circ$  (202),  $26.4^\circ$  (350),  $27.7^\circ$  (511),  $31.0^\circ$   
281 ( $402$ ) which match with literature from MOR ( $2\theta = 9.8^\circ$ ,  $13.5^\circ$ ,  $19.6^\circ$ ,  $22.3^\circ$ ,  $25.7^\circ$ ,  $26.3^\circ$ ,  $27.5^\circ$ ,  
282 and  $30.9^\circ$ ).<sup>86–88</sup> HMOR present similar diffraction peaks as NaMOR ( $2\theta = 9.8^\circ$ ,  $13.5^\circ$ ,  $19.7^\circ$ ,  
283  $22.4^\circ$ ,  $25.7^\circ$ ,  $26.4^\circ$ ,  $27.7^\circ$ , and  $31^\circ$ ). No other crystallographic phase is observed for both  
284 samples. **Figure 2b**) compares the HMOR nanocrystals with ANF-NaMOR and ANF-HMOR  
285 hybrid fibers. In the same **Figure 2b**), XRD of nanofibers is presented. No crystalline phase  
286 has been observed for the ANF sample, confirming the amorphous characteristic of ANF. ANF-  
287 NaMOR and ANF-HMOR diffractograms present peaks that correspond to MOR (**Figure 2a**)).  
288 No other crystallographic phase for the hybrid ANFs is observed.  
289

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290  
291 **Figure 2.** a) XRD diffraction pattern of bare NaMOR and HMOR nanocrystals and b) ANFs,  
292 ANF-NaMOR, and ANF-HMOR.

293 The effect of MOR has been observed in **Figure 1** with more densified hybrid nanofibers. The  
294 presence of MOR in the hybrid fibers became evident with the XRD analysis in **Figure 2**.  
295 However, an essential aspect is understanding how MOR affects the surface area in the  
296 nanofibers. In **Table 1**, the total surface area of the nanofibers is presented. From the produced  
297 catalysts, ANFs possess the highest surface area ( $192 \text{ m}^2/\text{g}$ ), followed by hybrid ANF-HMOR  
298 ( $121 \text{ m}^2/\text{g}$ ) and ANF-NaMOR ( $107 \text{ m}^2/\text{g}$ ). The reason for a reduced surface area for nanofibers  
299 is that the NaMOR or HMOR might block pore accessibility in ANFs.<sup>54,89,90</sup>

300 To generate insights into the pore distribution for ANFs with and without MOR, the analysis of  
301 the BET isotherms is presented in **Figure 3**. For ANFs, ANF-NaMOR, and ANF-HMOR in  
302 **Figure 3a**), adsorption-desorption isotherms showed hysteresis loops in the multilayer step,  
303 which is associated with capillary condensation type IV isotherms for mesopores with H2  
304 hysteresis according to IUPAC classification.<sup>91</sup> The hysteresis loop is characteristic of  
305 mesoporous materials with cage-like pores or pores with constrictions at the pore opening.<sup>92,93</sup>



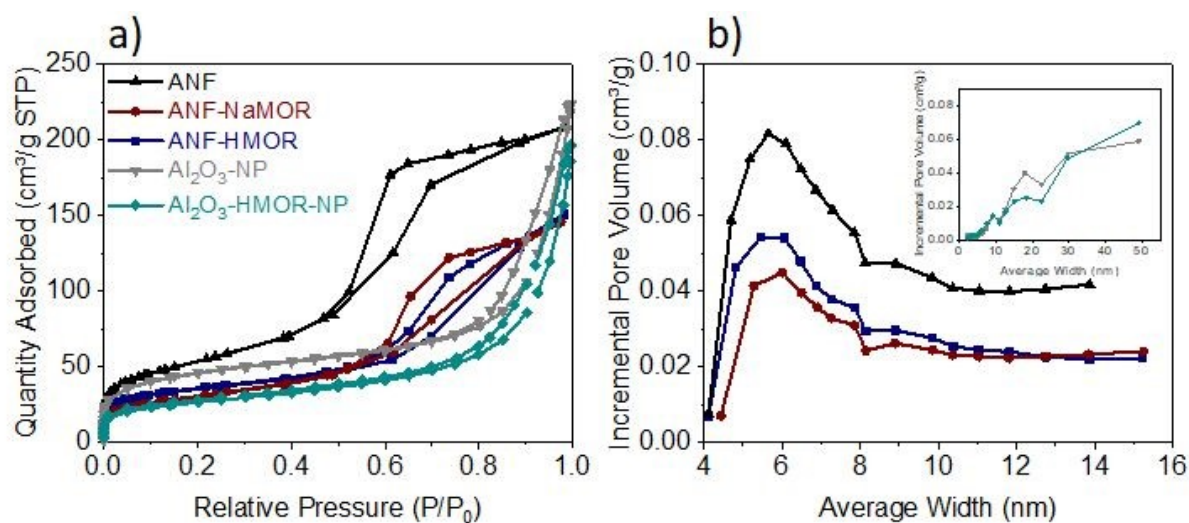


306 The pore distribution plots are presented in **Figure 3b)** and revealed a wide distribution of pore  
307 bodies, with a majority distribution of pore widths around 6 nm for ANFs and hybrid ANFs  
308 with NaMOR and HMOR. **Figure 3b)** shows that ANFs have the highest mesopore and  
309 incremental pore volume, followed by ANF-HMOR and ANF-NaMOR. This indicates that the  
310 MOR modifies the textural properties of ANFs by decreasing the number of pore bodies. The  
311 results agree with STEM images in **Figures 1b), 1d), and 1f)**.  
312 Taking the results from the ANFs and hybrid ANFs together, the effect of structuring should be  
313 compared with the same type of catalysts but without nanofiber shape, as shown in **Figure S5**.  
314 The Al<sub>2</sub>O<sub>3</sub>-NP and Al<sub>2</sub>O<sub>3</sub>-HMOR-NP control samples have been produced using the same  
315 alumina and HMOR precursors. The total surface area of Al<sub>2</sub>O<sub>3</sub>-NP and Al<sub>2</sub>O<sub>3</sub>-HMOR-NP are  
316 presented in **Table 1**. This table shows a decrease in surface area of approximately 30 m<sup>2</sup>/g for  
317 Al<sub>2</sub>O<sub>3</sub>-NP compared to the ANFs counterpart. Similar results are observed for Al<sub>2</sub>O<sub>3</sub>-HMOR-  
318 NP and the hybrid ANF-HMOR. We hypothesize that the ANFs are less prone to sintering due  
319 to restriction of the growth of crystals in the fibers (by confinement) and thus present a higher  
320 surface area, as shown in **Table 1**. When comparing the BET isotherms, variations between the  
321 Al<sub>2</sub>O<sub>3</sub>-NP or Al<sub>2</sub>O<sub>3</sub>-HMOR-NP are observed. In this case, the type IV adsorption-desorption  
322 isotherm shape with an H3 hysteresis loop has been found for Al<sub>2</sub>O<sub>3</sub>-NP and Al<sub>2</sub>O<sub>3</sub>-HMOR-NP  
323 (**Figure 3a)**). Here, the sharp increase at high P/P<sub>0</sub> (0.85-0.99) suggests the presence of

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324 aggregated slit-shaped pores, which may originate in the interparticle voids. For isotherms with  
 325 hysteresis loop at high  $P/P_0$ , it is likely to observe wide pore size distribution,<sup>94–97</sup> as observed  
 326 in the inset in **Figure 3b**). The pore size corresponds to  $\text{Al}_2\text{O}_3$ -NP, and  $\text{Al}_2\text{O}_3$ -HMOR-NP is 9  
 327 nm, similar to the hybrid ANFs. These results might indicate that the hybrid ANFs also provide  
 328 access for the diffusion of  $\text{N}_2$  molecules, most probably due to the fiber network.<sup>43</sup>



329 **Figure 3.** (a) Adsorption-desorption isotherms and (b) pore size distribution for ANFs, ANF-  
 330 NaMOR, ANF-HMOR,  $\text{Al}_2\text{O}_3$ -NP, and  $\text{Al}_2\text{O}_3$ -HMOR-NP.

331  
 332 **Table 1.** Fiber diameter, surface area, pore size, and total acidity of ANFs, ANF-NaMOR, ANF-  
 333 HMOR,  $\text{Al}_2\text{O}_3$ -NP, and  $\text{Al}_2\text{O}_3$ -HMOR-NP.

Sample	Surface area (m <sup>2</sup> /g)	Total acidity at 373 K (μmol/g)	Total acidity at 373 K (μmol/ m <sup>2</sup> )
ANFs	192	178	0.9
ANF-NaMOR	107	116	1.1
ANF-HMOR	121	276	2.3
$\text{Al}_2\text{O}_3$ -NP	162	255	1.6



Al<sub>2</sub>O<sub>3</sub>-HMOR-NP

94

184

2.0

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334

335 Pyridine (Py) is used as a probe molecule to determine the nature of the acid sites (i.e., either  
336 LAS or BAS).<sup>98</sup> In **Figures 4a)** and **4b)**, the FTIR spectra of Py adsorbed at 303 K are presented.

337 The samples composed of alumina mainly (ANFs, Al<sub>2</sub>O<sub>3</sub>-NP), Al<sub>2</sub>O<sub>3</sub>-HMOR-NP, and hybrid

338 alumina (ANF-NaMOR, ANF-HMOR) present an intense band at 1446, 1577, and 1614 cm<sup>-1</sup>.

339 In the case of MOR (NaMOR, HMOR) used for comparison, these peaks are weaker. These

340 bands are attributed to Py adsorbed on LAS, produced by uncoordinated Al<sup>3+</sup> or cation

341 vacancies.<sup>99</sup> The signal at 1545 cm<sup>-1</sup> corresponds to Py adsorbed on BAS (PyH<sup>+</sup>) (**Figure 4b)**).

342 Among the MOR, only HMOR shows an IR band at 1545 cm<sup>-1</sup>. This band confirms that

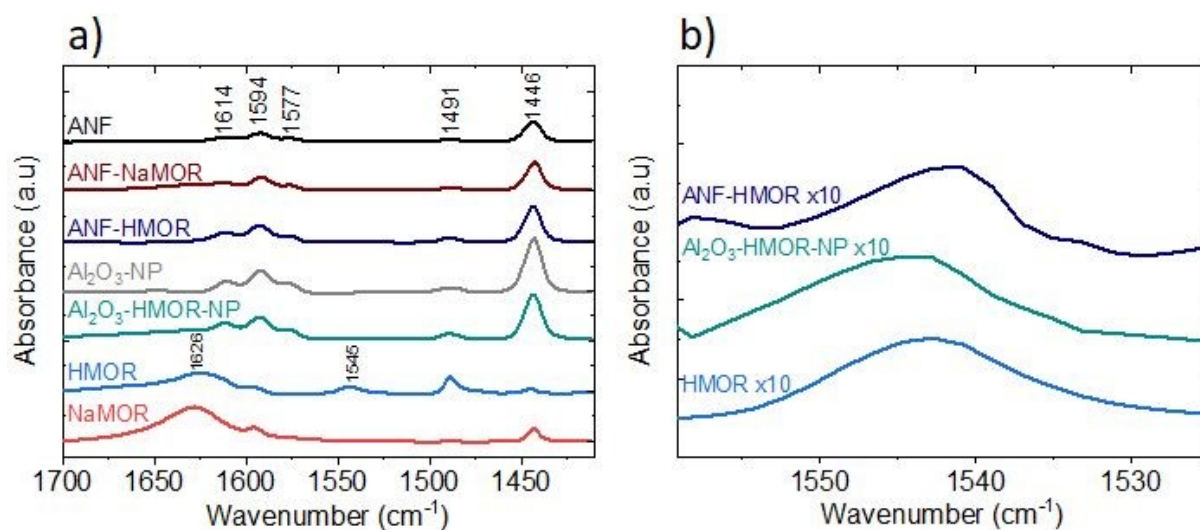
343 HMOR, ANF-HMOR, and Al<sub>2</sub>O<sub>3</sub>-HMOR-NP, contain BAS. The results help to validate the

344 presence of HMOR in the ANFs. NaMOR and ANF-NaMOR do not reveal BAS, and thus, are

345 not tested during DME production. Interestingly, it should be noted that for all samples, two

346 peaks close to 1594 cm<sup>-1</sup> and 1491 cm<sup>-1</sup> are present and are assigned to hydrogen-bonded Py

347 and Py adsorbed on both LAS and BAS.<sup>100</sup>



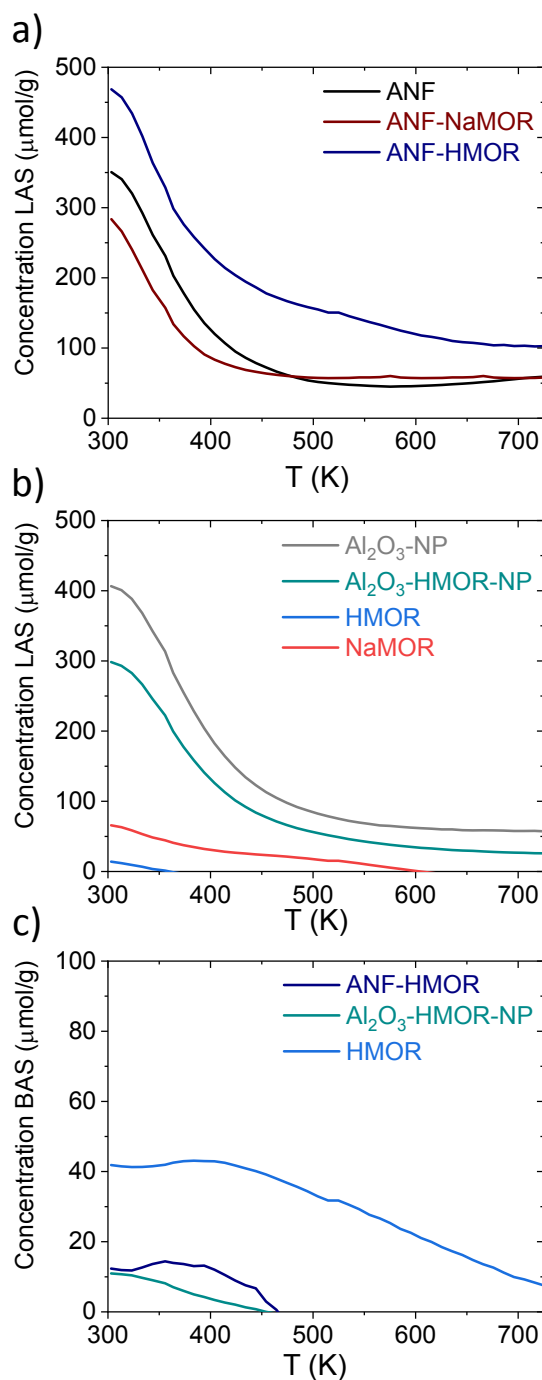
348



349 **Figure 4.** FTIR spectra after Py adsorption at 303 K. a) Full Py range. b) Detailed Py spectra  
350 highlighting the BAS band.

351 We continued with Py-TPD analysis to determine the amount and the strength of LAS and BAS  
352 from **Figure 4**. Py-TPD in **Figure 5** shows the LAS and BAS density (expressed in  $\mu\text{mol/g}$ ) as  
353 a function of temperature, estimated using the  $1446\text{ cm}^{-1}$  and  $1545\text{ cm}^{-1}$  IR bands, where the  
354 band at  $1446\text{ cm}^{-1}$  is used to estimate the total amount of LAS. Several authors<sup>101–103</sup> showed  
355 that the integrated molar extinction coefficients of LAS do not depend on the nature of oxides,  
356 the structure, and the strength of acid sites. Therefore, the Emeis's<sup>101</sup> averaged extinction  
357 coefficients of Py adsorption on LAS ( $2.22\text{ cm } \mu\text{mol}^{-1}$ ) and BAS ( $1.67\text{ cm } \mu\text{mol}^{-1}$ ) are used to  
358 quantify the number of sites. For BAS, the IR band at  $1545\text{ cm}^{-1}$  is used for quantification.





359  
360 **Figure 5.** Py-TPD for ANF, ANF-NaMOR, ANF-HMOR, Al<sub>2</sub>O<sub>3</sub>-NP, Al<sub>2</sub>O<sub>3</sub>-HMOR-NP,  
361 HMOR, and NaMOR. In **a)**, **b)** LAS (μmol/g), and **c)** BAS (μmol/g) are shown for various  
362 samples.

363 From **Figure 5a)**, at 303 K, the hybrid ANF-HMOR has the highest LAS content. This can be  
364 correlated to the presence of HMOR. Contrary to ANF-HMOR, ANF-NaMOR shows the  
365 lowest LAS concentration, probably because the NaMOR blocks the acid sites of the



366 nanofibers. Lastly, the LAS content remains also low in ANFs. In **Figure 5a**), the experiments  
367 demonstrate that LAS content in ANF-HMOR remains higher than Al<sub>2</sub>O<sub>3</sub>-NP, Al<sub>2</sub>O<sub>3</sub>-HMOR-  
368 NP, or MOR, as shown in **Figure 5b**). A possible explanation for ANF-HMOR is that  
369 incorporating modifiers on alumina (e.g., HMOR) might promote dealumination, leading to the  
370 formation of multiple Al species. Along with HMOR, such Al species can increase the amount  
371 of LAS.<sup>104,105</sup> The results indicate that structured hybrid systems, such as ANF-HMOR can  
372 achieve high acidity, even higher than unstructured acid catalysts (**Figure 5b**). The rationale  
373 behind our observations is that the nanofiber structure can help densify the acid sites and  
374 provide better access to molecules (such as Py), which might be challenging in unstructured  
375 acid catalysts (**Figure S5**). Furthermore, Py-TPD reveals that Py desorbs relatively fast from  
376 LAS at low temperatures (300-350 K), indicating the presence of weak acid sites (**Figure 5a**).  
377 At temperatures higher than 350 K, a slight decrease in Py desorption, most probably to the  
378 presence of medium and strong acid sites.<sup>43</sup> Interestingly, after 500 K, all the alumina-modified  
379 samples retain similar LAS, except for the ANF-HMOR, where the Py is still adsorbed at 700  
380 K, suggesting the presence of strongly adsorbed Py species over LAS. The results in **Figures**  
381 **5a**) and **5b**) (also shown in **Table 1**) confirm that hybrid ANF-HMOR is the most acid catalyst  
382 (276 μmol/g), followed by ANFs (178 μmol/g) and ANF-NaMOR (116 μmol/g).

383 In **Figure 5c**), HMOR presents the highest BAS density. Py starts desorbing at 400 K and  
384 remains adsorbed until 723 K, which means it has the highest Brønsted acid strength. Hybrid  
385 ANF-HMOR and Al<sub>2</sub>O<sub>3</sub>-HMOR-NP present less BAS density due to the lower amount of  
386 HMOR. BAS disappears at 460 K in both cases, indicating that sites have a lower BAS strength.  
387 It is essential to mention that although Py desorption occurs in **Figure 5**, the acid sites remain  
388 present and can help to catalyze reactions, such as methanol dehydration to DME.



389 The amount of BAS and LAS for three different temperatures (303, 373, and 423 K) from  
 390 **Figure 5** are shown in **Table 2**. In **Table 2**, the ANF-HMOR has the highest acidity and  
 391 LAS/BAS ratios at 303 K and 373 K, except at 423 K. At 423 K, BAS content is slightly high  
 392 for ANF-HMOR (9  $\mu\text{mol/g}$ ) and reflected in **Table 2**. Overall, **Figure 5** shows that  
 393 incorporating MOR in the alumina modulates the acid site amount and nature.

394 **Table 2**. Calculated LAS, BAS, total acidity ( $\mu\text{mol/g}$ ), and LAS/BAS ratios samples at various  
 395 selected temperatures.

T	303K				373K				423K			
Sample	LAS	BAS	Total acidity	LAS/BAS	LAS	BAS	Total acidity	LAS/BAS	LAS	BAS	Total acidity	LAS/BAS
ANFs	351	-	351	-	178	-	178	-	95	-	95	-
ANF-NaMOR	283	-	283	-	117	-	117	-	73	-	73	-
ANF-HMOR	469	12	481	38	276	14	290	20	204	9	213	23
Al <sub>2</sub> O <sub>3</sub> -NP	406	-	406	-	255	-	255	-	148	-	148	-
Al <sub>2</sub> O <sub>3</sub> -HMOR-NP	298	11	309	27	178	6	184	30	101	2	103	49
HMOR	14	42	56	0.33	-	43	43	-	-	42	42	-
NaMOR	66	-	66	-	37	-	37	-	27	-	27	-

396

### 397 Methanol dehydration to DME

398 The methanol dehydration to DME is assessed as a proof of concept reaction to underline the  
 399 functionality of the hybrid nanofibers. **Figure 6a)** shows the methanol conversion of ANF,  
 400 ANF-HMOR, Al<sub>2</sub>O<sub>3</sub>-NP, Al<sub>2</sub>O<sub>3</sub>-HMOR-NP, and HMOR over a temperature range of 423 and  
 401 673 K. From these catalysts, HMOR starts converting the methanol at lower temperatures (<423  
 402 K) than Al<sub>2</sub>O<sub>3</sub>-NP and ANFs. However, for temperatures higher than 523 K, the alumina  
 403 materials are very active and reach the equilibrium conversion at ca. 613 K (Al<sub>2</sub>O<sub>3</sub>-NP) and 648  
 404 K (ANFs). At 673 K, ca. 38% of conversion is reached for HMOR, while for Al<sub>2</sub>O<sub>3</sub>-NP and  
 405 ANFs, the conversion is ca. 90%. Note that the measured conversion corresponds to the  
 406 equilibrium conversion. The low conversion of HMOR can be related to the low amount of acid  
 407 sites over the explored temperature range shown in **Figure 5** and **Figure 6a)**.

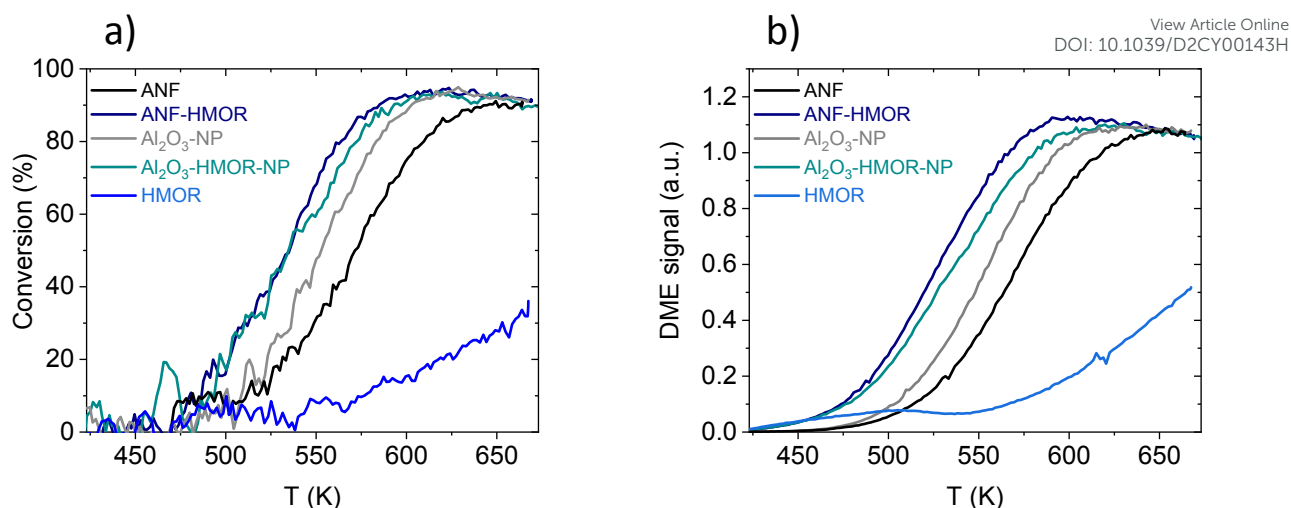


408 A comparison between Al<sub>2</sub>O<sub>3</sub>-NP and ANFs is also assessed. Al<sub>2</sub>O<sub>3</sub>-NP is more active than the  
409 ANFs, probably due to the higher amount of acid sites per weight of catalysts. Interestingly, the  
410 hybrid ANF-HMOR is more active than the Al<sub>2</sub>O<sub>3</sub>-NP and ANFs. This includes the light-off  
411 curves of ANF-HMOR and Al<sub>2</sub>O<sub>3</sub>-HMOR-NP, which are very similar. Such similarities include  
412 the methanol conversion temperature, which starts at 473 K and reaches the equilibrium  
413 conversion at ca. 598 K. However, variations in DME signal intensity are observed in **Figure**  
414 **6b)** for ANF-HMOR and Al<sub>2</sub>O<sub>3</sub>-HMOR-NP. In this case, the results indicate that ANF-HMOR  
415 is more selective (**Table 3**) to DME than the other acid catalysts.

416 It is then important to compare conversion (**Figure 6a**) and selectivity (**Table 3**) at 573K for  
417 ANF, ANF-HMOR, Al<sub>2</sub>O<sub>3</sub>-NP, Al<sub>2</sub>O<sub>3</sub>-HMOR-NP, and HMOR. ANF-HMOR remains the  
418 highest in **Figure 6a**) and **Table 3**, followed by Al<sub>2</sub>O<sub>3</sub>-HMOR-NP, ANFs Al<sub>2</sub>O<sub>3</sub>-HMOR-NP,  
419 Al<sub>2</sub>O<sub>3</sub>-NP, and HMOR. The temperature at 50% conversion (T<sub>50</sub>) and DME selectivity are also  
420 shown in the same table. Again, ANF-HMOR remains with the lowest T<sub>50</sub>, highest conversion  
421 at 573 K, and DME selectivity, followed by less selective acid catalysts such as Al<sub>2</sub>O<sub>3</sub>-HMOR-  
422 NP, ANFs, and Al<sub>2</sub>O<sub>3</sub>-NP. Interestingly, despite its lower conversion (**Figure 6a**), the ANFs  
423 are more selective to DME than the Al<sub>2</sub>O<sub>3</sub>-NP (**Table 3**), most probably due to the open  
424 structure network and the high surface area among the acid catalyst in **Table 1**. Furthermore,  
425 the apparent activation energy calculated from the rate of DME production vs. 1/T is shown in  
426 **Table 3** to compare the catalyst performance further. The activation energy for the ANFs, with  
427 (99 kJ/mol) and without (96 kJ/mol) HMOR present slightly lower values than the Al<sub>2</sub>O<sub>3</sub>-NP  
428 (108 and 110 kJ/mol). Our results show similar values to other catalysts in the literature. This  
429 entails conversion, selectivity, and activation energy.<sup>69,81,106</sup>







**Figure 6.** a) Methanol conversion during the light off curves. b) DME signal intensity during the light-off curves.

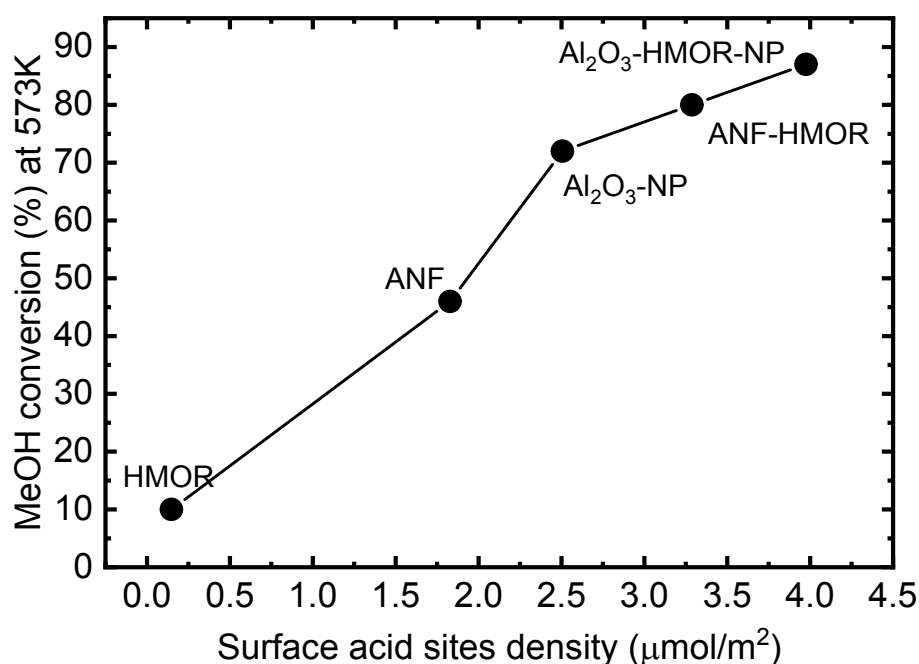
**Table 3.** Methanol conversion (%) and DME selectivity.

Sample	Methanol conversion (%) at 573 K*	DME Selectivity (relative intensity) at 573 K*	Conversion at T <sub>50</sub> (K)*	DME Selectivity (relative intensity) at T <sub>50</sub> (K)*	Apparent activation Energy (kJ/mol)
ANFs	46	1	573	0.9	96 ± 1
ANF-HMOR	87	1	534	1	99 ± 3
Al <sub>2</sub> O <sub>3</sub> -NP	72	0.9	553	0.8	110 ± 1
Al <sub>2</sub> O <sub>3</sub> -HMOR-NP	80	0.9	535	0.8	108 ± 4
HMOR	10	0.9	>673	-	84 ± 4

\*The results are derived from the light-off curve, where the experimental error is lower than 15%.

We then compare the acidity (**Figure 5** and **Table 2**) with the catalytic performance (**Figure 6** and **Table 3**) to generate insights into the ANF-HMOR synergy. It is generally accepted that the catalyst composition, surface area, porosity (i.e., pore size and its distribution), and surface acidity affect the performance of the methanol dehydration reaction to DME.<sup>70</sup> In this reaction, the catalytic activity depends on the surface acidic properties, such as the total number of acidic sites and their strength. **Figure S6** shows the number of acid sites (μmol/g) and the T<sub>50</sub> (K) as a function of the surface area (m<sup>2</sup>/g). Here, it is observed that the acid sites do not depend on

443 the surface area, and it also does not directly influence the catalyst activity. Earlier reports<sup>70,107</sup> showed that the catalytic activity could be correlated with the number of acidic sites; however, 444 this behavior has not been observed but provides insight into other factors affecting activity.<sup>75</sup> 445 From the mechanistic point, methanol dehydration is considered a bimolecular reaction 446 between two intermediates adsorbed on adjacent surface sites and requires the proximity of two 447 acid sites with adequate acidity.<sup>81</sup> Thus, increasing the acid sites density leads to improved 448 catalyst performance. This becomes evident in **Figure 7**, which shows that the conversion 449 increases with the acid sites density ( $\mu\text{mol}/\text{m}^2$ ). The synergy between LAS and BAS produced 450 by interfacial interaction also enhances the methanol dehydration rate.<sup>108</sup> Therefore, the 451 addition of HMOR in the ANF and  $\text{Al}_2\text{O}_3$ -NP modifies both the acid site density and the acid 452 types by incorporating BAS, thus improving the catalyst performance. 453



454 **Figure 7.** Conversion at 573 K as a function of the acid sites density ( $\mu\text{mol}/\text{m}^2$ ) at 303 K for 455 the unstructured catalysts (HMOR,  $\text{Al}_2\text{O}_3$ -NP, and  $\text{Al}_2\text{O}_3$ -HMOR-NP) and nanofibers (ANF, 456 and ANF-HMOR). 457



458 In addition to the nature and strength of the acid sites, the textural properties, such as the surface  
459 area, porosity, and average pore diameter, can affect the catalytic performance in dehydration  
460 reactions.<sup>69,81</sup> The BET isotherms (**Figure 3b**) suggest the presence of aggregated slit-shaped  
461 pores, which may originate in the interparticle voids in the Al<sub>2</sub>O<sub>3</sub>-NP and Al<sub>2</sub>O<sub>3</sub>-HMOR-NP.  
462 Additionally, they present a wide pore size distribution. On the contrary, the pore distribution  
463 plots revealed a wide distribution of pore bodies, with a majority distribution of pore widths  
464 around 6 nm for ANFs and hybrid ANFs with NaMOR and HMOR. Furthermore, compared to  
465 the NP that forms agglomerates and lacks structured macroporosity (**Figure S5**), the nanofibers  
466 present a lower diffusion length (d=240-320 nm). This is expected due to the non-woven  
467 nanofiber structure that contains macropore mesh.<sup>43</sup> These differences in the average pore size,  
468 pore size distribution, and diffusion length may explain the variations in selectivity. In the  
469 Al<sub>2</sub>O<sub>3</sub>-NP and Al<sub>2</sub>O<sub>3</sub>-HMOR-NP, the products could have a higher retention time leading to  
470 by-products, such as CO and hydrocarbons, and thus decreasing the DME selectivity. Our  
471 results suggest that hierarchical structures like fibers and HMOR can enhance chemical reaction  
472 selectivity synergistically.

473 Based on the catalytic tests used to highlight the hybrid nanofibers' functionality, we can  
474 conclude that a higher conversion of methanol to DME is achieved when samples contain high  
475 acid sites densities and both types of acid sites (LAS and BAS). The presence of both types of  
476 acid sites provides synergy effects that positively influence the activity towards the methanol  
477 dehydration to DME. Additionally, the fiber morphology favors the DME selectivity. Further

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- 478 studies on ANF-HMOR materials could optimize the amount of BAS and LAS to maximize View Article Online  
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- 479 conversion and selectivity under dehydration reactions conditions.



480 **Conclusions**View Article Online  
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481 Hybrid ANFs with high acidity has been synthesized using electrospinning. Acid sites tunability  
482 is possible in these nanofibers using MOR nanocrystals. The nanofibers have shown multilevel  
483 pore combinations, such as mesopores and macropores. IR-Py demonstrates the nature type,  
484 and desorption strength of the acid sites in the ANF-HMOR, which prevail between 423 and  
485 673 K. The methanol dehydration reactions showed the advantage of the ANF-HMOR  
486 synergistically contributing to increase methanol conversion and DME selectivity.



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