

Electrochemical Characterization of Chromate Free Conversion Coatings on Electrogalvanized Steel

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The chromate conversion treatment is widely used, but it requires highly toxic chromic acid solutions with the consequent effluent disposal and ecological problems. The removal of these toxic chemicals is considered a priority within European Union. The corrosion resistance of three alternative treatments applied on electrogalvanized steel, and immersed in aerated 0.3 M Na₂SO₄ solution, pH 10, at 25 °C, was investigated using electrochemical techniques. Their performance was compared with the obtained using the traditional Cr⁶⁺-based treatment in the same conditions. The achieved results show that the alternative coatings exhibited discrete protective properties in the sulphate solution. The nitro-cobalt chemical conversion treatment showed similar protective properties than the traditional Cr⁶⁺-based treatment, while with the Cr³⁺-based treatment those were very poor. The phosphate treatment initially performed acceptably but as the time elapsed, its protective properties decreased.

Keywords: *conversion-coating, electrodeposition, electrochemical techniques, corrosion*

1. Introduction

Electroplated zinc coating is employed as active galvanic protection for steel. However, zinc is very reactive and thus high corrosion rates of this coating are observed in internal and external atmospheres¹. For this reason, a post-treatment is necessary to increase their useful life. In current industrial practice, this treatment consists of immersion in a chemical bath that forms a conversion layer over plated zinc. Such a layer behaves as a dielectric passive one with high corrosion resistance, and provides better surface for paint adherence. The main problem of the traditionally used post-treatments is the presence of Cr⁶⁺ salts, considered carcinogenic substances whose use is forbidden by European norms². Molybdates, tungstates, permanganates and vanadates, including chromium like elements, were the first chemical elements tried as hexavalent chromium substitutes³⁻⁷. Recently alternative coatings were also developed based on zirconium and titanium salts⁸⁻⁹, cobalt salts^{10,11}, organic polymers^{12,13} and rare earth salts¹⁴. However, the preparation and corrosion behavior of these coatings is not clear and their practical use is doubtful.

In order to find an alternative treatment to Cr⁶⁺ conversion coatings, several treatments providing good anti-corrosive behavior, high benefit/cost relation and, mainly, low environmental impact are still to be developed. Usually, the coatings' corrosion performance is evaluated using traditional essays such as Salt Spray¹⁵, Kesternich test¹⁶, saturated humidity¹⁷. However, the authors consider important the application of electrochemical methods to obtain faster information about the corrosion reactions kinetics.

Among the electrochemical techniques that can be used, the electrochemical impedance spectroscopy (EIS) was selected based on results already obtained when the bare and/or coated metals corrosion was evaluated¹⁸⁻²¹.

The main purpose of the present work was to find an environmentally friendly conversion treatment that can be used as an acceptable alternative to the Cr⁶⁺-based treatment. The corrosion behavior of electrogalvanized steel sheets covered with Cr⁶⁺-free treatments was investigated by electrochemical techniques. The obtained results were compared with those coming from applying the traditional Cr⁶⁺-based treatment.

2. Experimental Details

2.1. Samples

Electrogalvanized steel samples (7.5 cm × 10 cm × 0.1 cm) industrially produced and covered with the following conversion treatments: (A) based on Cr⁺³; (B) nitro-cobalt chemical conversion; (C) phosphate; and (D) traditional Cr⁶⁺, were investigated. In each case, a commercial conversion bath was formulated and the coating produced according to the respective supplier recommendations.

2.2. Thickness measurements

Coatings thickness was measured using the Helmut Fischer equipment DUALSCOPE MP4.

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2.3. Morphology

Coatings morphology was observed by scanning electron microscopy (SEM) and the surface microanalysis was performed by energy dispersive spectrometry (EDXS) using a LEICA S440 microscopic.

2.4. Electrochemical behavior

All measurements were performed at a constant room temperature in aerated 0.3 mol.L⁻¹ Na₂SO₄ solution, pH 10, in which the zinc dissolution rate is very slow²² at 25 ± 2 °C. Test electrolytes were prepared from analytical grade materials and distilled water. Solution pH was adjusted by small additions of NaOH solution.

The electrochemical cell consisted of a PMMA cylindrical electrolyte holder attached to the coated surface filled with the test solution. The exposed area was 7.07 cm². The coated metal acted as working electrode, while a Hg/HgSO₄ (SSE) and a platinum mesh were the reference and counter electrodes, respectively. Throughout this paper, all electrochemical potentials are referenced to the Saturated Calomel Electrode (SCE).

Polarization curves were performed with a 1286 Electrochemical Interface at a scan rate of 1 mV.s⁻¹, over the range -300 mV < η < +200 mV vs. the open-circuit potential. The corrosion current density (*i*_{corr}) and corrosion potential (*E*_{corr}) were obtained from the Tafel slopes by extrapolation of the linear portion of the anodic and cathodic branches.

EIS measurements were performed in the frequency range between 10⁻² Hz and 10⁵ Hz using a Solartron 1260 Frequency Response Analyzer coupled to a Solartron 1286 Electrochemical Interface. A sinusoidal signal with amplitude of 13 mV was applied and eight frequency points per decade were registered. The corrosion evolution was analyzed until the appearance of white corrosion products on the samples surface.

All impedance measurements were carried out in a Faraday cage in order to minimize external interference on the system studied.

Taking into account that the corrosion behavior of passivated, painted and/or multi coated materials strictly depends on the production procedure, all the tests were carried out on three replicates of each sample type and the average results obtained for them are reported in the following Tables and Figures.

3. Results and Discussion

The thicknesses and compositions of the investigated samples are reported in Table 1. It can be observed that all the samples present similar coating thickness. Samples coated with the treatments **A**, **C** and **D** were lucid grey, while those protected with the **B** treatment were dark grey. As it was not possible to obtain information about the passive layer thickness, the values shown in Table 1 correspond to the total coating thickness (zinc plus passive layer).

3.1. Morphology

Coatings surface morphology was observed by SEM with magnifications of 2,000X and 10,000X, Figure 1.

Table 1. Thickness and composition of zinc coatings after conversion treatment.

Treatment identification	Conversion Treatment based on	Composition	Coating thickness (μm)
A	Cr ³⁺	Zn, Fe, Cr, P, S	9.1 ± 0.1
B	nitro-cobalt	Zn, Fe, Co, P, S	9.7 ± 0.1
C	phosphate	Zn, Fe, P, S	9.5 ± 0.1
D	Cr ⁶⁺	Zn, Fe, Cr, P, S	8.7 ± 0.2

In general, the coatings exhibited micro-rough and homogenous structure with irregular size growth.

The surface of the **A** samples presented a less uniform structure formed by small nodular grains while, at the lower magnification, the **B** samples exhibited small spherical shaped particles. The surface morphologies of the **C** and **D** samples were very similar and exhibited a plate-like structure, which was more uniform and compact for the latter samples.

Semi-quantitative elemental analysis of surface coatings made by EDXS indicated the presence of S and P; possibly related to the sulfate and phosphate ions contained in the baths compositions. On the other hand, due to the low Cr content found in the surface, **A** and **D** samples did not present the network of cracks characterizing the chromate coatings.

3.2. Electrochemical tests

Corrosion potential measurements and polarization curves performed on electrogalvanised steel surfaces protected by different conversion treatments but exposed to the same aqueous electrolyte provide an opportunity to better analyze the evolution of their electrochemical behavior. When the overall coating system is considered, it should be noted that, being the thin conversion layer the outermost one, electrochemical interactions between this layer and its environment starts just after getting into contact, particularly if the medium is a saline solution. For that reason, the studied conversion coatings play a paramount role in delaying zinc dissolution, acting as a barrier layer to the diffusion of corrosion inducing species towards the underlying zinc film and/or inhibiting the oxygen reduction reaction by polarizing the cathodic areas.

3.2.1. Corrosion potential values

As seen in Figure 2, the corrosion potential (*E*_{corr}) values of all the coated panels ranged between -1.02 V/SCE and -1.05 V/SCE, i.e., at least from the thermodynamic point of view, the chemically different coating layers applied on the zinc surface of those panels did not give rise to marked changes in their electrochemical behavior.

3.2.2. Polarization curves

The anodic and cathodic processes of zinc corrosion, dissolution of zinc



and oxygen reduction

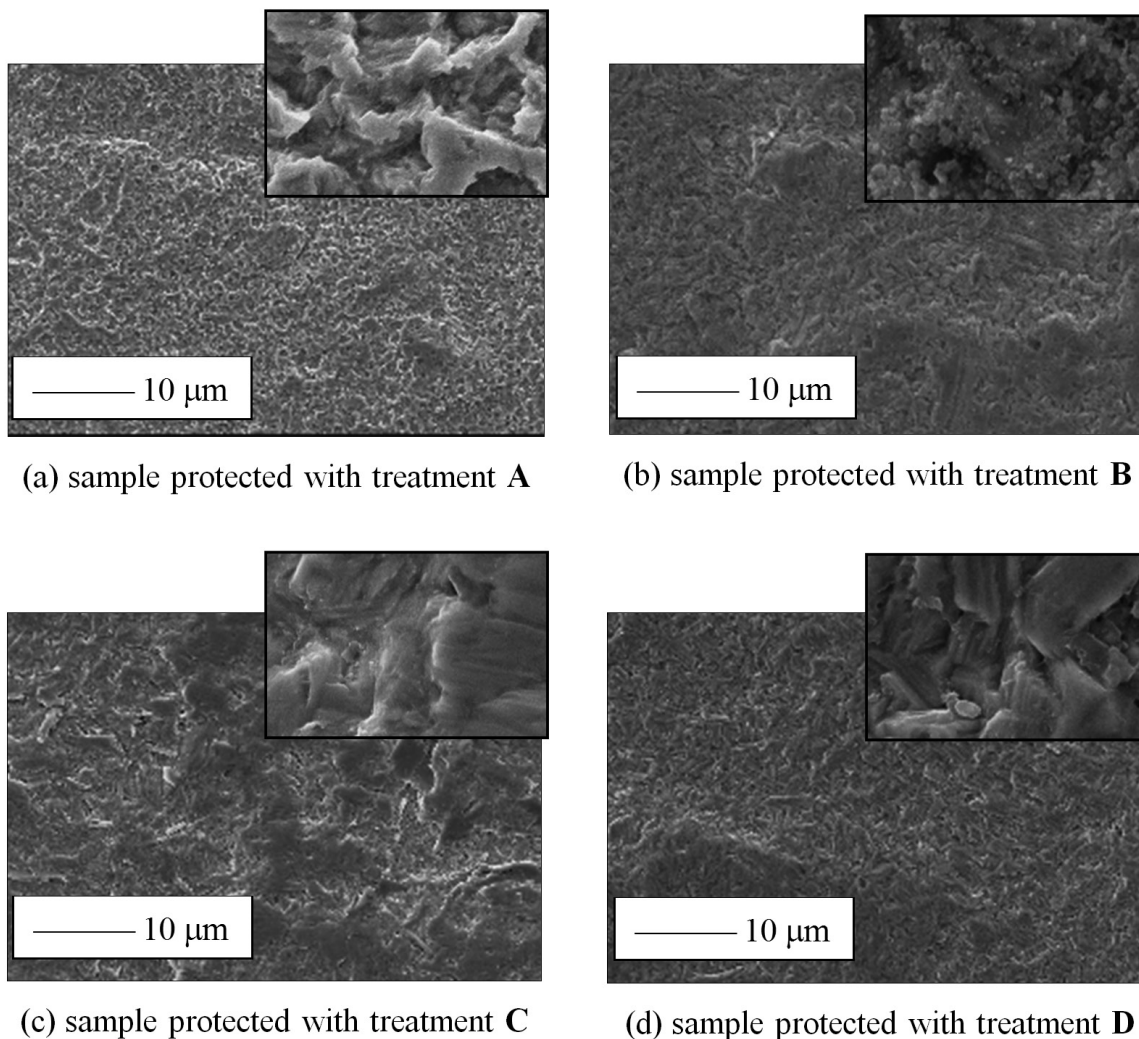


Figure 1. SEM micrographs of the electrogalvanized steel samples covered with different conversion treatments.

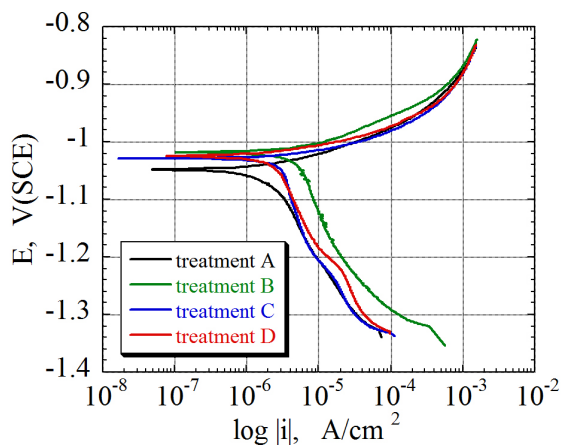
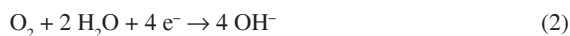


Figure 2. Potentiodynamic polarization curves of electrogalvanized steel protected with the different conversion treatments in aerated $0.3 \text{ mol.L}^{-1} \text{ Na}_2\text{SO}_4$ solution, pH 10. Scan rate 1 mV.s^{-1} .



occurred in such a way that the former process took place at defects of the conversion layer and the latter on the surface mostly.

Hence, zinc hydroxide precipitates on the surface and changes to zinc oxide gradually, forming a passive film²³, as:

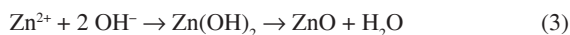


Figure 2 depicts typical potentiodynamic polarization curves for electrogalvanized steel samples covered with the different conversion layers and immersed in aerated alkaline sulfate solution. In it can be readily observed that even though the anodic curves did not give much information since the corresponding to the A, C and D samples were rather similar and slightly greater than the corresponding to the sample B, after active zinc dissolution, the anodic current density showed a certain trend to reach a limiting value. Such

a result seems to be due to a diffusion-controlled process derived from the high dissolution rate reached at high anodic overpotentials, which may act as a protective barrier²⁴.

The same Figure shows that not only an opposite and slightly more significant difference took place in the cathodic branch, but also that the corrosion rate in the aerated Na_2SO_4 medium was under cathodic control (oxygen diffusion) regardless the conversion layer chemical composition. So, the lowest cathodic current density, indicating the more significant suppression of the oxygen reduction reaction, corresponded to the **A** and **C** samples, followed by the sample **D**, with a shoulder at ≈ -1.2 V/SCE attributed to the onset of the hydrogen evolution reaction. The higher value was shown by the sample **B**. From the latter results, the polarization level for the oxygen reduction reaction was ranked in the order: treatment A \equiv treatment C \approx treatment D > treatment B.

Table 2 shows that whereas the corrosion potential (E_{corr}) of the electrogalvanised sheet panels covered with the different conversion layers stabilized around -1 V/SCE, the corrosion current density (i_{corr}) calculated by extrapolation of the Tafel slopes was also comparable. This feature could be explained in terms of the fact that the porous nature of the studied conversion layers as well as of the corrosion products layer that was being formed allowed, although limitedly, the continuous development of zinc corrosion processes underneath the likely Zn oxo-hydroxide layer covering the localized conversion layer defects.

4. EIS Measurements

4.1. Impedance spectra

The assessment of the coatings protective properties was based on the analysis of impedance spectra evolution at different exposure times in the aerated $0.3 \text{ mol L}^{-1} \text{ Na}_2\text{SO}_4$ solution.

At first glance, a comparative evaluation of the coatings corrosion resistance was carried out by observing the values of both the $|Z|$ at low frequencies and the maximum phase angle. The analysis of the phase angle spectra can furnish useful information because it is quite sensitive to coating degradation²⁵.

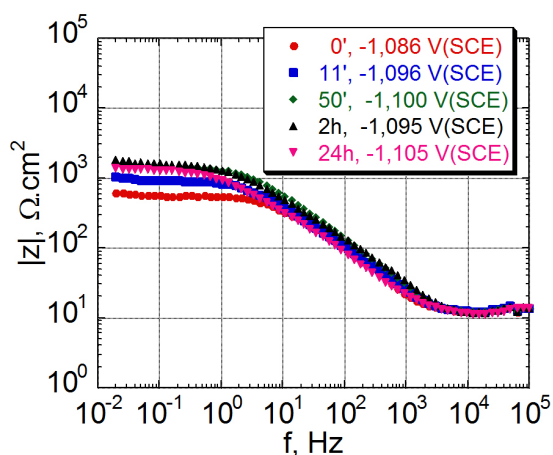
Figure 3a shows the Bode plots representing the impedance modulus ($|Z|$) vs. frequency for the sample **A** at different immersion times in the test solution. As seen, at low frequency (0.02 Hz) and short immersion times ($<2 \text{ h}$), the $|Z|$ values increased up to $10^3 \Omega \text{ cm}^2$, and after 24 h of immersion, they were slightly great than this value. The coupled phase angle evolution, Figure 3b, allows observing

Table 2. Values of E_{corr} and j_{corr} of Zn coatings after conversion treatment.

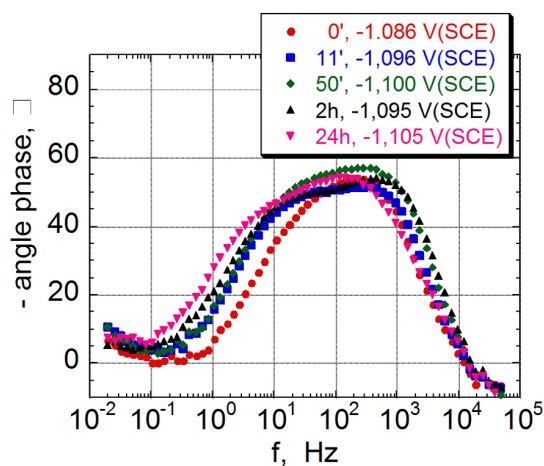
Treatment Identification	E_{corr} V(SCE)	i_{corr} $\mu\text{A}\cdot\text{cm}^{-2}$
A	-1.05	3.00
B	-1.02	4.00
C	-1.02	3.00
D	-1.02	3.00

a first time constant with a maximum value of 58° while, at low frequency (0.02 Hz), the curves suggest the appearance of a shallow second time constant which remained after 24 h of immersion. This confirms the presence of the corrosion products that, nevertheless, are not very protective as the impedance modulus slightly decreases. For this immersion time, the high frequency phase angle slightly deformed in comparison with the other situation would be indicating the onset of a new process that accelerates the interfacial reactions. This process could be, for instance, diffusion of aggressive species through the non-protective corrosion products. After 2 h of immersion, at medium frequencies, a small modification of this time constant took place. A possible explanation for this behavior is based on the assumption that the conversion coating was not compact.

Figure 4a shows the Bode plot of $|Z|$ vs. frequency at different immersion times in the test solution for the sample **B**. It can be seen that except for the diagram acquired just after the immersion, which can represent a very unstable situation, the impedance at low frequency (0.02 Hz)



(a)



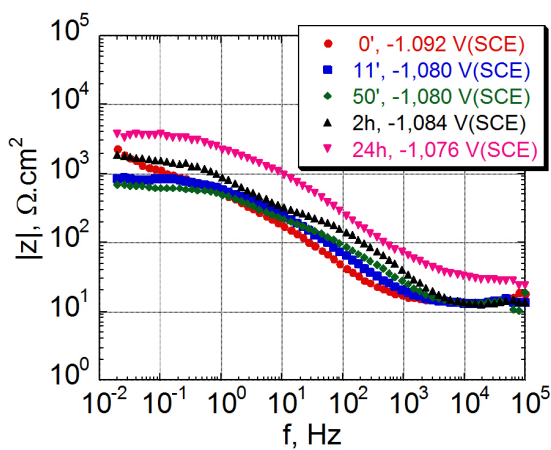
(b)

Figure 3. (a) Bode magnitude and (b) phase angle plots as a function of immersion time in aerated $0.3 \text{ mol}\cdot\text{L}^{-1} \text{ Na}_2\text{SO}_4$, pH 10, solution for Cr^{3+} chromated electrogalvanised steel coating – sample protected with treatment A.

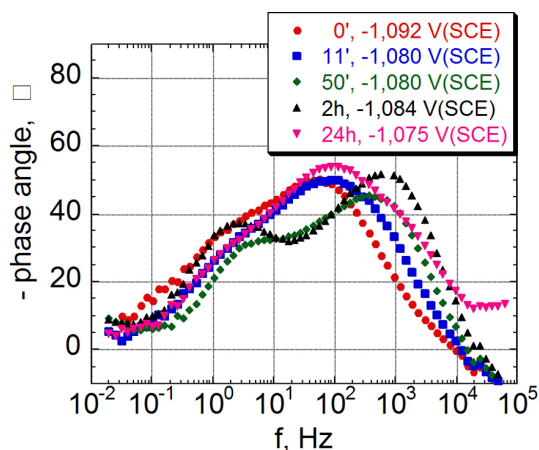
increased with the immersion time indicating improvement of the overall protective properties. This improvement was attributed to the sealant effect afforded by the zinc corrosion products gathered within the micropores and/or other coating defects. As well, Figure 4b shows that at the beginning of the test a time constant with a maximum phase angle value of 55° was well defined, and that after 50 min of exposure a second time constant indicating the onset of the corrosion process was clearly defined. After 24 h, the second time constant merge as the phase angle and it is very wide and deformed. The high frequency time constant is wide and deformed indicating an overlapping of processes. This is valid for all the immersion times, even though for 50 min and 2 hours the two time constants are clearly separated. In the low frequency region, there are almost no differences between the phase angle responses for the experiments after 11 min.

Figure 5a shows the $|Z|$ vs. frequency at different immersion times in the test solution for the sample C. As seen, except for the diagram acquired just after

the immersion, which as already can represent a very unstable situation, the impedance at low frequency (0.02 Hz) clearly decreased almost an order the magnitude from the 11 min up to 2 h of immersion, but thenceforth it remained apparently without changes until the 24 h. In principle, this evolution suggests the presence of an initially increasing electrochemical activity within the coating layer and at the zinc/coating interface, which attained an apparent equilibrium state as the exposure time elapsed since the impedance spectrum at the lower frequencies and after 24 h overlapped with the obtained at 2 h. Such interpretation was confirmed by the angle phase evolution, Figure 5b, where the maximum value not only shifted towards higher frequencies but also decreased indicating the loss of part of the coating dielectric capacitance (i.e., its isolating effect). As well, the appearance of a well-defined third time constant in the impedance spectrum obtained after 24 h of exposure demonstrate that even though at the lower frequency the $|Z|$ value at this time was equal than the obtained at 2h, the resistive and capacitive components contributing to such

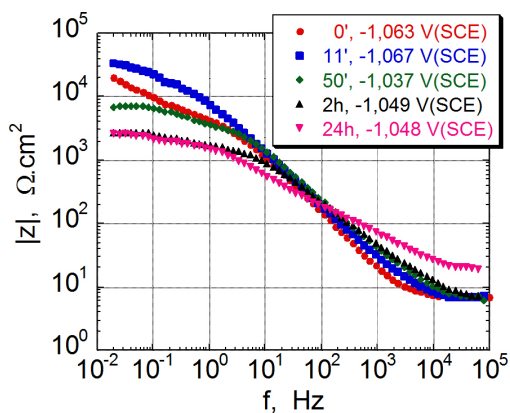


(a)

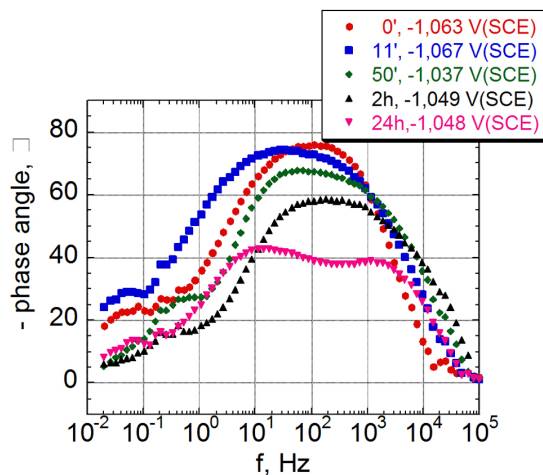


(b)

Figure 4. (a) Bode magnitude and (b) phase angle plots as a function of immersion time in aerated $0.3 \text{ mol.L}^{-1} \text{ Na}_2\text{SO}_4$, pH 10, solution, for nitro-cobalt electroplated steel coating – **sample protected with treatment B.**



(a)



(b)

Figure 5. (a) Bode magnitude and (b) phase angle plots as a function of immersion time in aerated $0.3 \text{ mol.L}^{-1} \text{ Na}_2\text{SO}_4$, pH 10, solution, for phosphatized electroplated steel coating – **sample protected with treatment C.**

value changed quali- and quantitatively. In this case, it was assumed that the corrosion resistance diminishing of the coated sample was compensated by the contribution of the barrier effect afforded by the corrosion products gathered within the coating defects.

With regard to the sample **D**, Figure 6a, it can be seen that at low frequencies it exhibited slightly higher initial $|Z|$ value ($\approx 4.10^3 \Omega\text{cm}^2$) than those ($1.5\text{--}2.7 \Omega\text{cm}^2$) obtained at longer immersion times in the test solution. All these values were suggesting an electrochemically active interface. This type of behavior could be explained

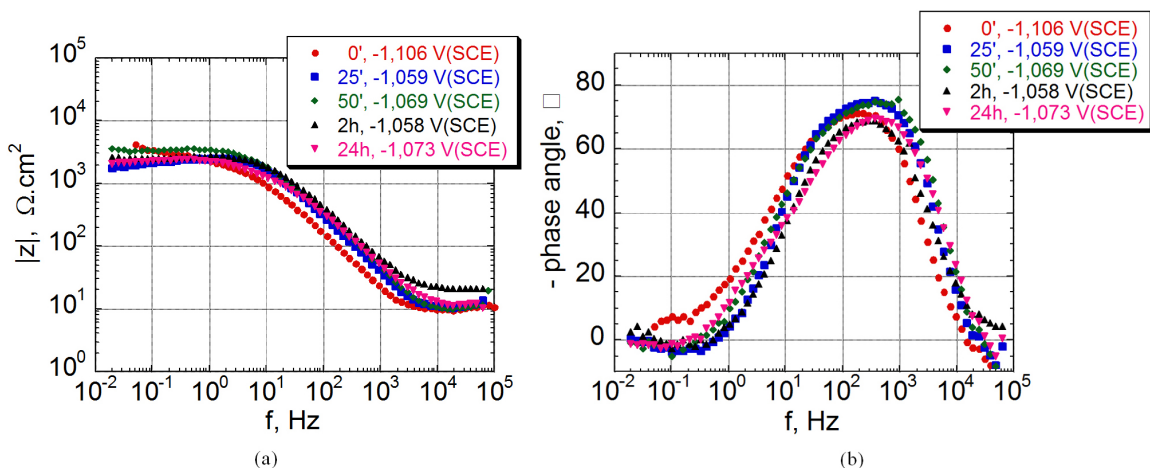
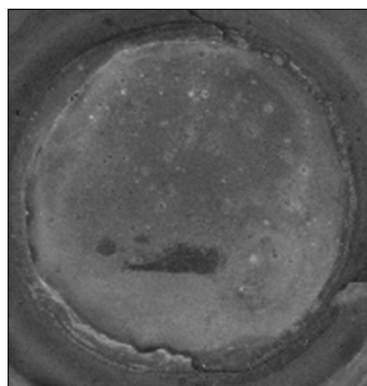
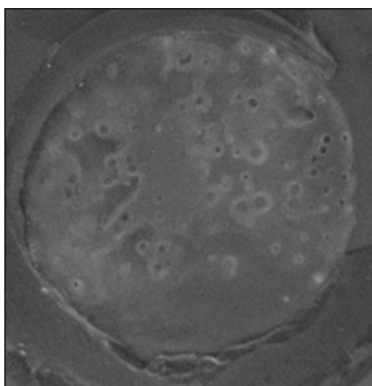
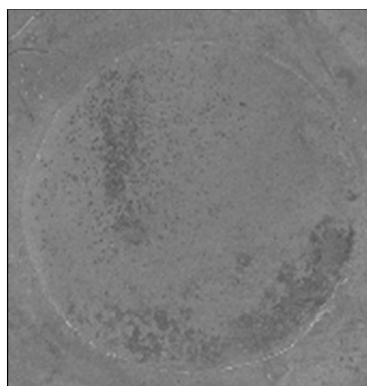
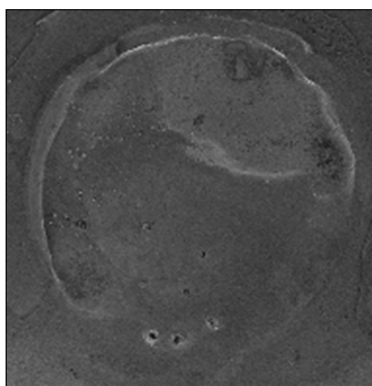


Figure 6. (a) Bode magnitude and (b) phase angle plots as a function of immersion time in aerated $0.3 \text{ mol.L}^{-1} \text{ Na}_2\text{SO}_4$, pH 10, solution, for Cr^{6+} chromated electrogalvanised steel sample – sample protected with treatment **D**.



(a) sample protected with treatment **A** (b) sample protected with treatment **B**



(c) sample protected with treatment **C** (d) sample protected with treatment **D**

Figure 7. Visual aspect of the samples after 24 h immersed in aerated $0.3 \text{ mol.L}^{-1} \text{ Na}_2\text{SO}_4$ solution, pH 10, at room temperature.

assuming that initially the loose corrosion products tended to become more compact, but as the time elapsed, part of them diffuse towards the electrolyte contributing to slightly diminish the coating resistive and capacitive properties. Despite this, changes underwent by the conversion layer had no significant effect on the corrosion behavior of the total coating probably due to the Cr^{+6} content and its self-healing characteristics.

Figure 6b illustrates that the time constant defined in the low frequency region just after immersion disappeared after 25 min and was replaced by an inductive loop; also that at medium frequencies a maximum phase angle of 75° was defined. As a second time constant did not appear in the impedance spectrum it was assumed, and confirmed by the visual inspection, that during this short period did not take place a significant zinc corrosion process.

5. Visual Inspection

After 24 h of immersion in aerated $0.3 \text{ mol L}^{-1} \text{ Na}_2\text{SO}_4$ solution, pH 10, the visual aspect of the electrogalvanized and treated **A**, **B**, **C** or **D** samples is depicted in Figure 7. In it can be seen that the surface of the sample **A** showed more white (zinc) and reddish (steel) corrosion products than the sample **C**, while in the case of the samples **B** and **C** only white corrosion products could be seen at naked eye. Probably due to the self-healing effect provided by the free- Cr^{6+} ions able to diffuse within the conversion layer structure, the sample **D** was the less attacked.

6. Conclusions

The development of the present experimental study for 24 h of immersion in naturally aerated $0.3 \text{ mol L}^{-1} \text{ Na}_2\text{SO}_4$ solution, pH 10, allows the following main conclusions to be drawn:

- The electrochemical response given by the same samples subjected to anodic and cathodic polarizations allowed to infer that: 1) the corrosion current densities

estimated from the Tafel slopes extrapolation were rather similar; 2) the polarization level for the oxygen reduction reaction as a function of the treatment composition was ranked in the order: $A \equiv C \approx D > B$; and 3) regardless the chemical composition of the conversion layer, the corrosion rate was under cathodic control (oxygen diffusion);

- The open-circuit potential evolution as a function of the immersion time could be used to evaluate the samples' corrosion behavior at least from a thermodynamic point of view;
- The EIS data showed that within the two first hours of immersion the evolution of the total impedance and phase angle values in the four coated samples was clearly differentiated and indicative of significant electrochemical activity. However, after 24 hours of immersion mainly the impedance values were rather similar. This was explained assuming that once formed the layer of zinc corrosion products, which blocked the conversion coating defects, the zinc corrosion process in the localized areas underneath that layer should not be very different. From the experimental data, a ranking of corrosion protective properties afforded by the different conversion treatments would be as follows: $D \approx C > B \gg A$;
- Visual inspections at naked eye of the tested samples allowed concluding that, the **D** samples did not show corrosion but the other presented different forms of attack. White and reddish corrosion products (samples **A**), only white (**B** and **C** samples).

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